

# Digitalisation of Pharmaceutical Product Development with Physics-based Multiscale Models

Formulation 4.0: Put Digital into Formulation, London, UK, 26<sup>th</sup> July 2024

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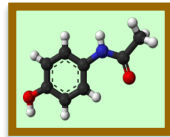
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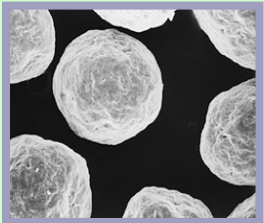


# Digital Formulation Engineering



Primary manufacturing

(synthesis, crystallization)



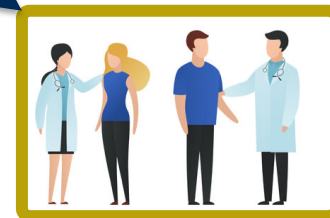
**Secondary  
manufacturing**



Formulation  
Engineering;  
Process  
Engineering



Digital Transform APIs to Products– Digital Product Engineering



# An ambitious scientific question

Can we develop a digital tool that can assess the performance, process-ability and product properties of identified drug molecules

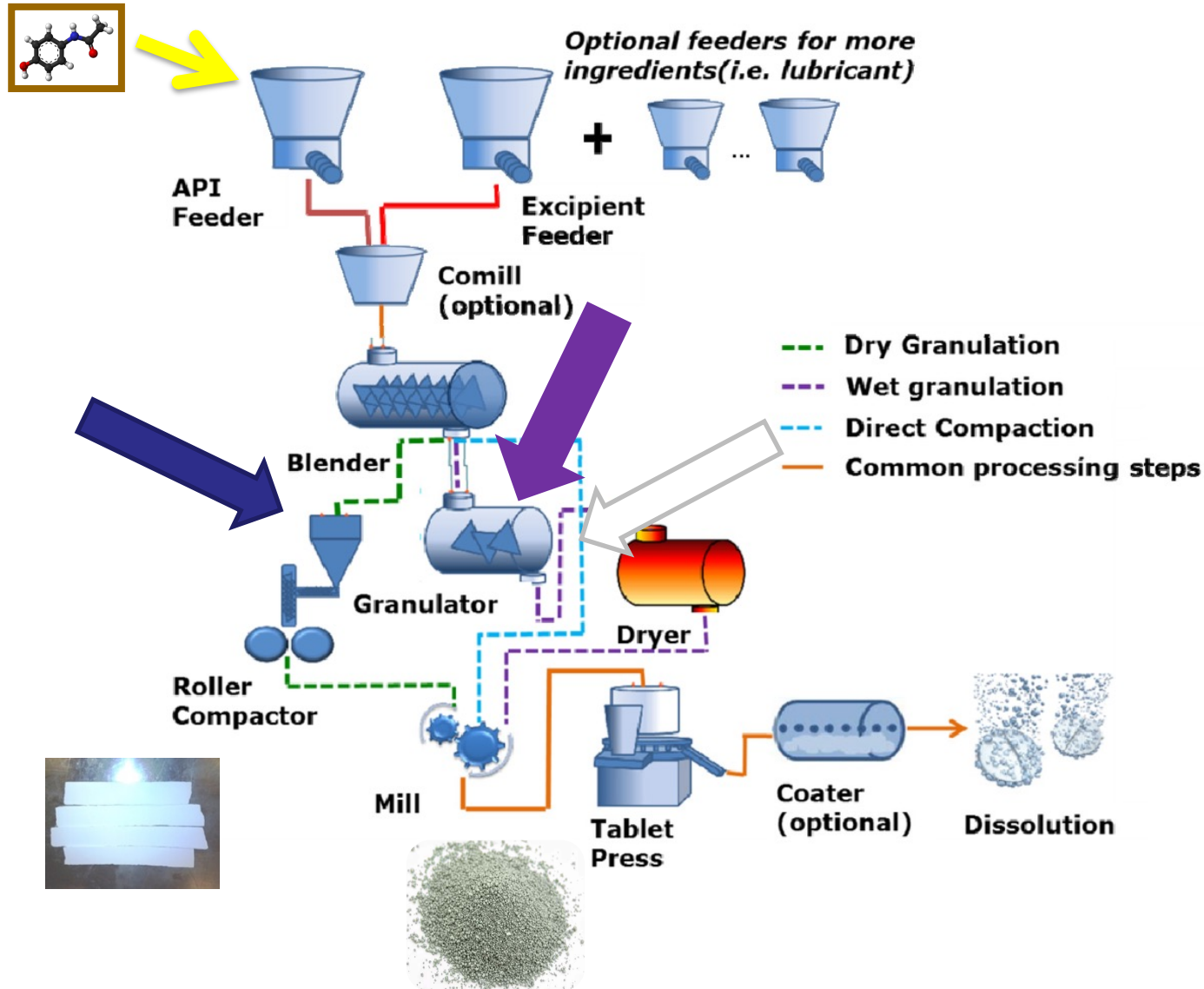
At a very early stage of drug development

Using only a very limited amount of materials

Based upon a small amount of experiments

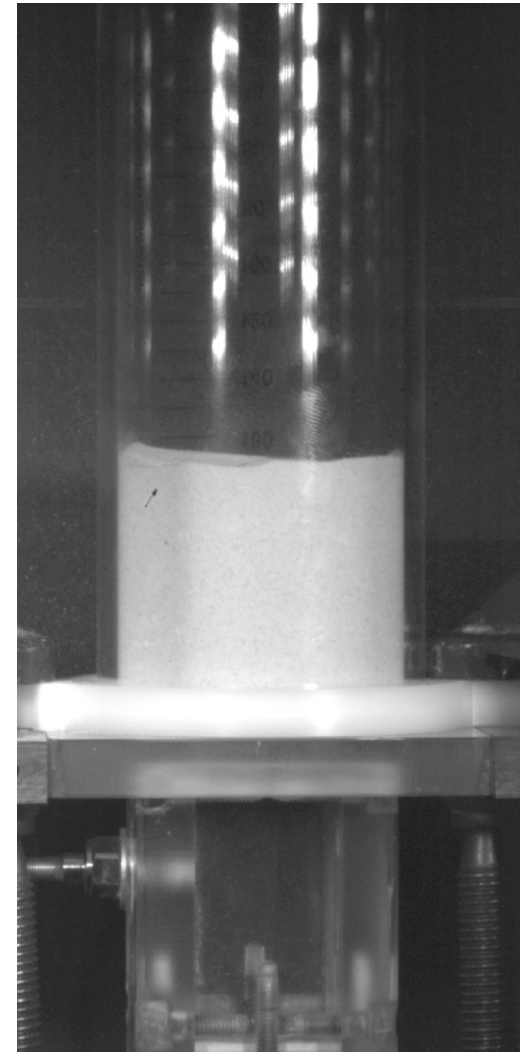
so that optimal formulation and manufacturing processes can be designed and the duration and costs of drug development can be significantly shortened?

# Pharmaceutical Manufacturing Processes

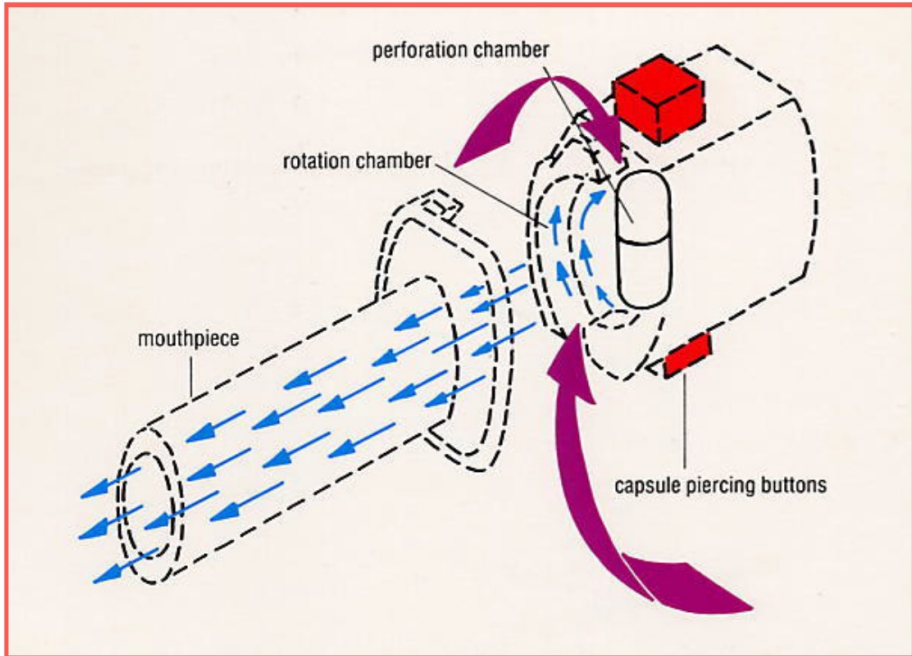
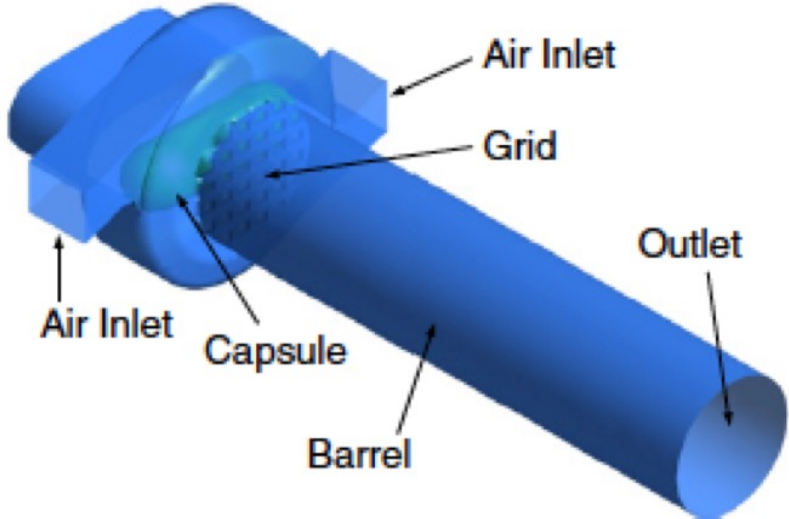
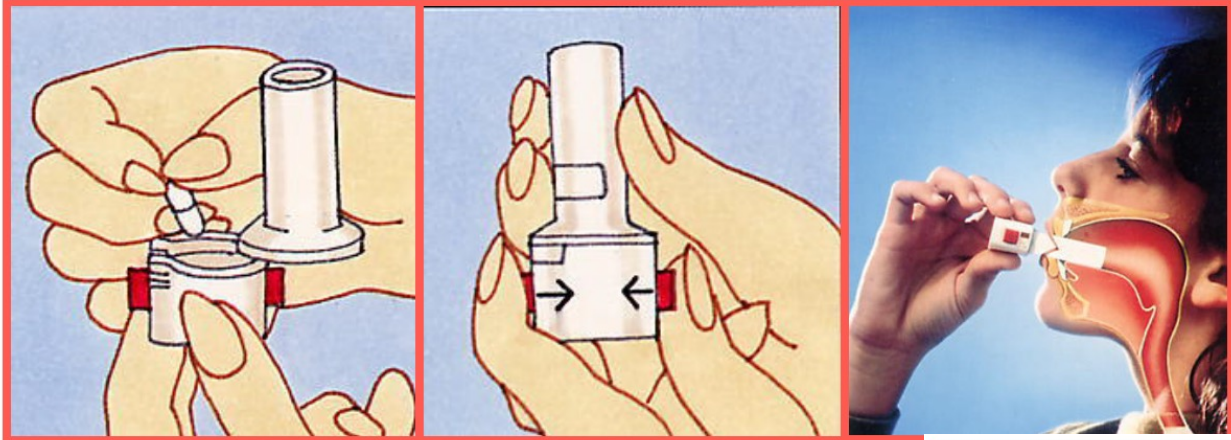


# Formulation development challenge

- With an identified API, formulation development and process design is not a trivial task.
- Need to ensure each unit operation is performed properly.
- Conventional trial-and-error approach is time consuming and costly.
- To some extent, pharmaceutical industry lags behind many other industries in exploiting innovative tools and technologies, such as digital technology and AI.
- Partly due to the distinctive materials attributes of powders from conventional solids, liquids and gases.
- For a typical manufacturing process, **powders can manifest themselves as fluids or solids in different unit operations.**
- Computational tools need to be able to describe the diverse powder behaviours. It is challenging (not impossible) for one model to fit all requirements.

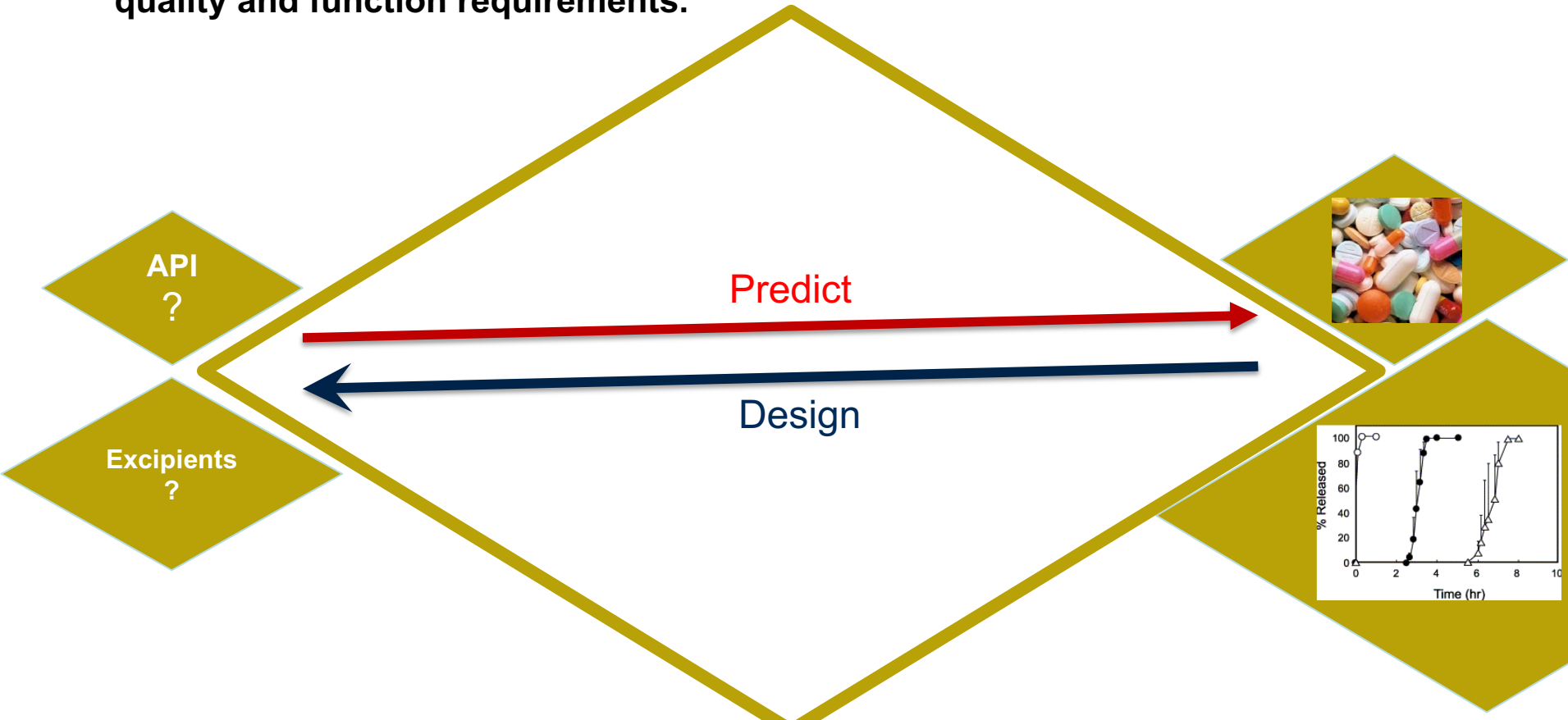


# A system approach in product development



# Key questions in pharmaceutical product development

- 1) Can we predict the behaviour of API and excipients in formulation and manufacturing?
- 2) Can we use it to optimise the formulation and process conditions?
- 3) Can we design the formulation and manufacturing processes based upon the quality and function requirements.



# Two computational approaches

## Mechanistic Modelling

- ❑ Based upon underlying physics, chemistry and biology
- ❑ Using mathematical tools (e.g. Differential equations, stochastic models) to describe the dynamic behaviour of the system
- ❑ Formulate mathematical/numerical models capturing the interplay between various parameters.
- ❑ Focus on unit operations, i.e. step by step (hopper flow, mixing/blending, milling, dry granulation, wet granulation, die filling, tableting roll compaction coating)

## Machine Learning

- ❑ Enables computers to learn from data and make predictions without explicitly considering the underlying physics, chemistry or biology.
- ❑ Using algorithms that allow computers to learn patterns and insights from large datasets, facilitating predictive analysis.
- ❑ Depend on data, not process.



# Mechanistic Modelling Tools

Computational  
Fluid Dynamics  
(CFD)

Discrete  
Element  
Methods  
(DEM)

Finite Element  
Methods  
(FEM)

DEM-CFD

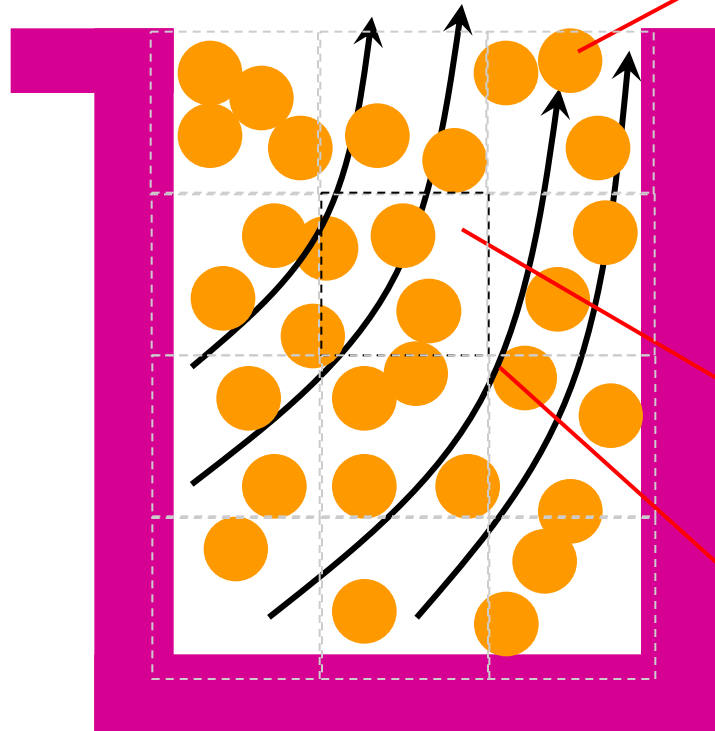
DEM-FEM

OIDP

Tablets

...

# Discrete element method (DEM)



The flow of particles is modelled using DEM.

The interaction between particles are rigorously modelled using theoretical contact mechanics:

- Hertz-Mindlin-Deresiewicz for elastic particles
- JKR for adhesive particles

The interaction between air and particles is considered.

The flow of air is modelled using CFD.

Particle equations of motion:

$$F_i = F_i^c + F_i^{fp} + F_i^e + m_i g = m_i \ddot{x}_i$$

$$T_i = I_i \ddot{\theta}_i$$

fluid particle interaction force

$$F_i^{fp} = -V_{pi} \nabla p + V_{pi} \nabla \cdot \tau_f + \varepsilon f_{di}$$

Total fluid-particle interaction force per unit volume

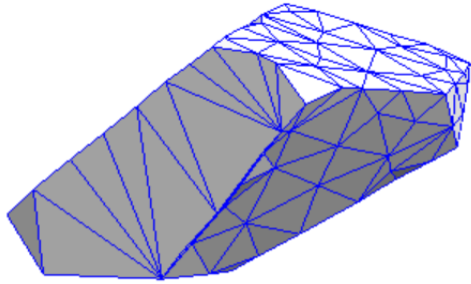
$$F_{fp} = \frac{\sum_{i=1}^{n_c} F_i^{fp}}{\Delta V_c}$$

Fluid continuity and momentum equations

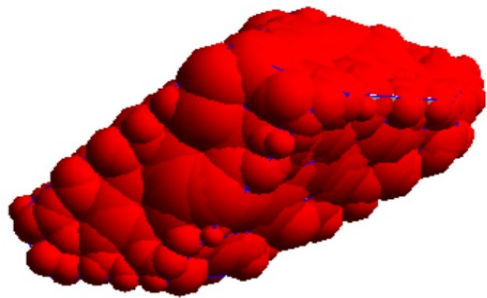
$$\frac{\partial(\varepsilon \rho_f)}{\partial t} + \nabla \cdot (\varepsilon \rho_f u) = 0$$

$$\frac{\partial(\varepsilon \rho_f u)}{\partial t} + \nabla \cdot (\varepsilon \rho_f u u) = -\nabla p_f + \nabla \cdot \tau_f + F_{fp} + \varepsilon \rho_f g$$

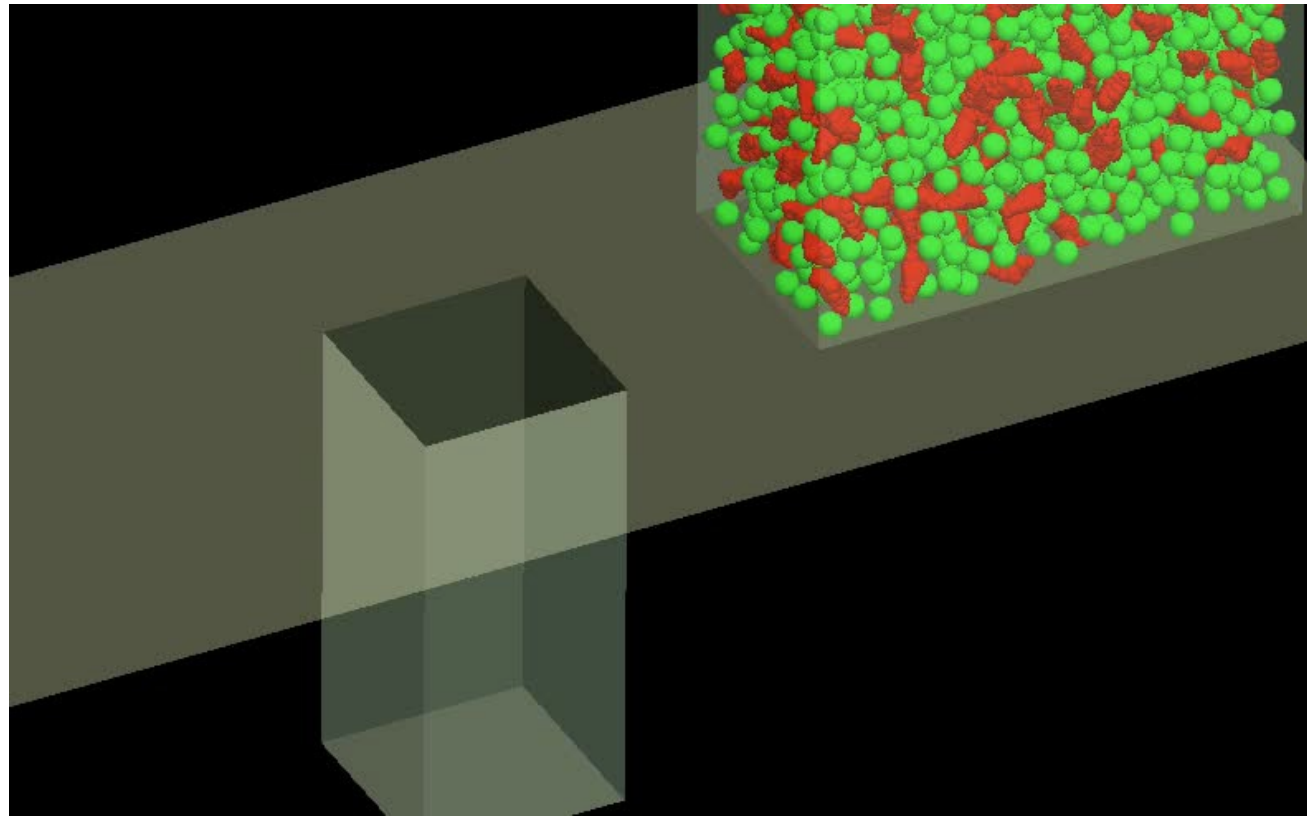
# DEM with real particles (Wu et al. 2016)



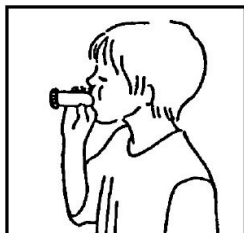
**Real crystal**



**DEM approximation**



# DEM-CFD for mechanistic understanding: Dry Powder Inhalation



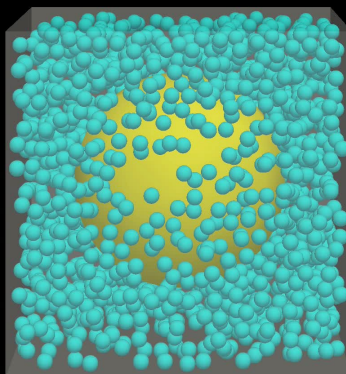
Deliver medicines directly to the lungs and airways in the form of dry powders;

For treating pulmonary and respiratory diseases, such as asthma, bronchitis and emphysema.

J Yang, CY Wu, M Adams. 2015. *Current Pharmaceutical Design* 21 (40), 5915-5922

J Yang, CY Wu, M Adams. 2014. *Acta Pharmaceutica Sinica B* 4 (1), 52-59I.

Attachment of drug particles onto a carrier in formulation development for dry powder inhalation



Detachment of drug particles from a carrier in air flow

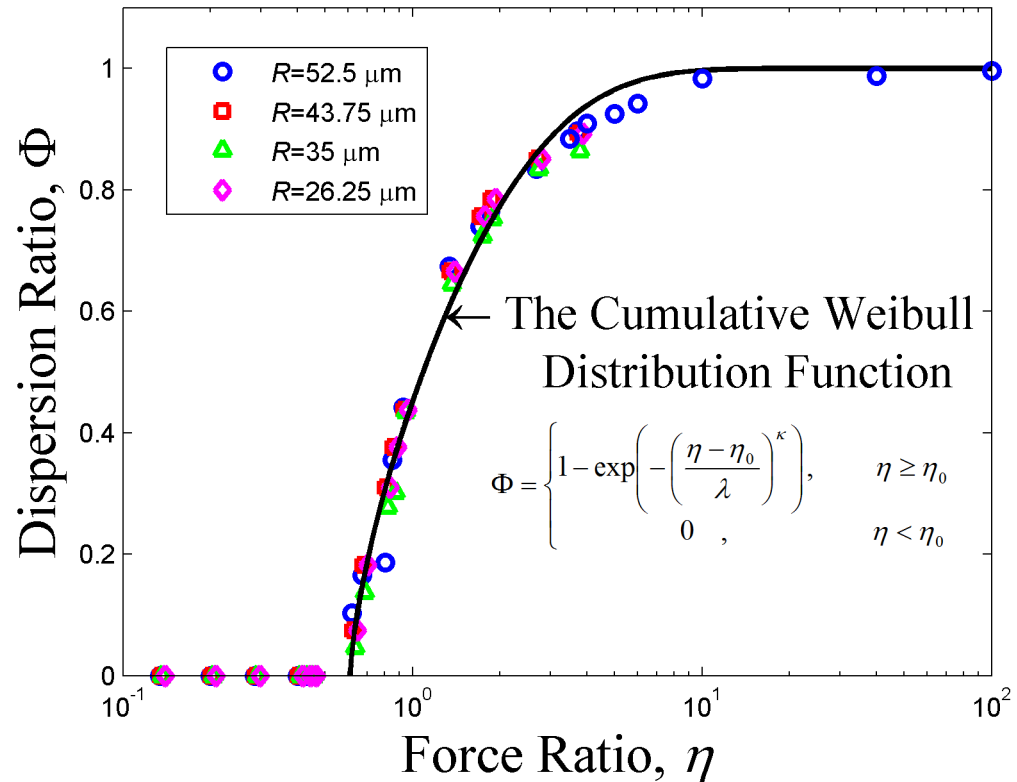


J Yang, CY Wu, M Adams. 2013. *Granular Matter* 15 (4), 417-426

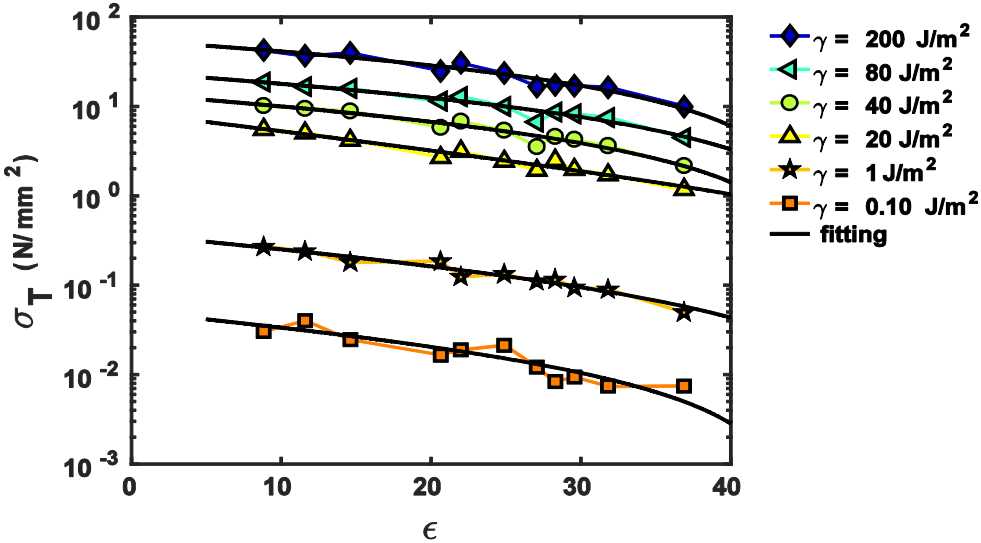
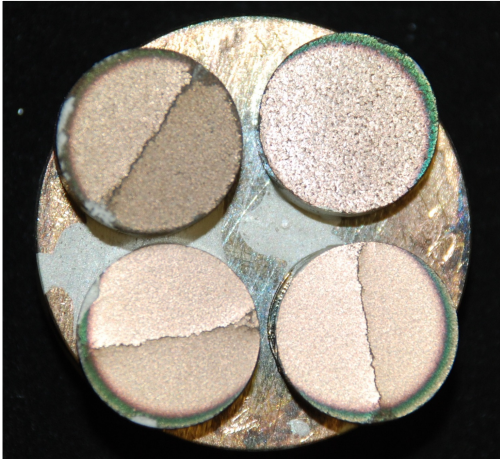
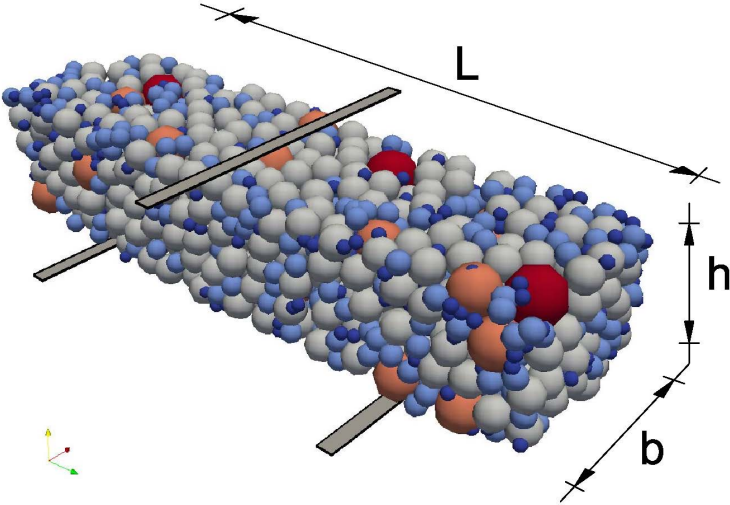
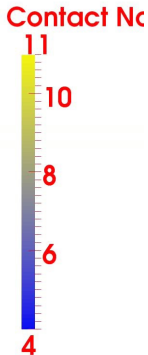
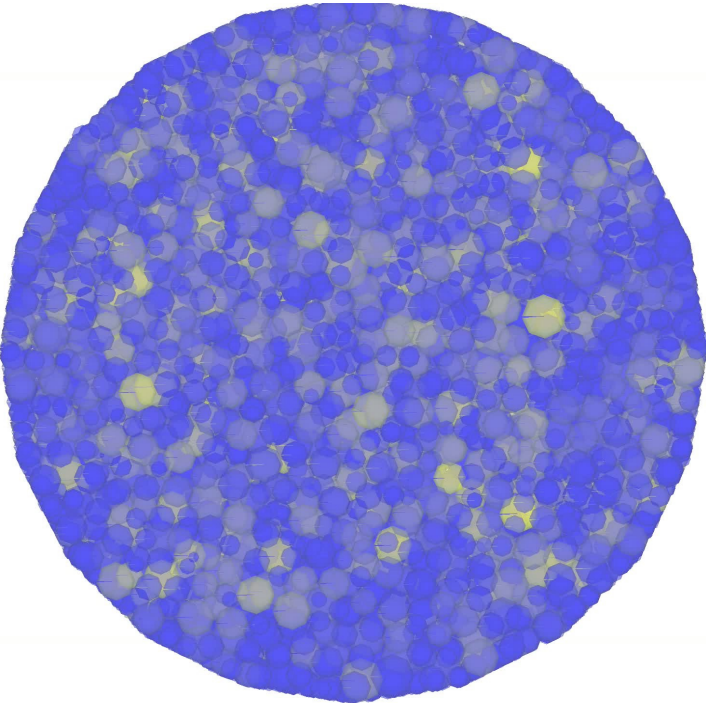
# Detachment Mechanism

DPIs Performance is the result of the balance of the removal force and adhesive force.

$$\eta = \frac{F_d}{F_c}$$

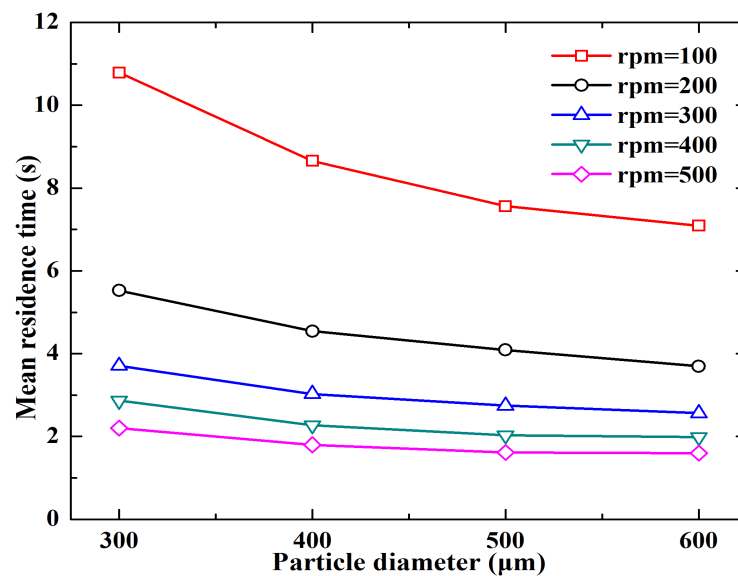
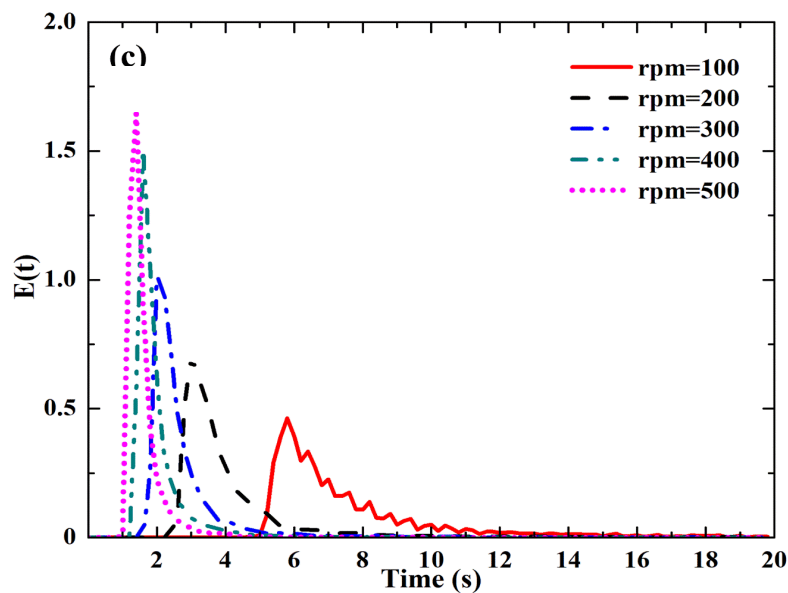


# DEM for mechanistic understanding: Mechanical Characterisation

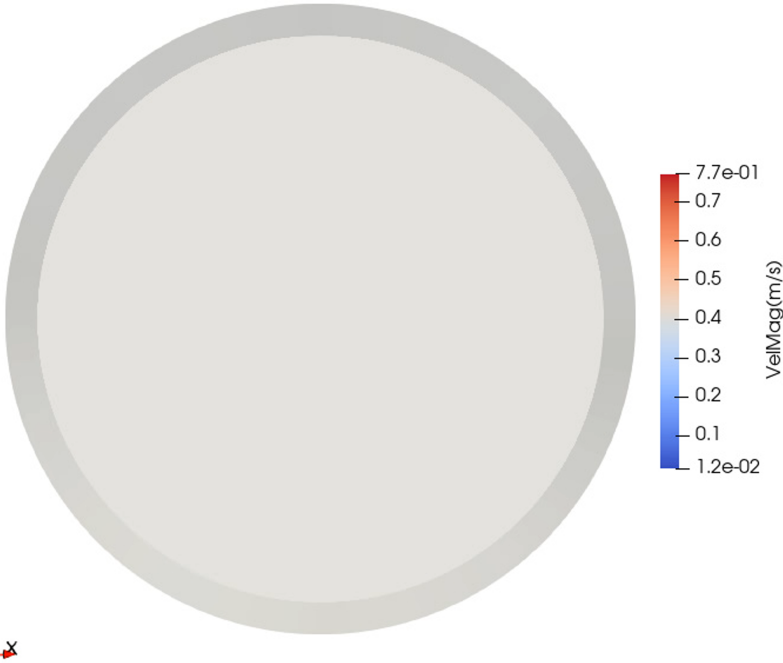
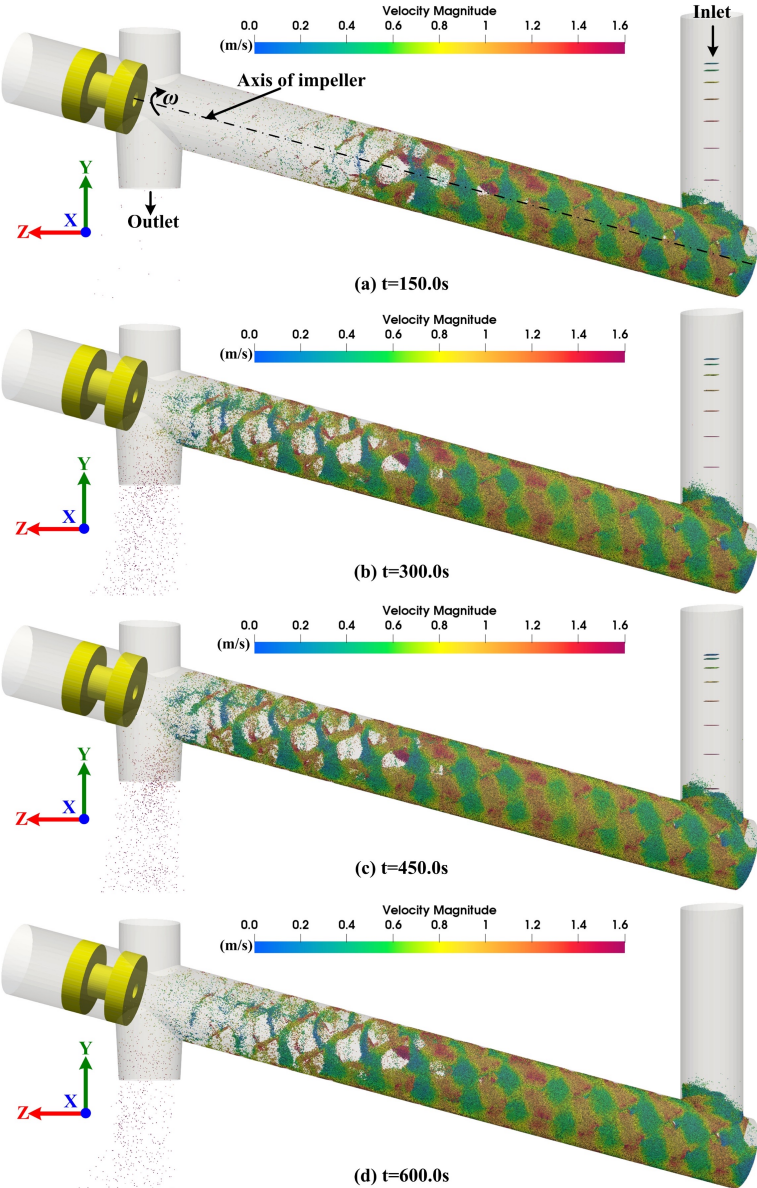


S Loreti, CY Wu. 2018. Three-dimensional discrete element modelling of three point bending tests: The effect of surface energy on the tensile strength. Powder Technology 337, 119-126

# DEM for Process Modelling: Twin Screw Granulation



# DEM for Process Modelling: Continuous Blending & Film Coating

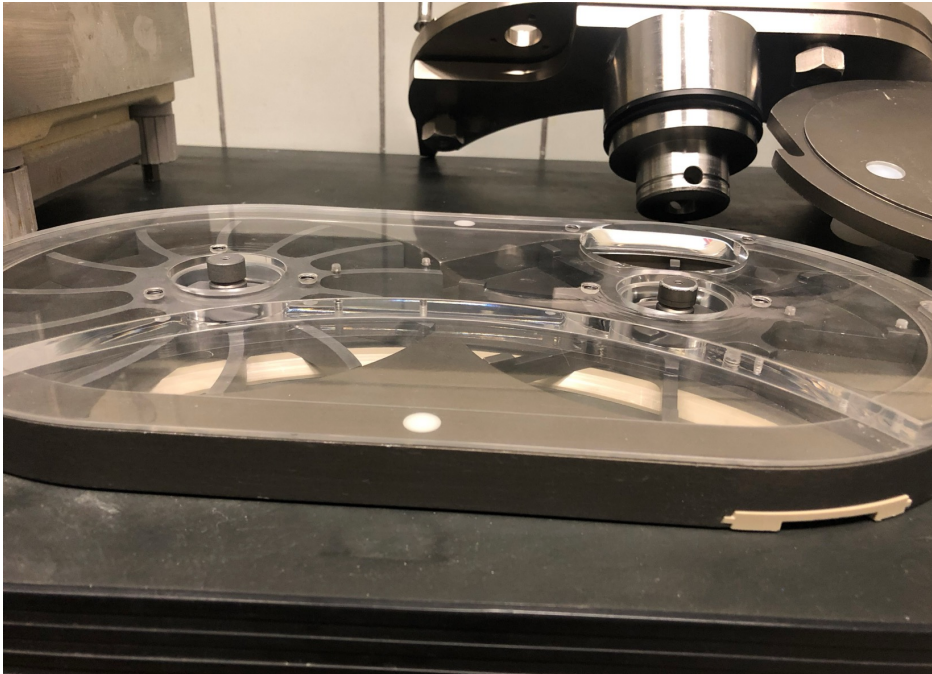


C Zheng, L Li, BJ Nitert, N Govender, T Chamberlain, L Zhang, CY Wu. Powder Technology 412 (2022) 117968



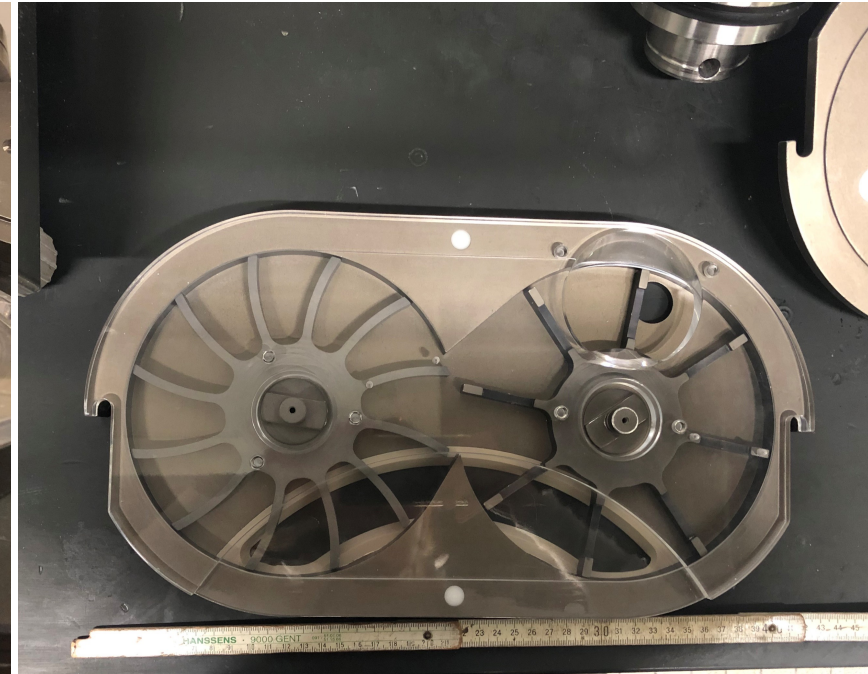
# Mechanistic modelling of die filling in a rotary tableting system

Side view



**Photos of feed frame**

Top view

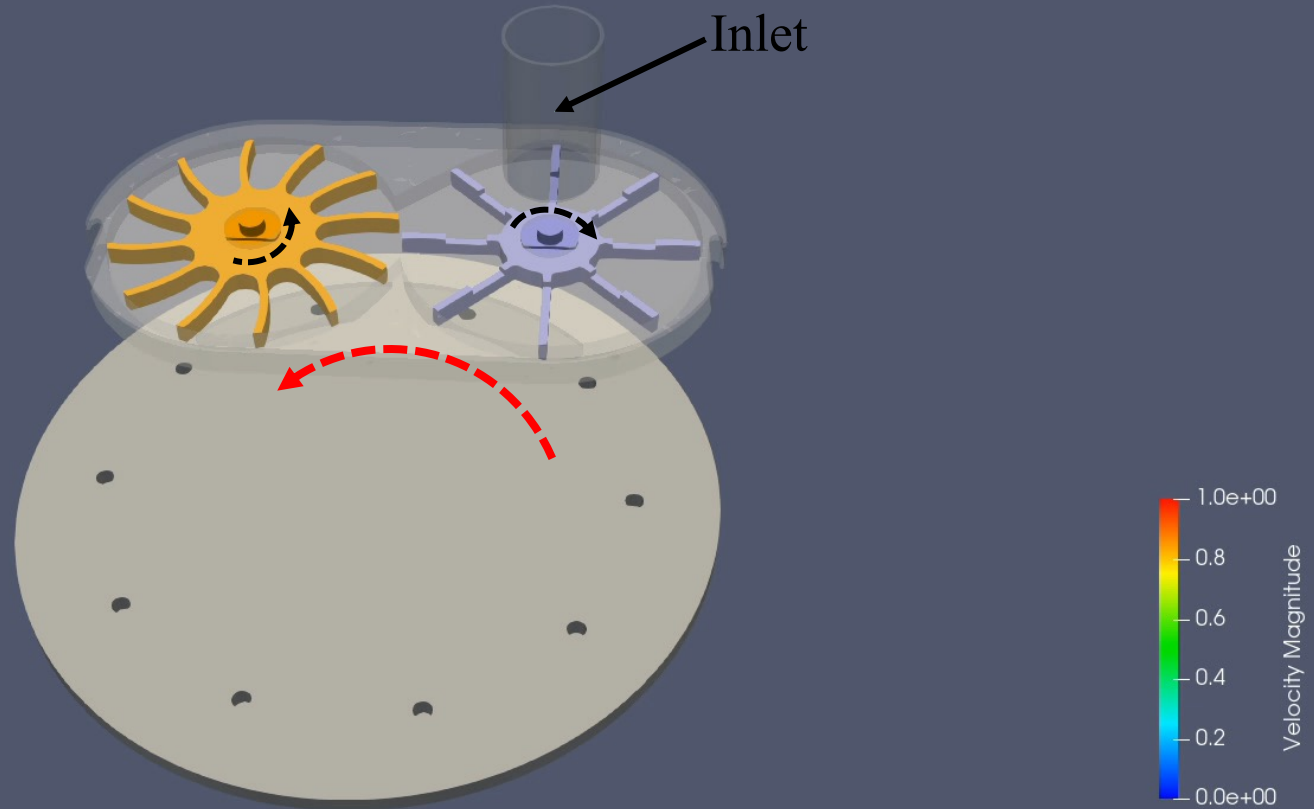


**Photos of feed frame**

# DEM modelling of the feed frame

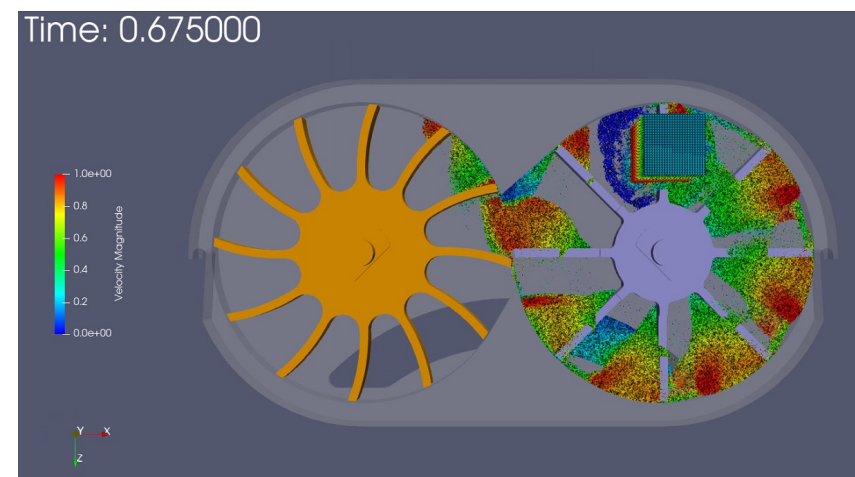
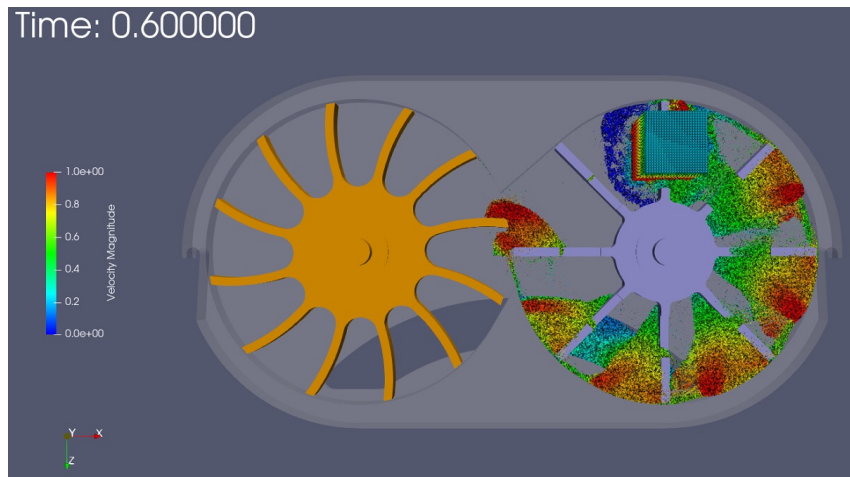
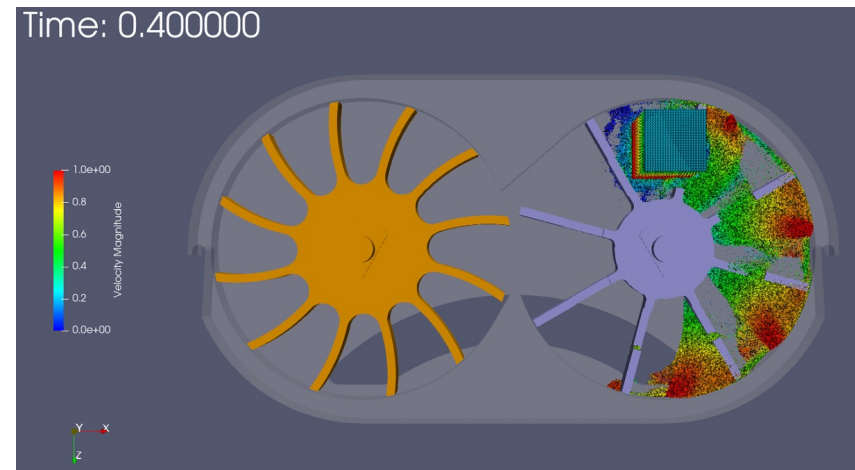
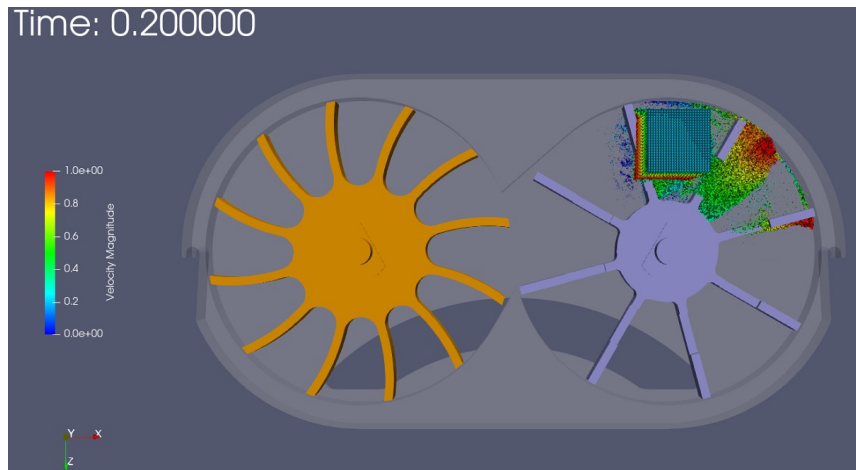
Time: 0.000000

Particle=4000k;  
Mean size=425  $\mu\text{m}$ ;  
Feeding rate=400g/s;  
Paddle1 speed=100rpm;  
Paddle2 speed=100rpm;  
Turret speed=10rpm;  
Simulation time=1.5s;



**Animation of initial DEM model for feed frame**

# Particle flow patterns



**Snapshots of powder distribution in feed frame (Top view)**

# Impact of cohesion

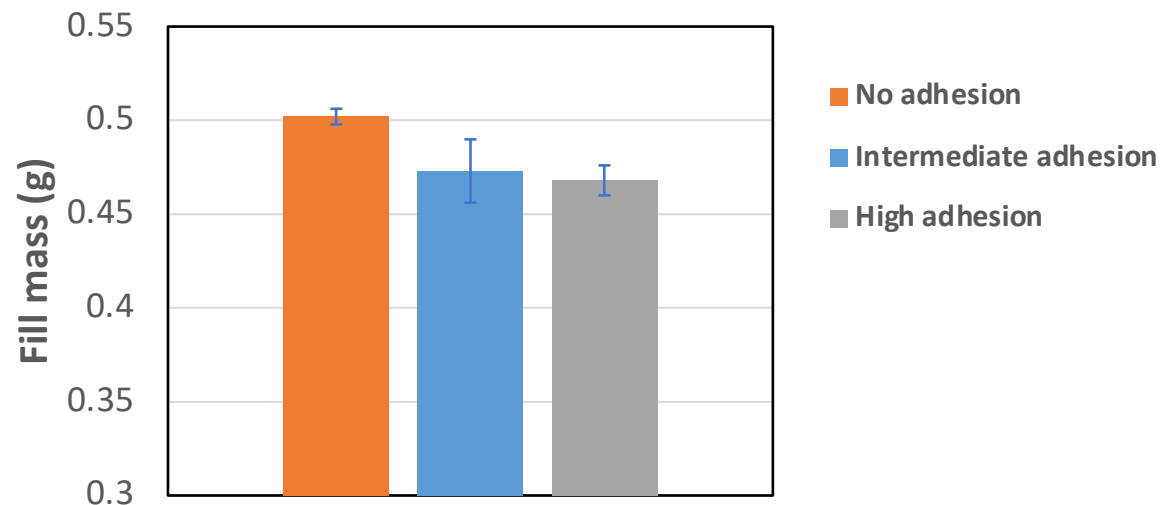
Particle size ratio	Cohesion	Turret speed (rpm)	Paddle 1 speed	Paddle 2 speed	Average mass (g)	RSD (%)	Hold-up mass (g)
1.6	intermediate	55	57.5	69	0.474	1.46	294
<b>1.6</b>	<b>No adhesion</b>	<b>10</b>	<b>15</b>	<b>18</b>	<b>0.502</b>	<b>0.83</b>	<b>293</b>
<b>1.6</b>	<b>Intermediate</b>	<b>10</b>	<b>15</b>	<b>18</b>	<b>0.473</b>	<b>3.57</b>	<b>287</b>
<b>1.6</b>	<b>High</b>	<b>10</b>	<b>15</b>	<b>18</b>	<b>0.468</b>	<b>1.71</b>	<b>278</b>

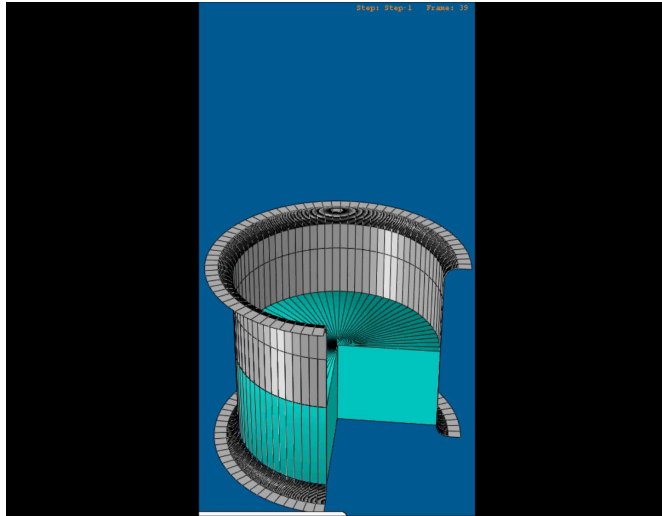
Cohesion number

$$= \frac{\text{Work of cohesion}}{\text{Gravitational potential energy}}$$

$$Coh = \frac{1}{\rho g} \left( \frac{\Gamma^5}{E^{*2} R^{*8}} \right)^{1/3}$$

$$\Gamma_2 = \Gamma_1 \left( \frac{R^*_2}{R^*_1} \right)^{8/5}$$

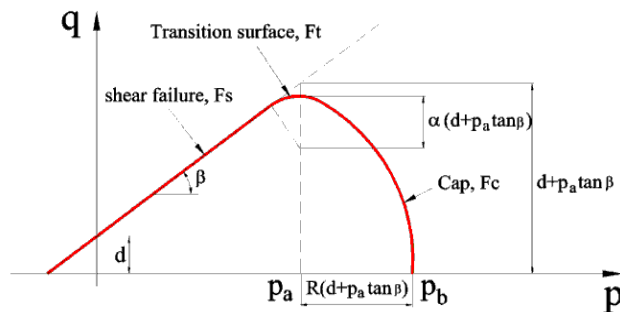




**Powder is regarded as continuum elastic-plastic media.**

Compaction behaviour is modelled by solving a boundary value problem, i.e. partial differential equations representing:

- Balance laws (mass, energy, momentum);
- Constitutive laws (stress-strain, friction).



**Drucker-Prager-Cap model**

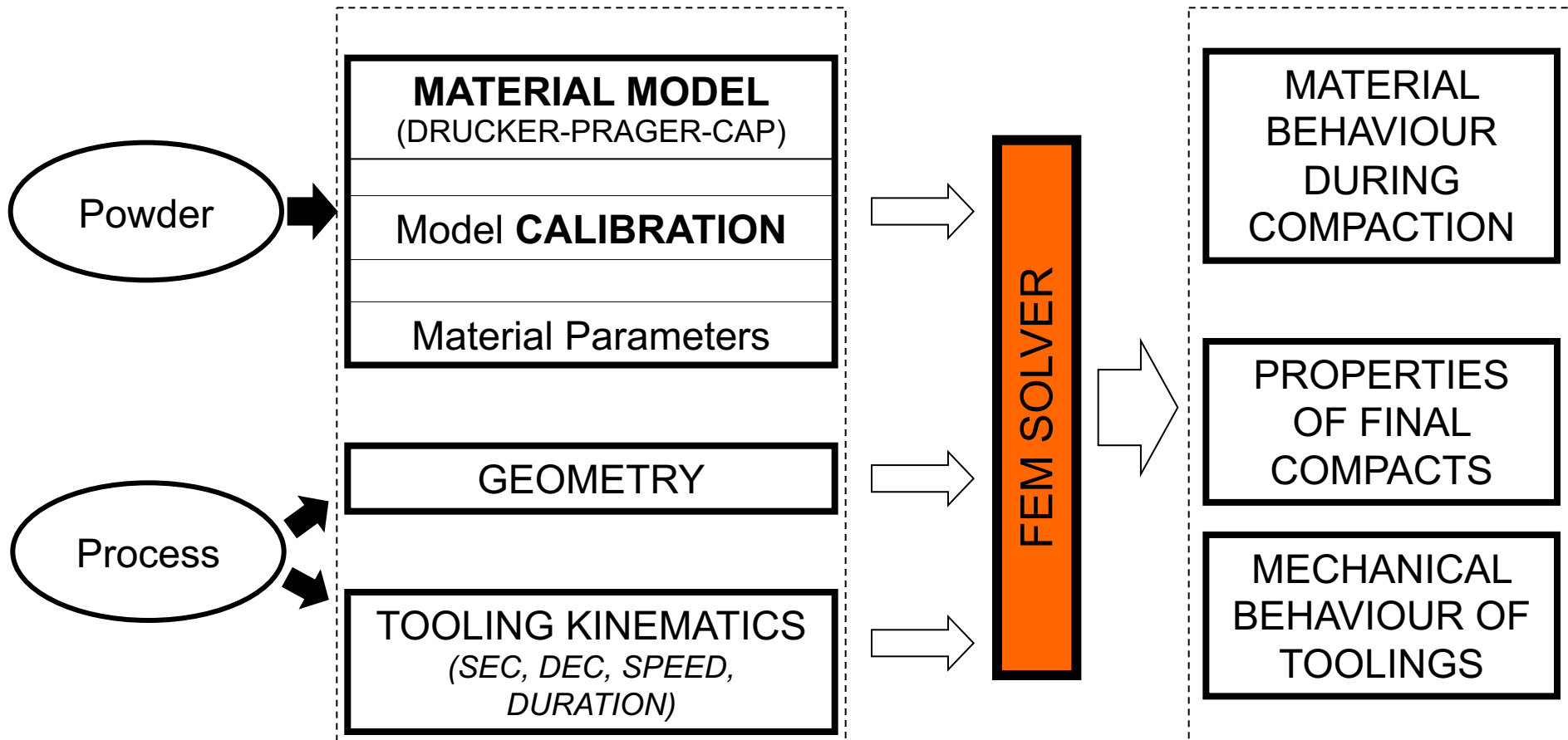
## **Drucker-Prager-Cap model:**

- A reasonable representation of the powder behaviour.
- Easy for numerical implementation and experimental calibration.
- Widely used for metallic and ceramic powders.
- Recently for pharmaceutical powders (Michrafy 2002; Sinka 2001, 2002, Wu et al. 2005,2008, Frenning et al. 2007).

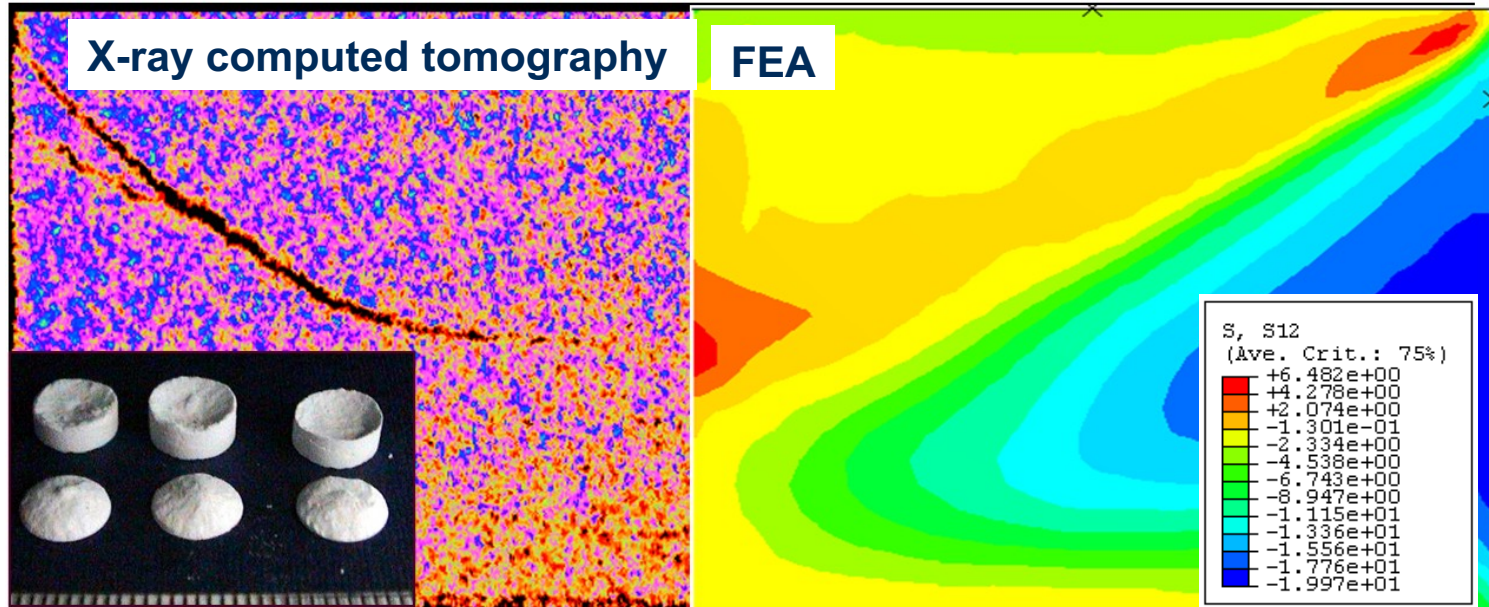
# Finite Element Modelling of Powder Compaction

## INPUT

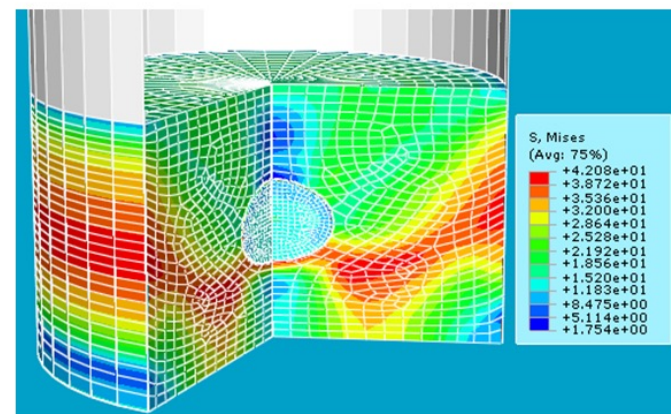
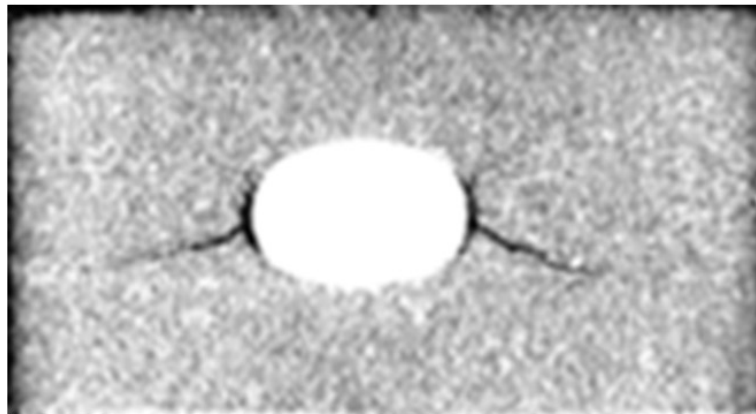
## OUTPUT



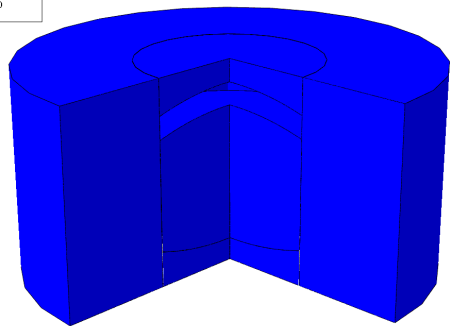
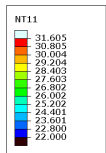
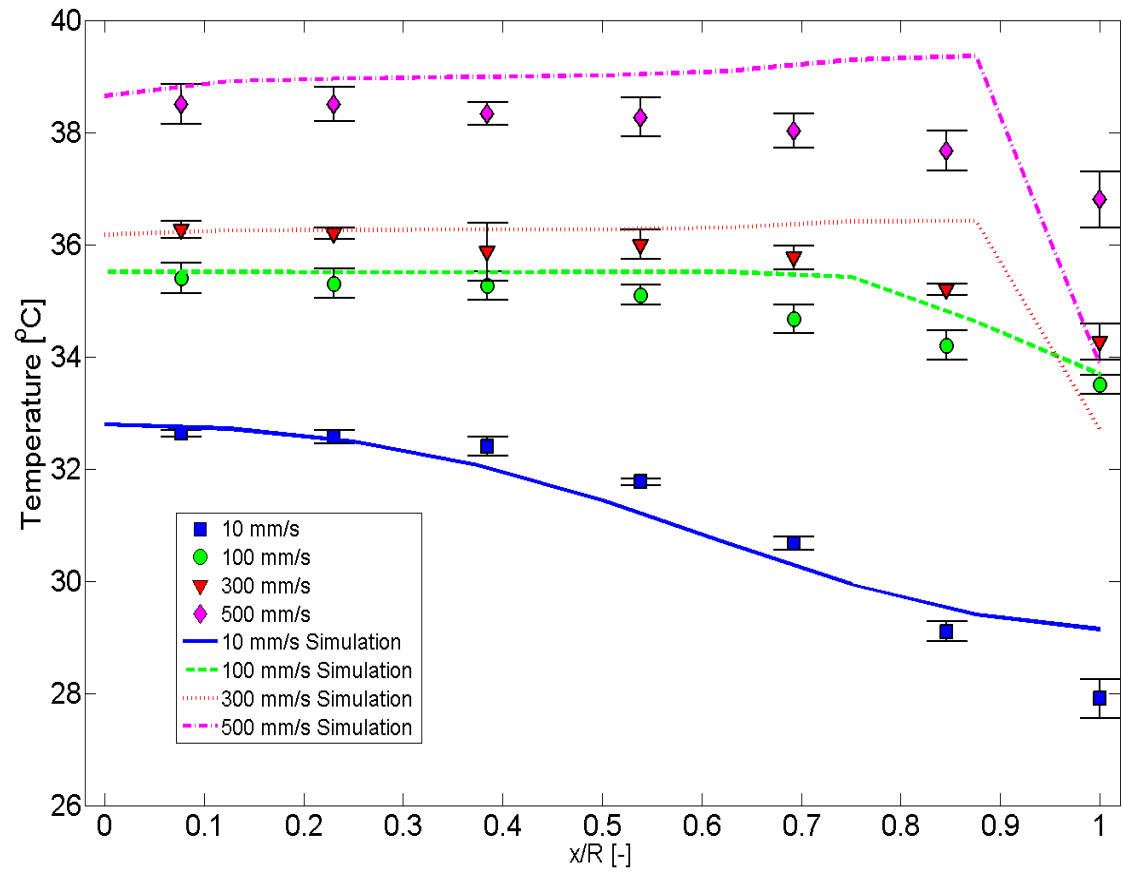
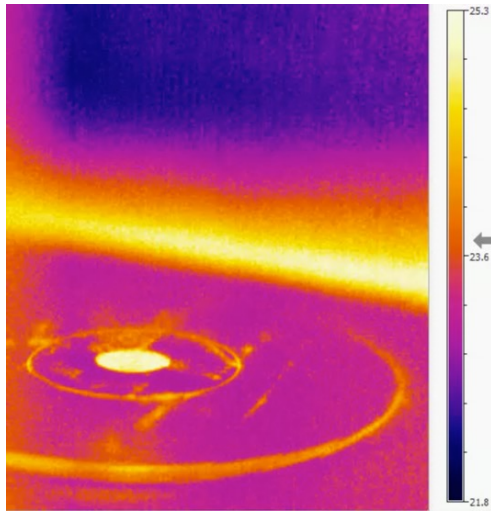
# Indicating problems associated with manufacturing



Wu C.Y., Ruddy O., Bentham A.C., Hancock B.C., Best S.M. and Elliott J.A. (2005), "Modelling the mechanical behaviour of pharmaceutical powders during compaction". *Powder Technology*, 152(1-3):107-117

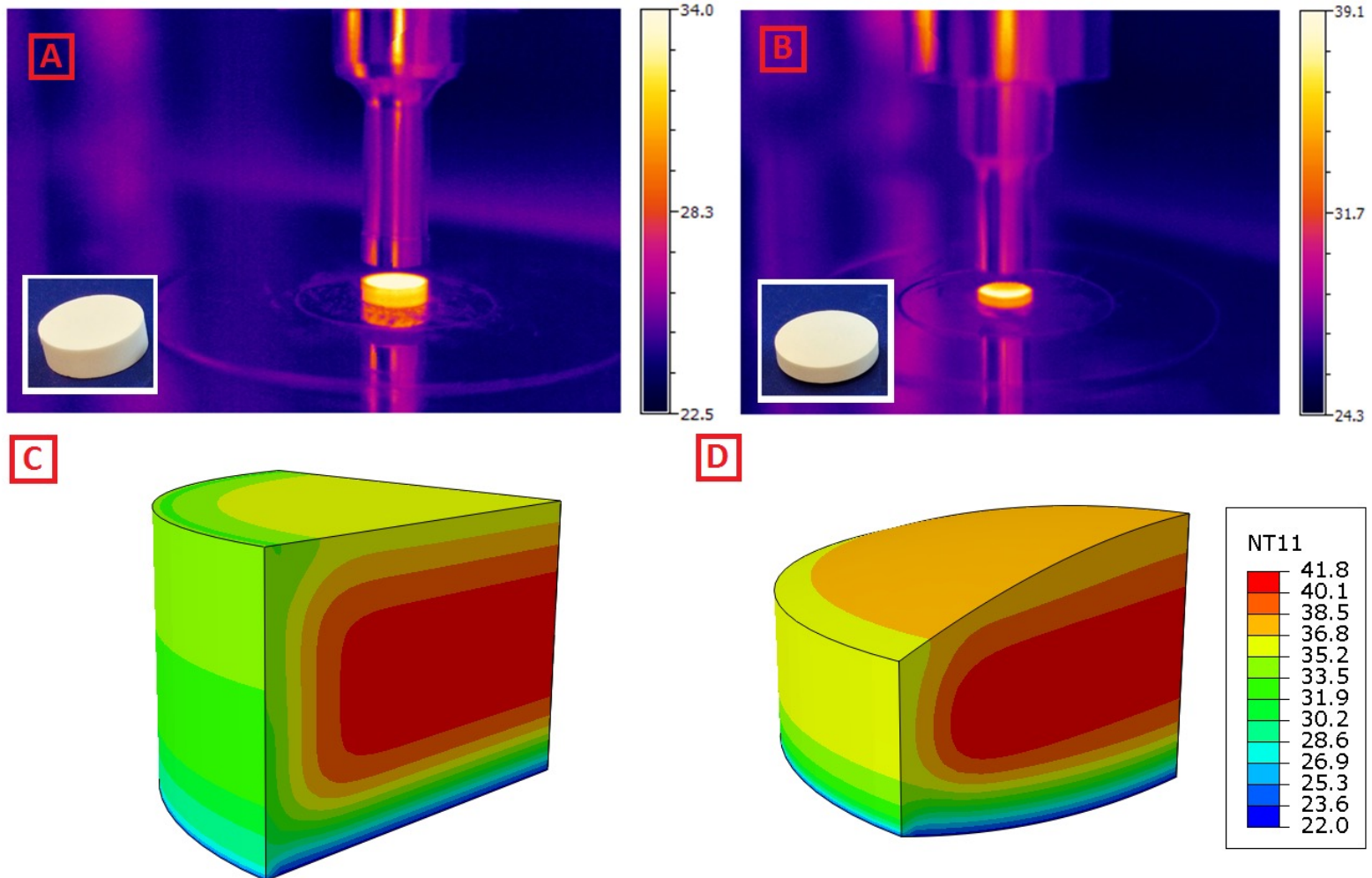


# Heat Generation and temperature rise



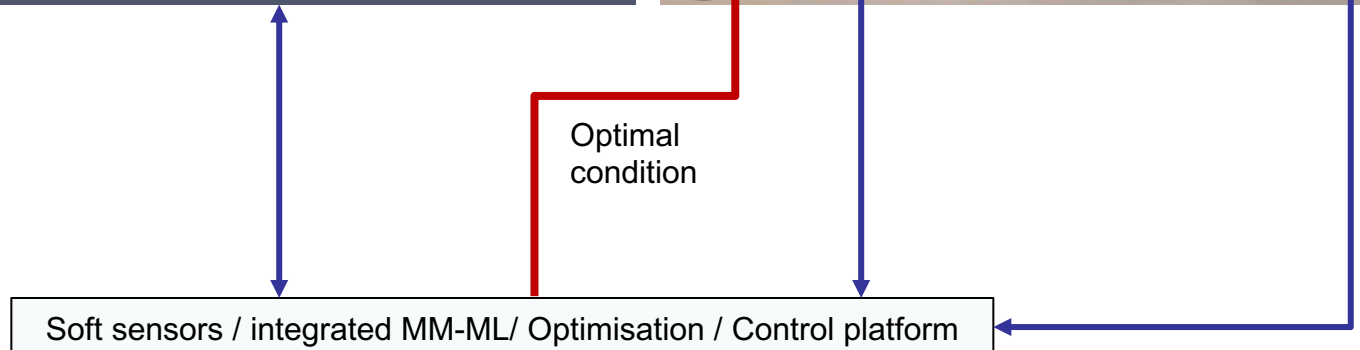
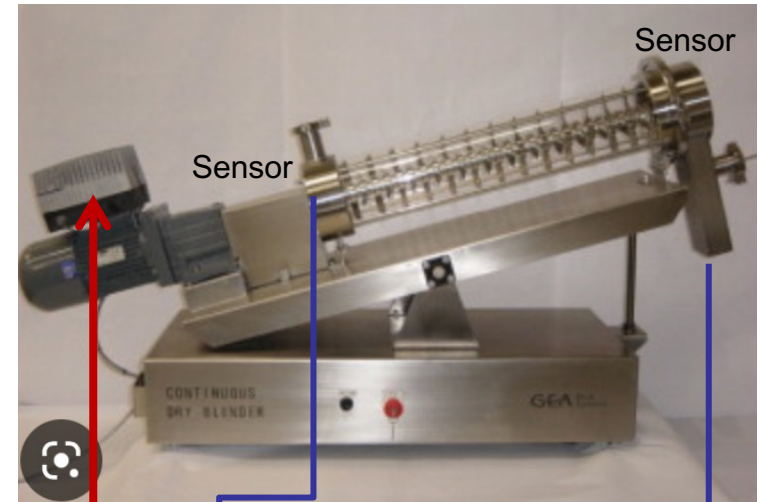
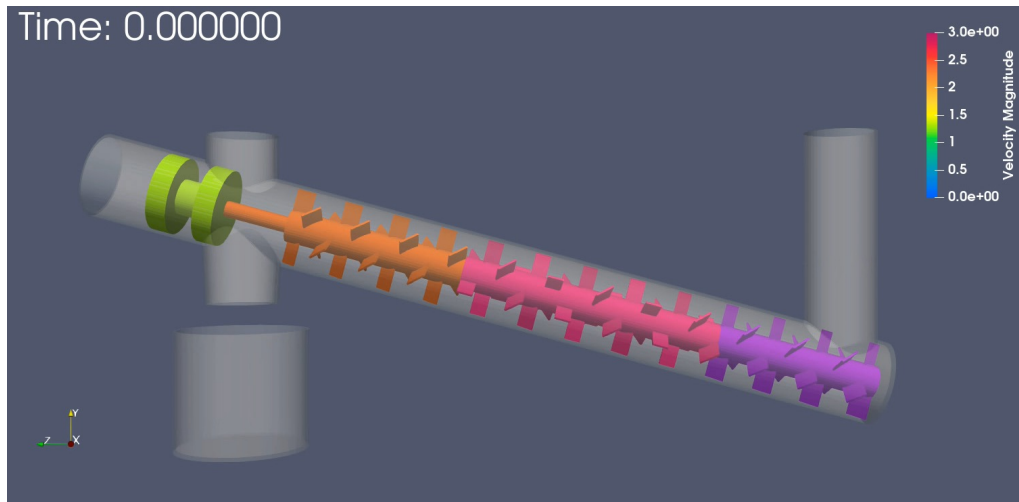


# Heat Generation and temperature rise



# Towards Digital Twins

- ❑ Rapid decision-making
- ❑ High fidelity



## **Strengths:**

- ❑ Accurate representation of underlying physical and chemical processes.
- ❑ Enables a deep understanding of the system's behavior and interactions.
- ❑ Well-defined parameters allow for precise predictions and control.

## **Limitations:**

- ❑ Complexity in incorporating all variables and interactions.
- ❑ Parameter identification are often extensive.
- ❑ Difficulty in adapting to new scenarios or system changes without significant re-calibration.

# Remarks & Perspectives

- ❑ Duly consideration of different mechanical behaviours of powders at various process stages is essential in applying different computational methods.
- ❑ **Mechanistic modelling is versatile with wide applications** in mixing, conveying, powder flow, die filling and tableting.
- ❑ Great potential to **integrate these methods with ML for pharmaceutical formulation development.**
- ❑ **Open Data** with robust data infrastructure will significantly enhance the deployment of AI in pharmaceutical product development
- ❑ Computational tools will play an important part in pharmaceutical manufacture of the future: Digital twins, Pharm 4.0, continuous manufacturing, etc.

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