

# Microfluidics Reaction Technology (MRT) for Continuous, Bottom-Up Production of Drugs

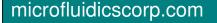
#### Thomai "Mimi" Panagiotou, Ph.D.

Chief Technology Officer, Microfluidics International

And

# Robert J. Fisher

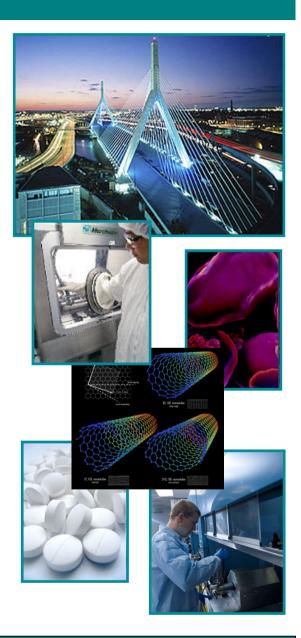
Chemical Engineering, MIT





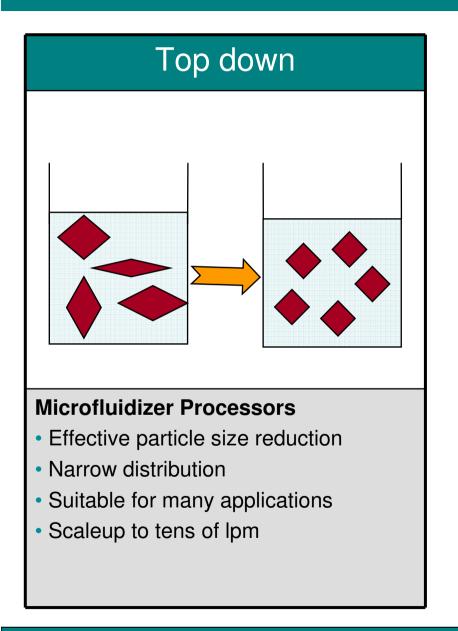
# **Microfluidics at a Glance**

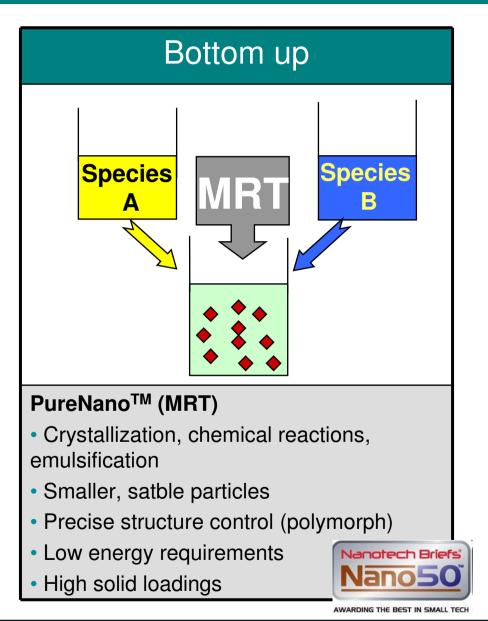
- Microfluidizer<sup>®</sup> high shear fluid processors for processing of multiphase fluids to produce nanomaterials
- "Top Down" and "Bottom Up"
- Lab to large scale processors are used for production of market drugs, vaccines, inkjet inks, coatings, nutraceuticals and cosmetics
- Holistic approach to development Application
   Process
   Processor
- Headquartered in Boston, MA and Germany with localized sales and support in 47 countries
- 27 years serving customers worldwide





# Two Continuous Processing Technologies







# **Pharmaceutical / Biotech Applications**

### **By indication**

- Cancer drugs
- Anesthetics
- Inhalable drugs
- Anti-inflamatory
- Ocular drug
- Vaccine adjuvants

## By delivery method

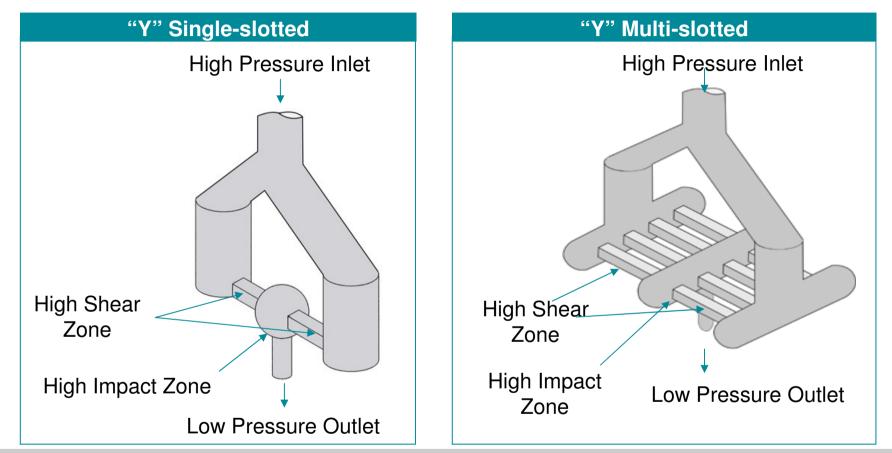
- Injectables
- Inhalables
- Orals
- Transdermals
- Targeted delivery
- Control delivery
- Medical devices

## By material type

- Emulsions for delivery of hydrophobic drugs
- Liposomes for delivery of hydrophobic/hydrophilic drugs
- Drug particles with tailored structure (crystalline/amorphous)
- Polymer drug encapsulation



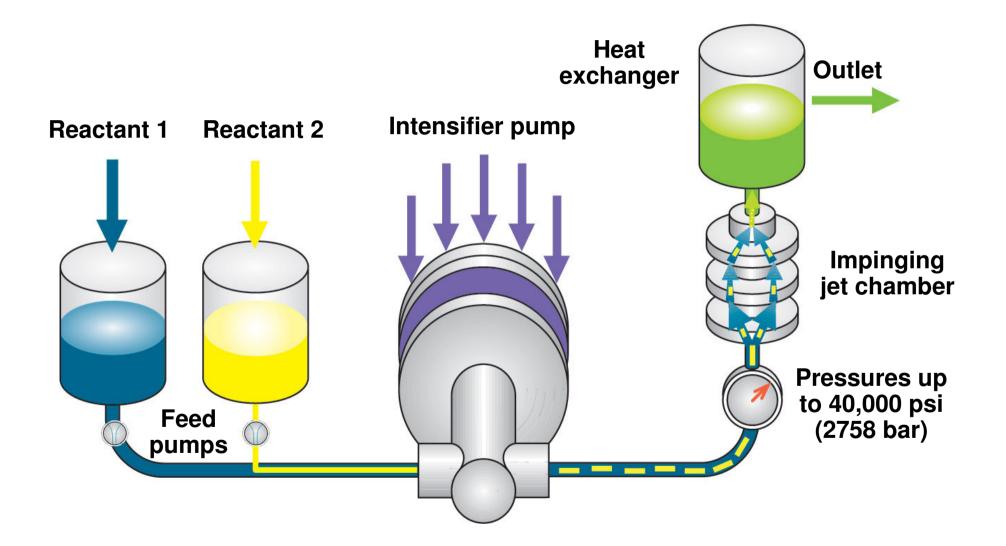
# Interaction Chamber – High velocity impinging jet



- Channel velocities over 400 m/s
- Channel minimum dimensions typically 50-300 microns
- Shear rates up to 10<sup>7</sup> s<sup>-1</sup>; controllable mixing in the 25-50 nm scale
- Constant mixing conditions for entire batch
- Demonstrated scalability to tens of liters per minute

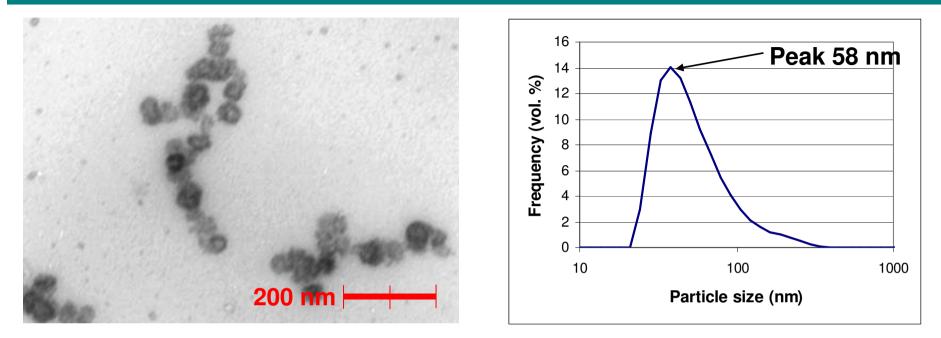


# PureNano<sup>™</sup> - MRT Configuration





### **Azithromycin Crystallization**



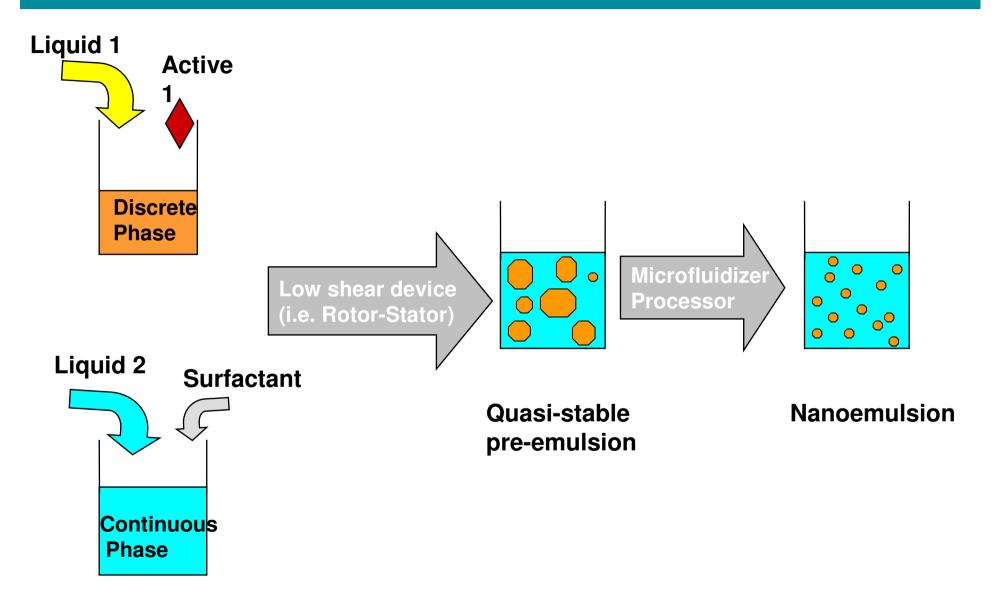
- **Concentration:** 75 mg Azithromycin/ml of DMSO
- DMSO to water ratio: 1:4
- Z-average PS: 82 nm
- Critical process parameters:
  - Solvent/anti-solvent type
  - Supersaturation
  - Temperature
  - Mixing intensity

#### Particles were stable - NO SURFACTANTS WERE USED

T. Panagiotou, et al NSTI-Nanotech 2007, www.nsti.org, ISBN 1420063766 Vol. 4, pp. 246-249, 2007.

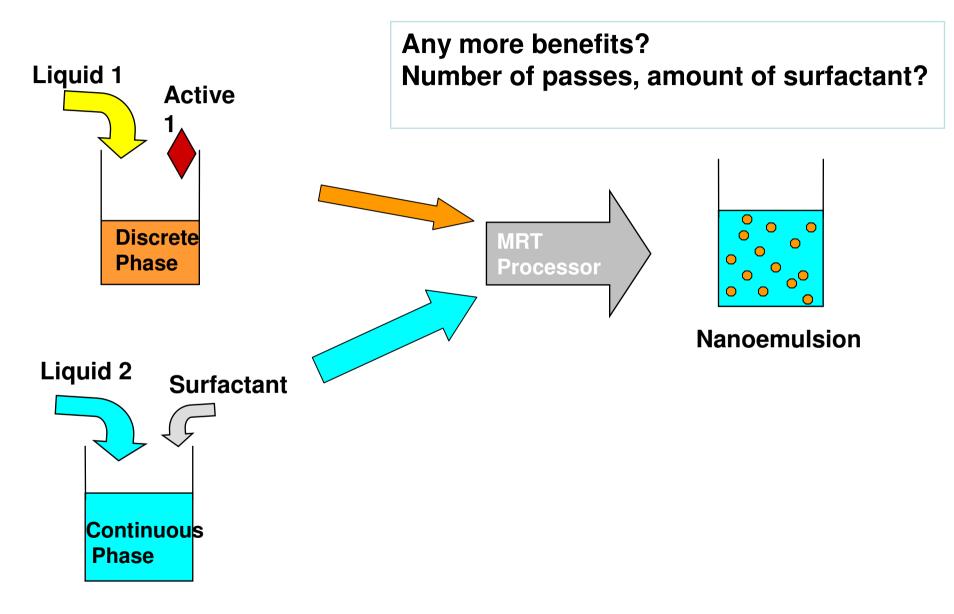


## **Emulsion Production – "Top Down"**



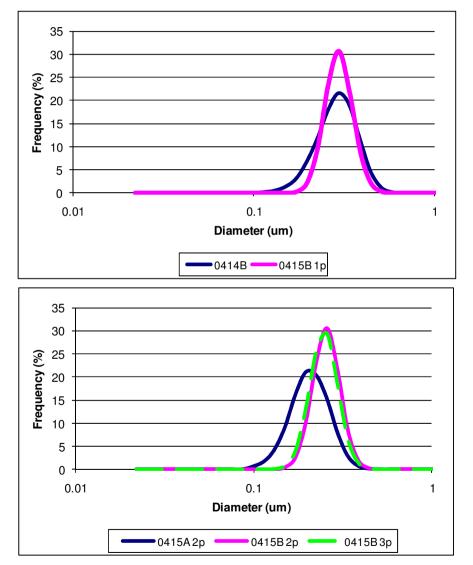


## Emulsion Production – "Bottom Up" (No Need for Pre-emulsion)





#### 40% o/w emulsion with 2.4% wt. surfactant



= PN ---- = Top Down ---- = Top Down

#### Single pass

• Top down and PN method gave similar results

#### **Two passes**

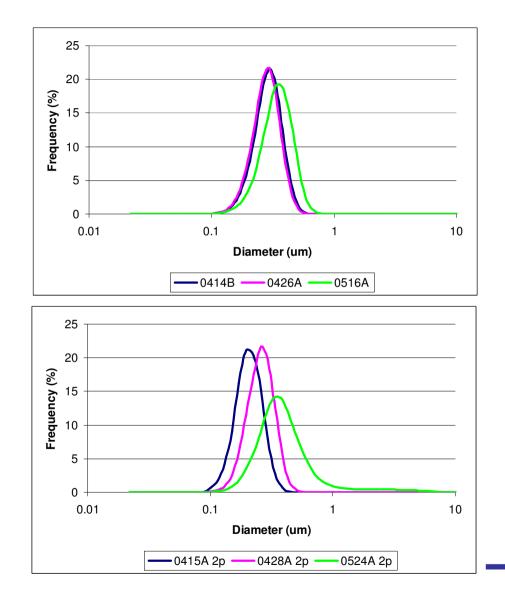
• PN median 19% (46 nm) smaller than 2 top-down passes with pre-mix

• PN median 17% (39 nm) smaller than 3 top-down passes with pre-mix

• Top-down particle size plateaued, while PN achieved smaller sizes



## 40% o/w emulsion with varying surfactant concentration



Deliver the oil over 1 pass (PN)

- Shape of peaks identical
- Emulsion starts to break down with 1.8% T80

Deliver the oil over 2 passes (PN)

- 1.8% is not sufficient
- 2.4% and 2.0% both decrease further with oil delivery delayed over an additional pass

### Surfactant

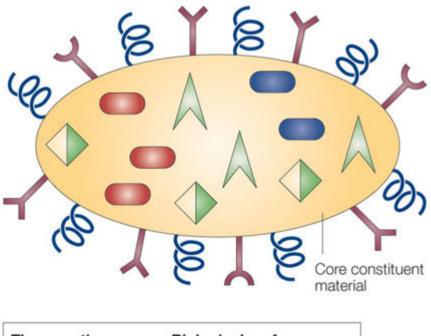
= 2.4% \_\_\_\_ = 2.0% \_\_\_\_ = 1.8%

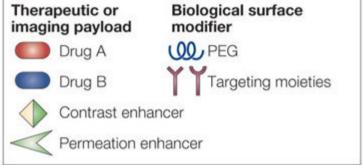


# **Multi-functional Nanosystems**

- Combination drug products
- Drug and resistance modulator
- Drug and energy delivery (heat, light, and sound)

# Drug and imaging agent



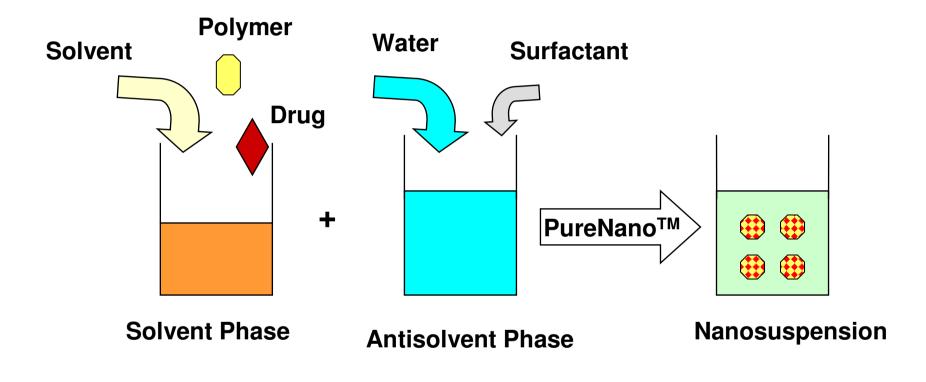


Ref. M. Ferrari. Nat Rev Cancer., 5(3):161-71 (2005).

Nature Reviews | Cancer



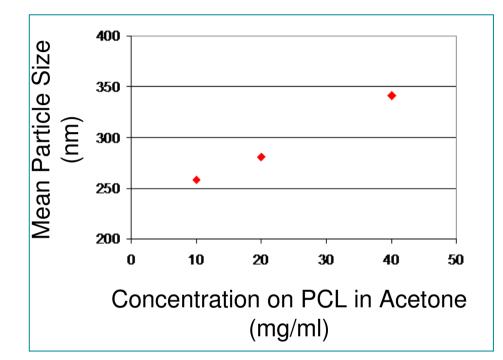
## Bottom-up Precipitation/Nanoencapsulation Using PureNano<sup>™</sup>



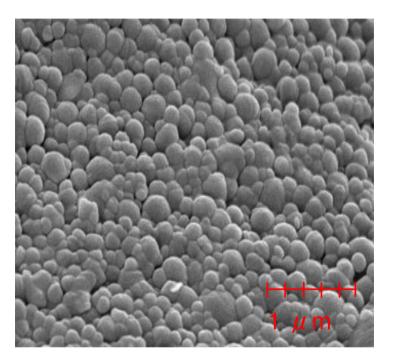
- · Solvent is miscible with water
- Polymer and API precipitate as soon as the solvent and the water phase mix
- Post processing includes removal of solvent



## **PCL particles - Effects of Key Process Parameters**



- PCL particles
- Mixing ratio: 1:9
- Pressure: 100 MPa

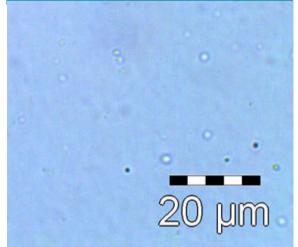


#### PCL nanoparticles created by PureNano<sup>™</sup>



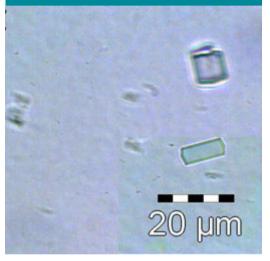


#### Polymer Encapsulation Using PureNano<sup>™</sup>





Polymer Encapsulation in Beaker



20 mg/ml PLGA +10 mg/ml CBZ in acetone mixed with water using PureNano<sup>™</sup> (1:3 ratio)

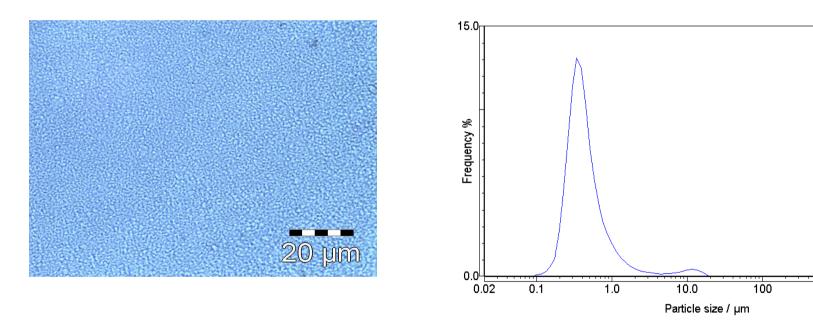
10 mg/ml CBZ in acetone mixed with water using PureNano<sup>™</sup> (1:3 ratio) 20 mg/ml PLGA +10 mg/ml CBZ in acetone mixed with water using PureNano<sup>™</sup> (1:3 ratio)



Polymer Matrix	Initial Polymer Concentration (mg/ml)	Initial Drug Concentration (mg/ml)		Final Drug Concentration in Nanoparticles (wt. %)
PLGA	5	2.5	66.7	25.6
PLGA	5	1.25	56.9	12.0
PCL	5	1.25	58.9	13.2

## **Organic Calcium Salt in Sub-micron Particles (3-phase Reaction)**

- Process: Acid-Base reaction
- Reactants: Calcium hydroxide (Ca(OH)<sub>2</sub>) water slurry and a fatty acid melt at 65-85<sup>o</sup>C; reactant streams are immiscible
- **Product:** Stable calcium salt nanosuspension with over 38% solids



• Median particle size (D50): 367 nm



100

Cumulative % undersize

<sup>\_</sup>0.0

1020

# PureNano<sup>™</sup> - Processes of and Advantages

### Crystallization, precipitation

- Controlled size micro/nano particles
- Smaller particles, lower energy than "top down"
- > Control of crystalline structure -high purity material

### Chemical reactions (single-,multi- phase)

- Expedited chemical reactions
- >Enhanced selectivity/minimizes side reactions
- ➢Particle size control

#### Nanoencapsulation

High encapsulation efficiency

### Emulsification

- > Avoid the need for pre-processing
- ➢Potentially minimizes the amount of surfactant

### Adsorption/chemisorption



## **PureNano<sup>™</sup> Machine Specifications**



- Flow rate: ~500 ml/min
- Reactant streams: Two
- Flow rate ratio: 1:1, 1:2,... 1:50
- Utility requirements (electrical):
  ~ 3 phase 50/60 Hz service,
  208/230/460V, 20A max

