

On the AI driven geometry optimisation of a stirred tank CFD model in laminar flow

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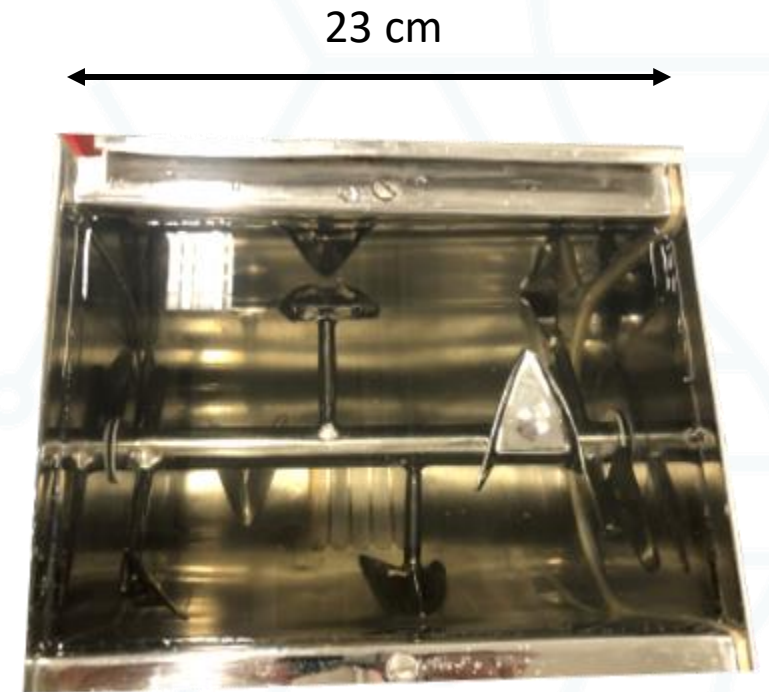
[1] School of Chemical Engineering, University of Birmingham.
[2] Hindustan Unilever R&D, Bangalore.
[3] Unilever R&D, Port Sunlight Laboratory.

Industrial mixing in a Ploughshare mixer

- Used in semi-solid and granular mixing.
- Poor axial mixing demonstrated for granulation [1-3]
- How to predict and improve viscous mixing?

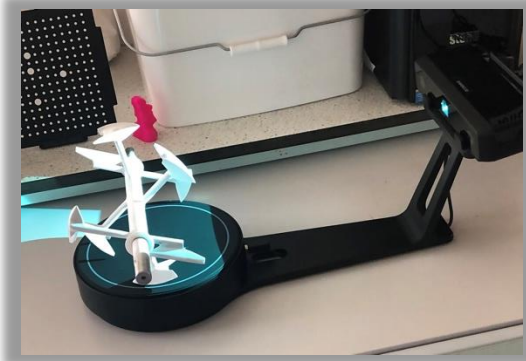
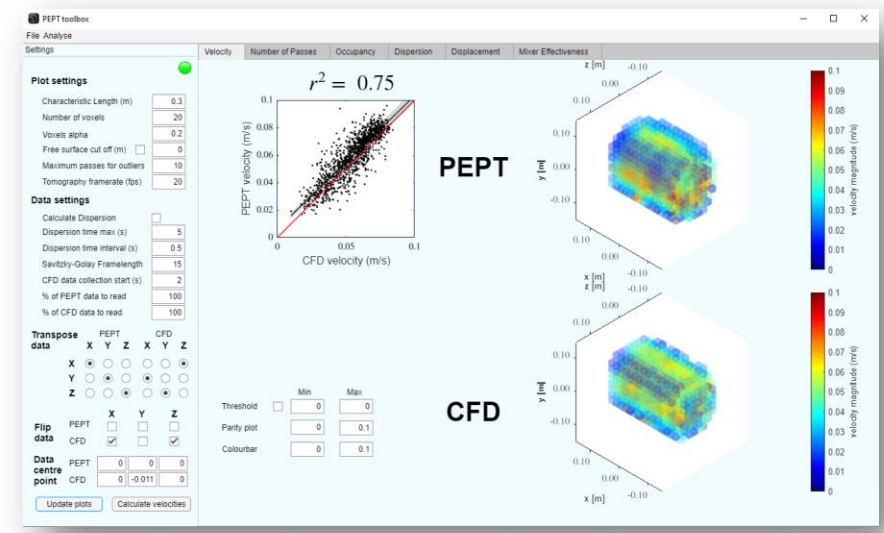
Aims

1. Build a **CFD** model to predict single-phase liquid mixing.
2. **Validate** mixing using Positron Emission Projection Imaging.
3. Develop **predictive models** for mixing.
4. Optimise impeller geometry with a **data-driven** approach.

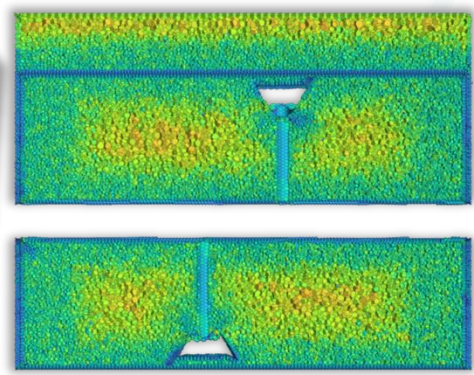
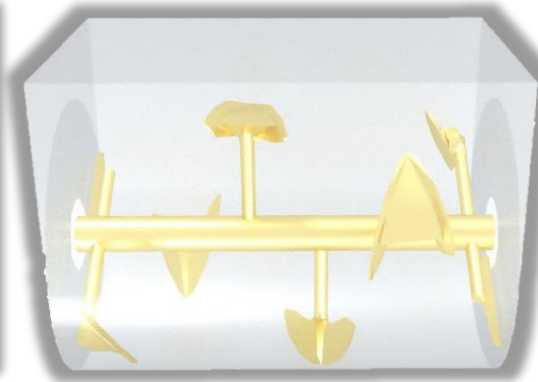


CFD model

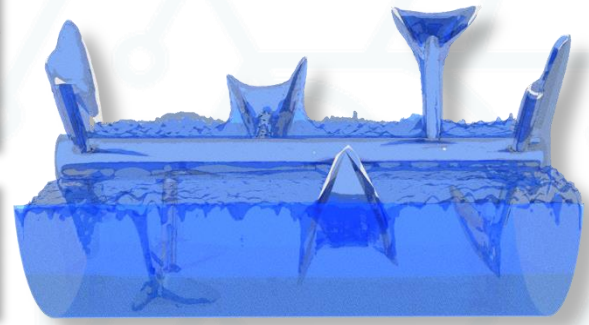
- Viscous mixing in laminar flow
- Sliding mesh, single-phase liquid.
- Velocity fields validated using PEPT in previous work [4]
- **Passive scalar tracers** used to predict mixing performance.



3d scanned impeller



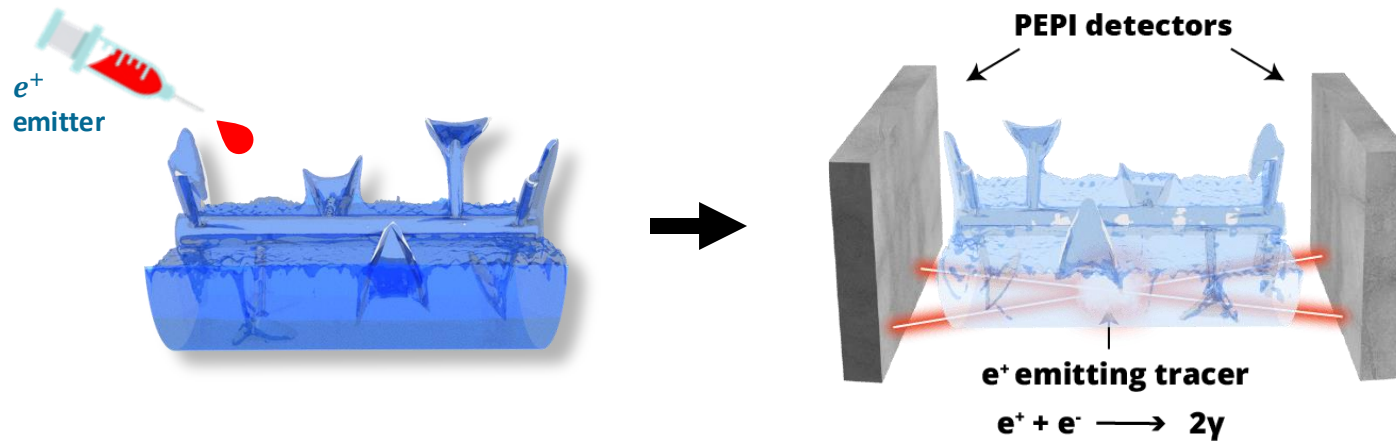
1.1 M cells



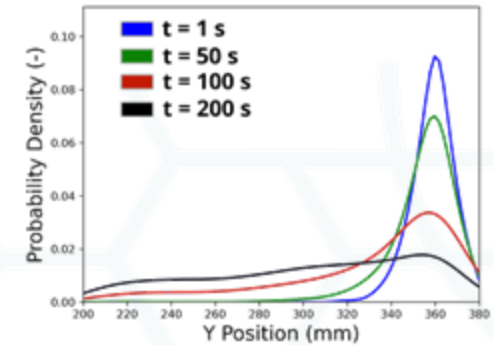
[4] Hart-Villamil, R., et al 2024. On the autonomous validation and comparison of particle models for a Newtonian laminar flow mixing model using PEPT. Chemical Engineering Research and Design 206, 139–150.

What is Positron Emission Projection Imaging (PEPI)?

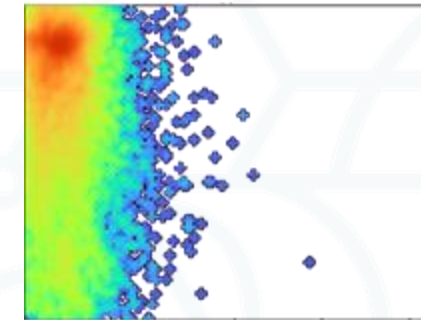
- Direct tracking of **species concentration** using gamma photons.
- It allows us to **'see inside' opaque systems**.
- ~ 2 mm spatial and ~1 s temporal resolution



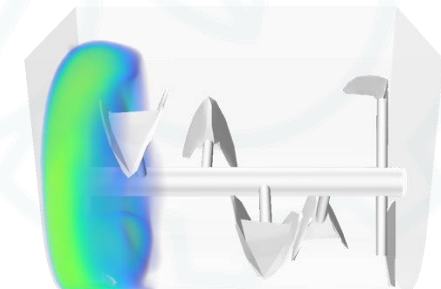
Mass distributions



Concentration fields



In-silico comparison



Validating the simulation

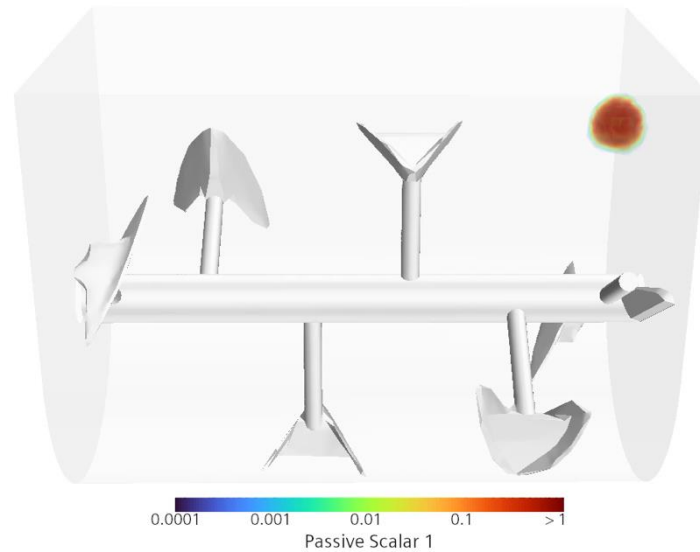
Glycerol in laminar flow

$N = 33 \text{ rpm}$

$\mu = 1.4 \text{ Pa s}$

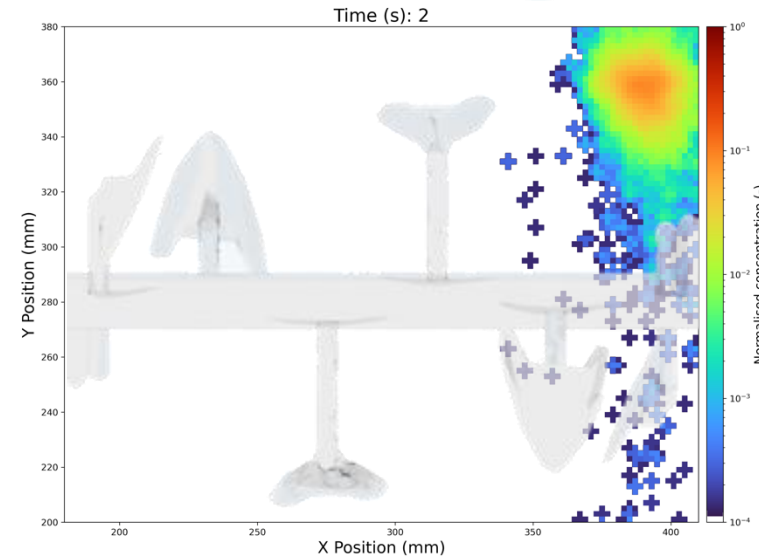
$\rho = 1256 \text{ kg m}^{-3}$

$Re = 10$



Solution Time 0.04 (s)

CFD model

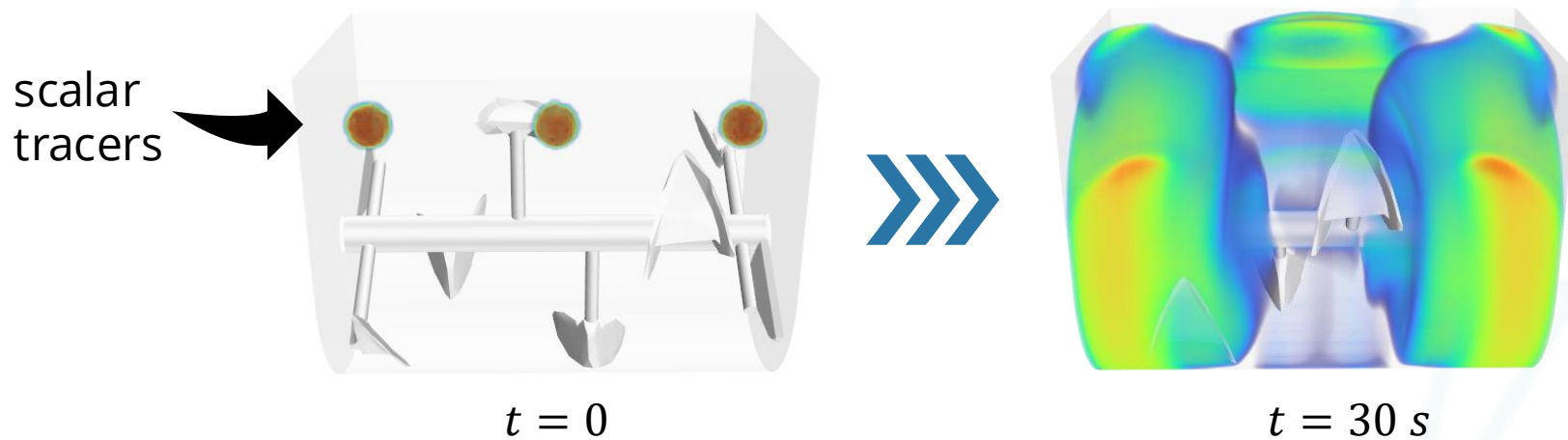


Positron Emission Projection Imaging

Exploring how ρ N K n Impacts Torque, Mixing

rotation rate \rightarrow N \leftarrow flow index
density \rightarrow ρ \leftarrow flow consistency n

- 60 parameter combinations sampled with Latin Hypercube



Equation discovery via symbolic regression

- Similar functionality to ANNs, but not a “black box”
- Closed-form mathematical equations
- Improved understanding
- Reduced dimensionality means almost **zero inference costs**



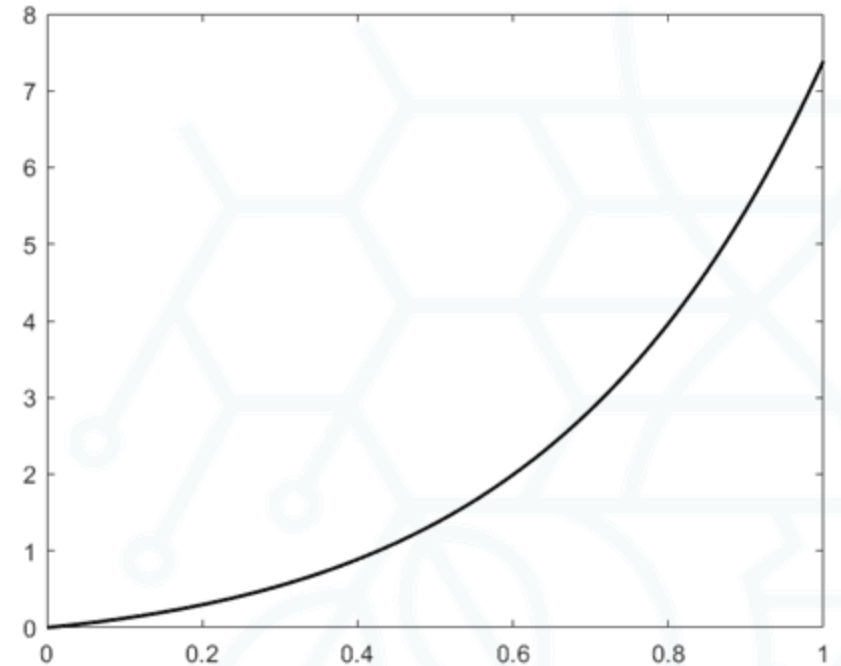
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$$f_1(x) =$$

$$f_2(x) =$$

a x x^α $e^{\alpha x}$ $\sin \alpha x$ $\cos \alpha x$ $\tan \alpha x$ $\log \alpha x$ $\ln \alpha x$

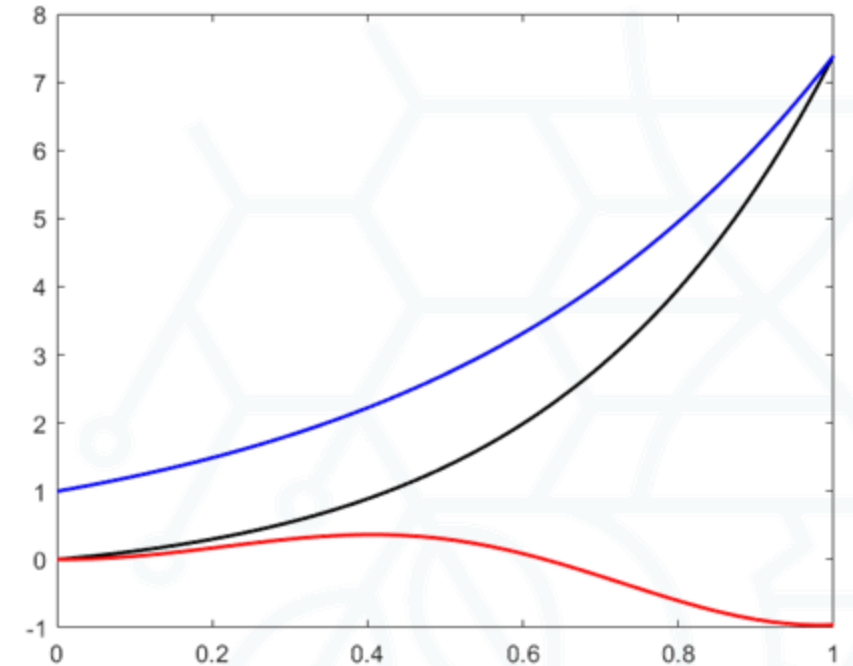


Equation discovery via symbolic regression

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$$f_1(x) = x \sin \alpha x$$

$$f_2(x) = a e^{\alpha x}$$



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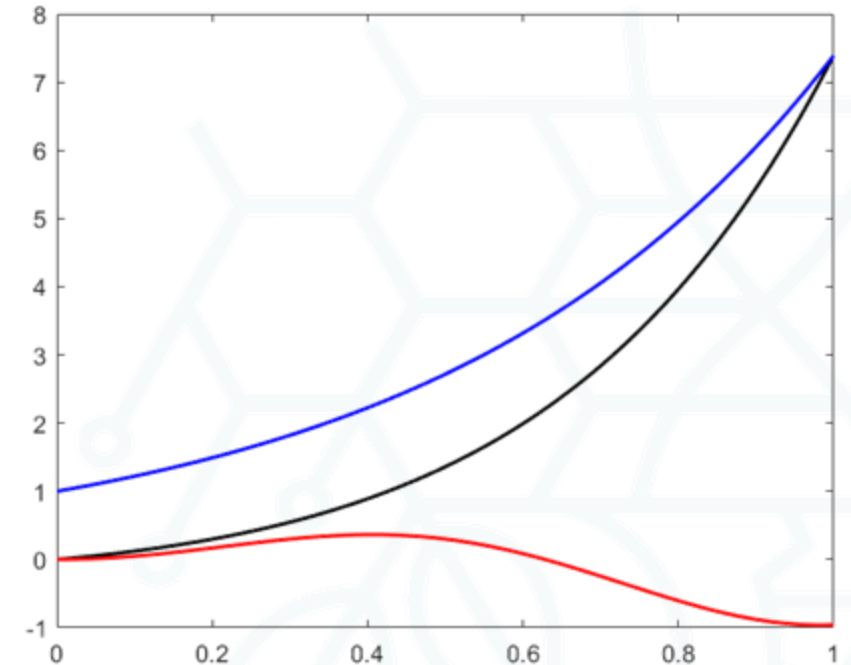
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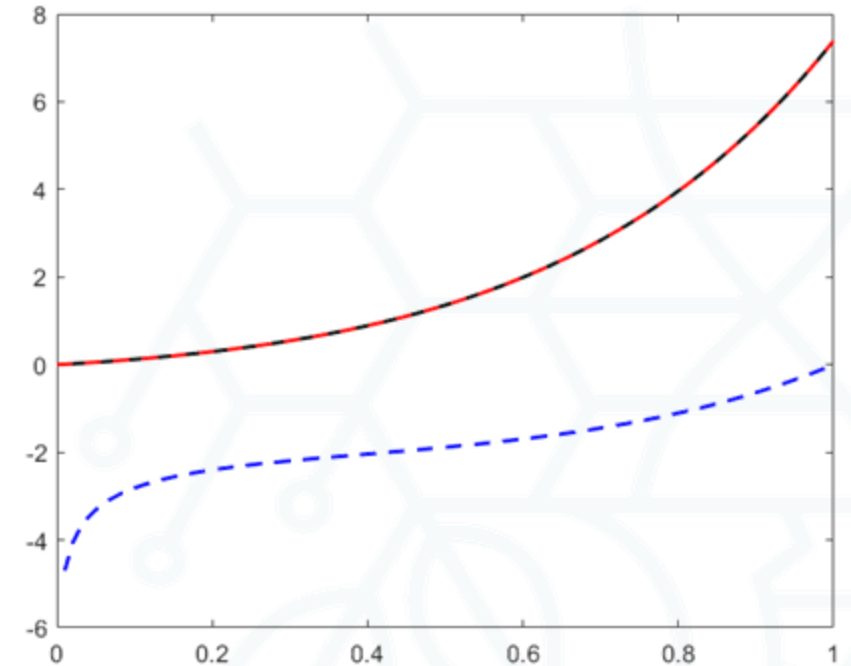
~~$f_1(x) =$~~

$f_2(x) = a e^{\alpha x}$

$f_3(x) = a x e^{\alpha x}$

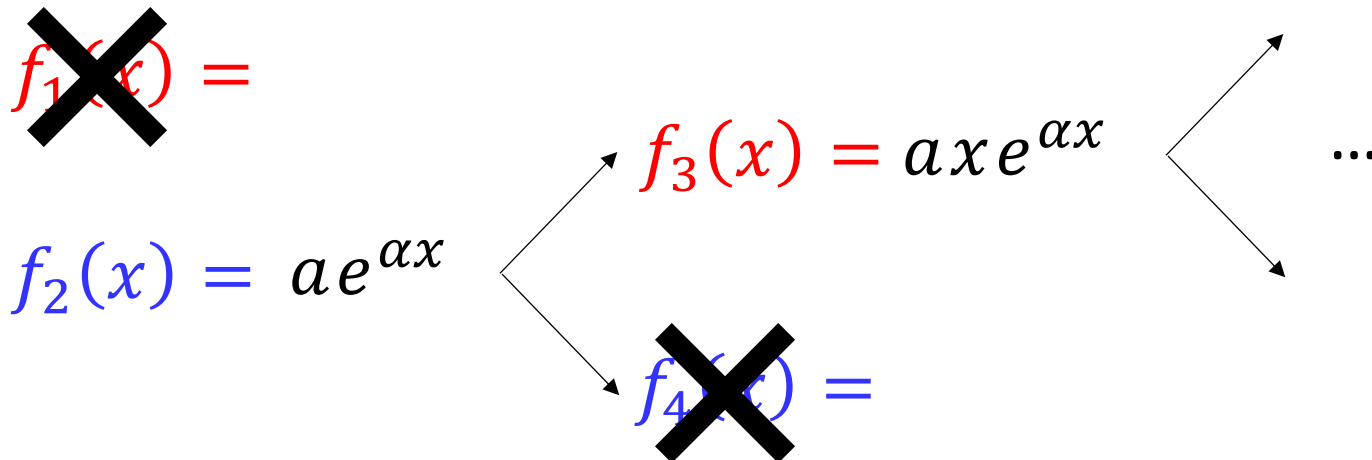
$f_4(x) = \ln \alpha x e^{\alpha x}$

a x x^α $e^{\alpha x}$ $\sin \alpha x$ $\cos \alpha x$ $\tan \alpha x$ $\log \alpha x$ $\ln \alpha x$

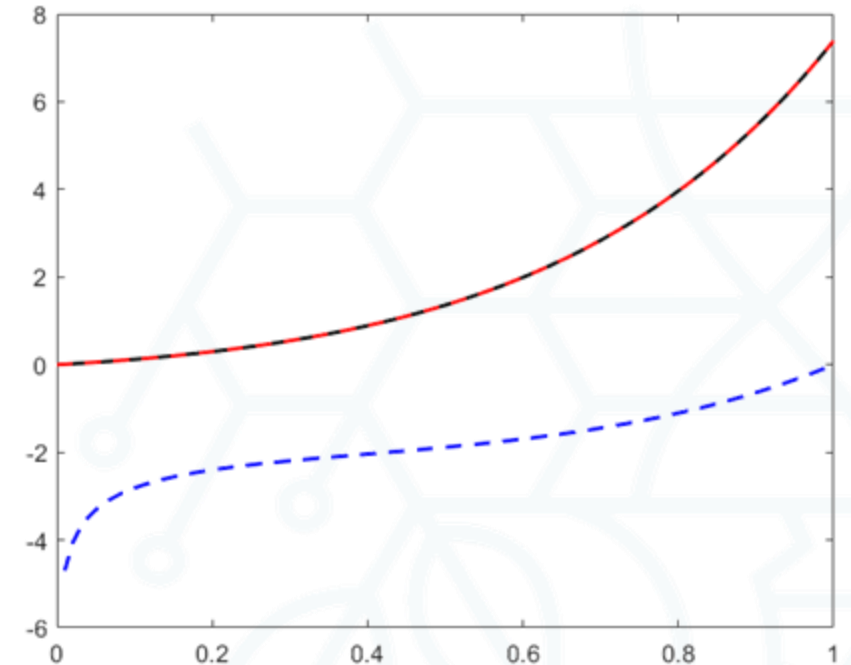


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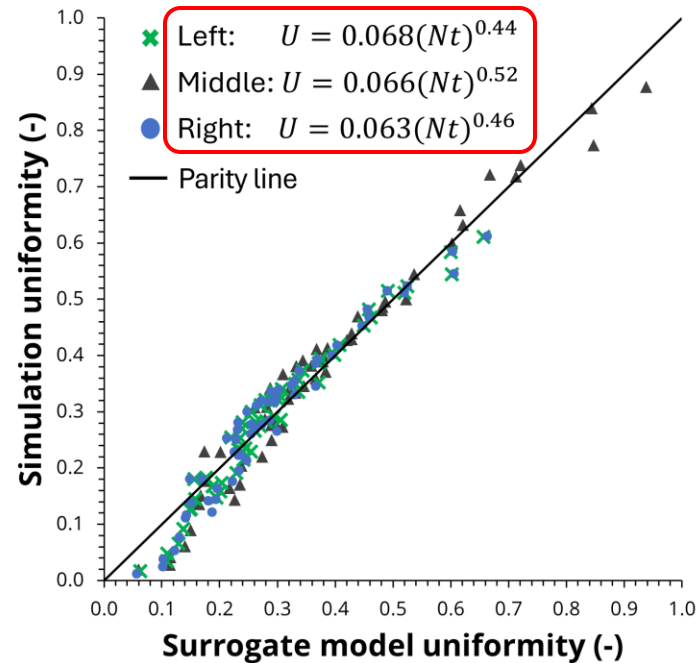
Exploring how ρ N K n Impacts Torque, Mixing

left $Nt_m = 401$ revs
 middle $Nt_m = 169$ revs
 right $Nt_m = 365$ revs

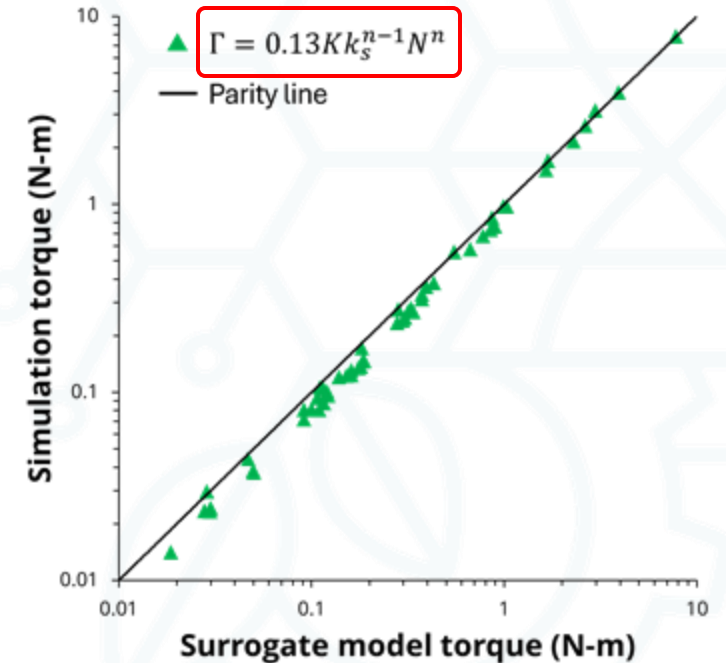
$$W_m = \frac{0.13Kk_s^{n-1}N^{n+1}t_m}{\rho V}$$

↙ Mixing energy

Mixing parity plot



Torque parity plot



[6] Tatterson, 1991. Fluid Mixing and Gas Dispersion in Agitated Tanks, McGraw-Hill, New York.

[7] Kresta, S. M., et al 2016. Advances in Industrial Mixing. John Wiley & Sons.

[8] Metzner, A. B., Otto, R. E., 1957. Agitation of non-Newtonian fluids. AIChEJ., 3: 3-10.

[9] Nicusan 2023. MEDEq Library. <https://med.readthedocs.io>

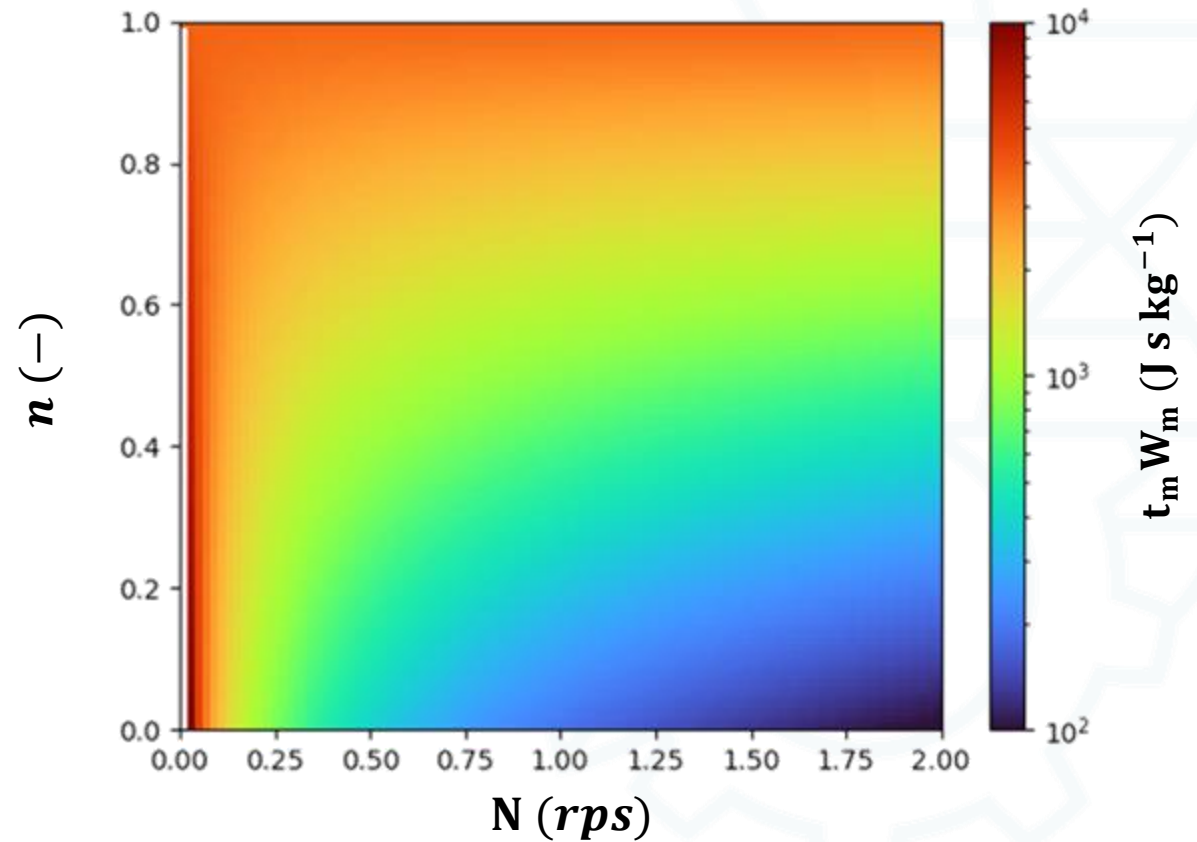
[10] Laplante, P. et al 2015. Demulsifier performance in froth treatment. Fuel Processing Technology, 138: 361-367.

Exploring how ρ N K n Impacts Torque, Mixing

What conditions for fastest mixing at lowest energy?

- Operate at $\min(t_m \times W_m)$
- For **Newtonian** liquid there are equal trade-offs.
- If more **shear-thinning**, better to increase rpm.

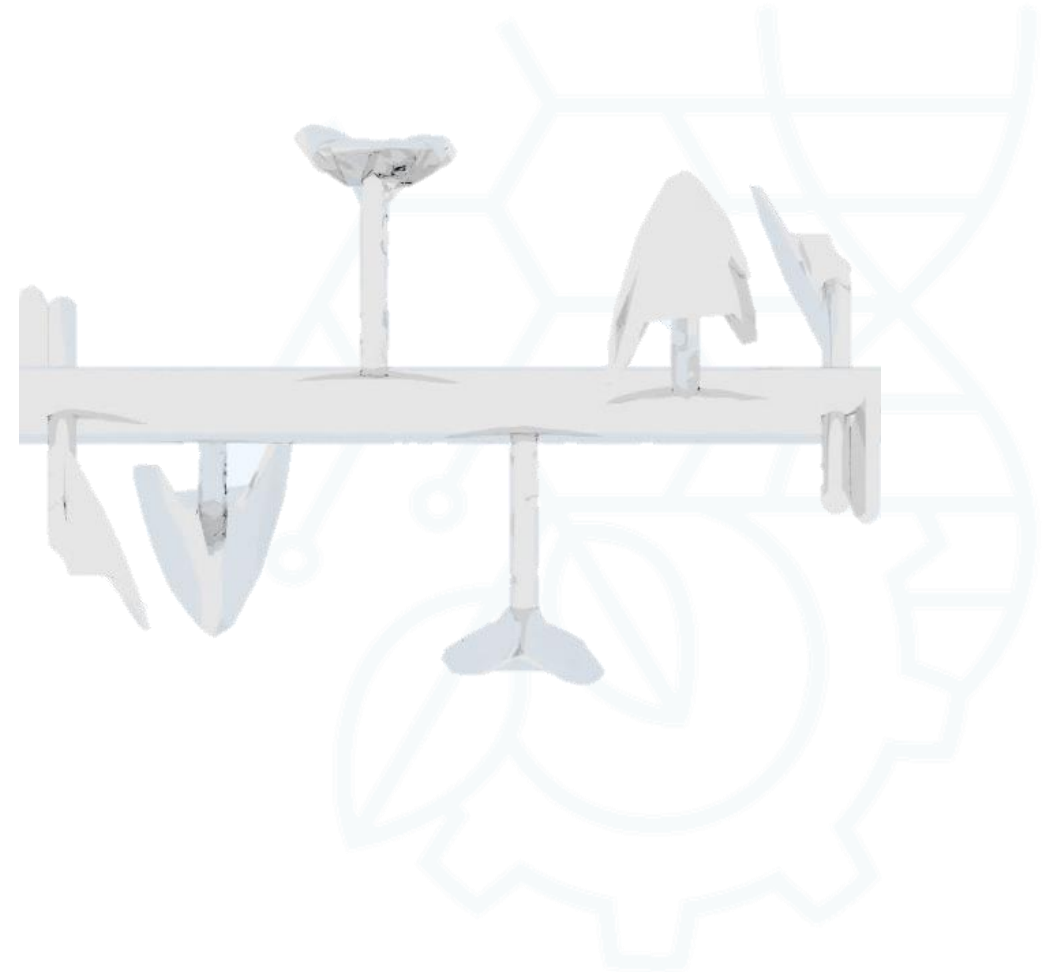
But what if you **can't** increase rotation rate or change fluid?



Optimisation

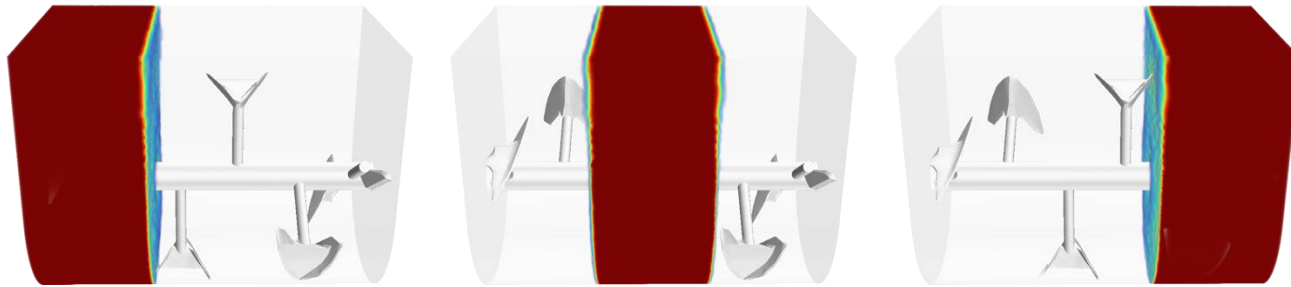
Objectives

- Maximise **axial mixing**
- Modify **geometry** using evolutionary algorithms
- Retain **plough-like** features



Optimisation

- Evaluating axial mixing

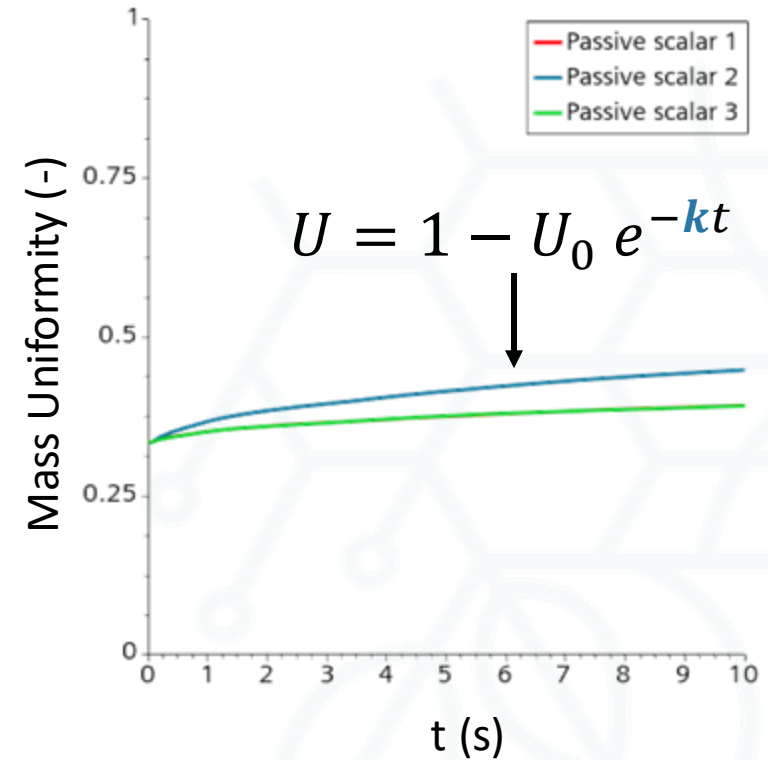


Maximise rate constant k

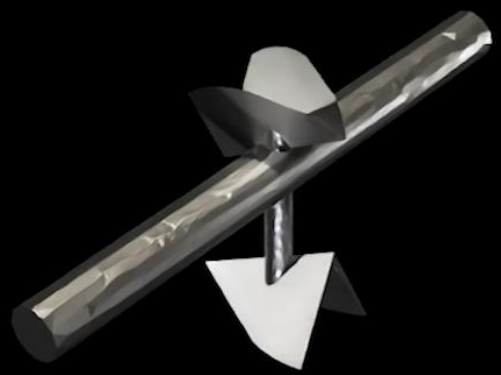
Error
function



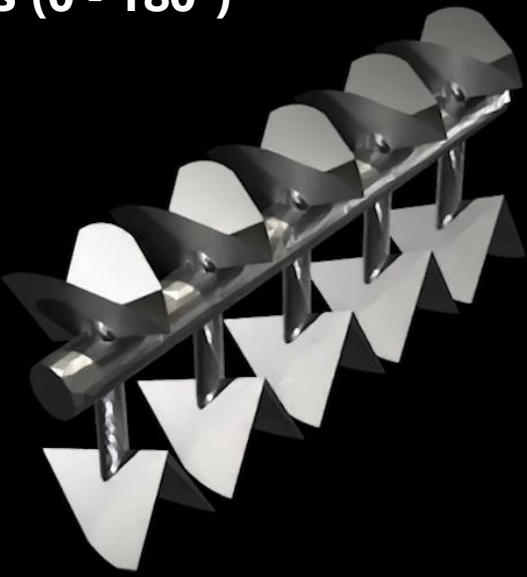
$$\text{Minimise } t_{1/2} = \frac{\ln 2}{k}$$



Number of plows (1-12)



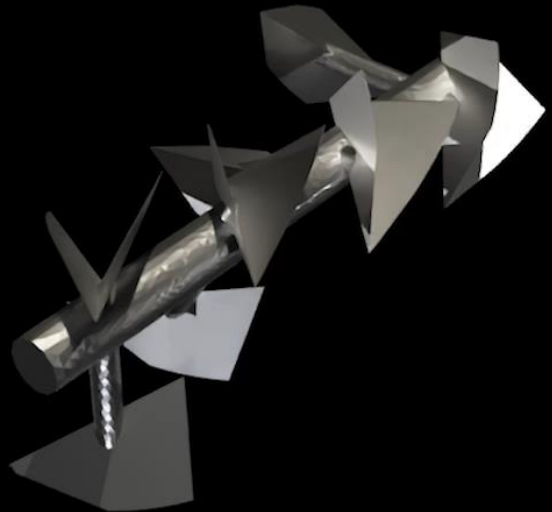
Bias (0 - 180°)



Side angle (-45 - 45°)



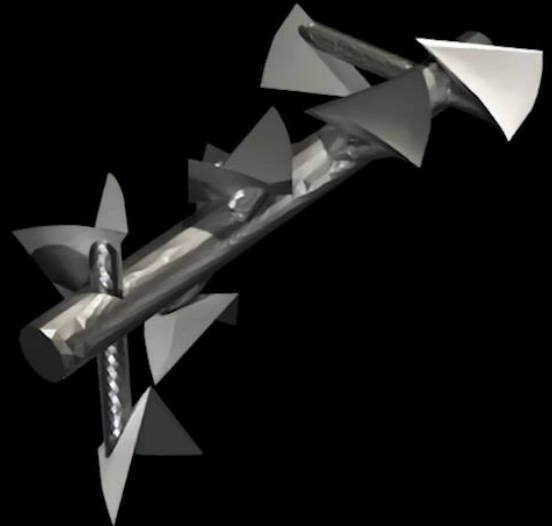
Twist angle (-45 - 45°)



Plough top height (-15 - 50 mm)

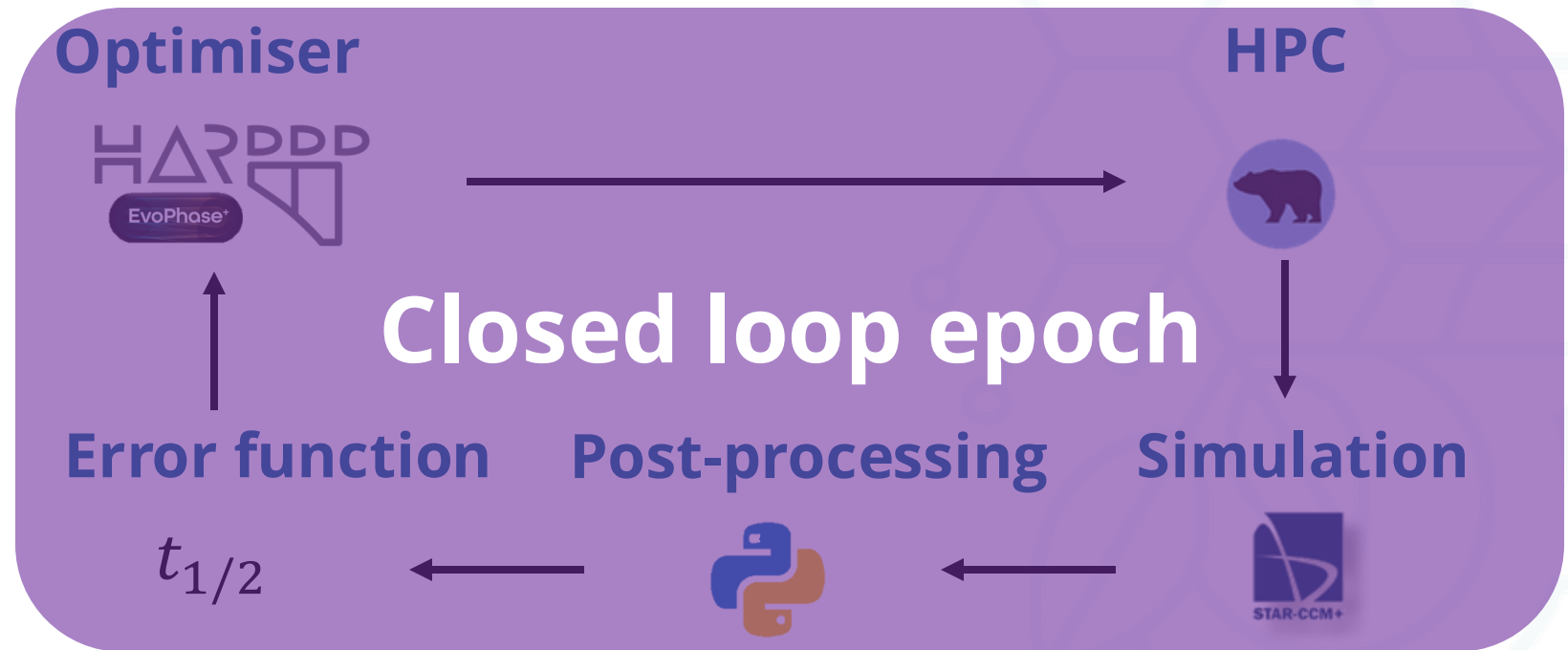
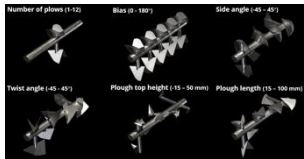


Plough length (15 - 100 mm)

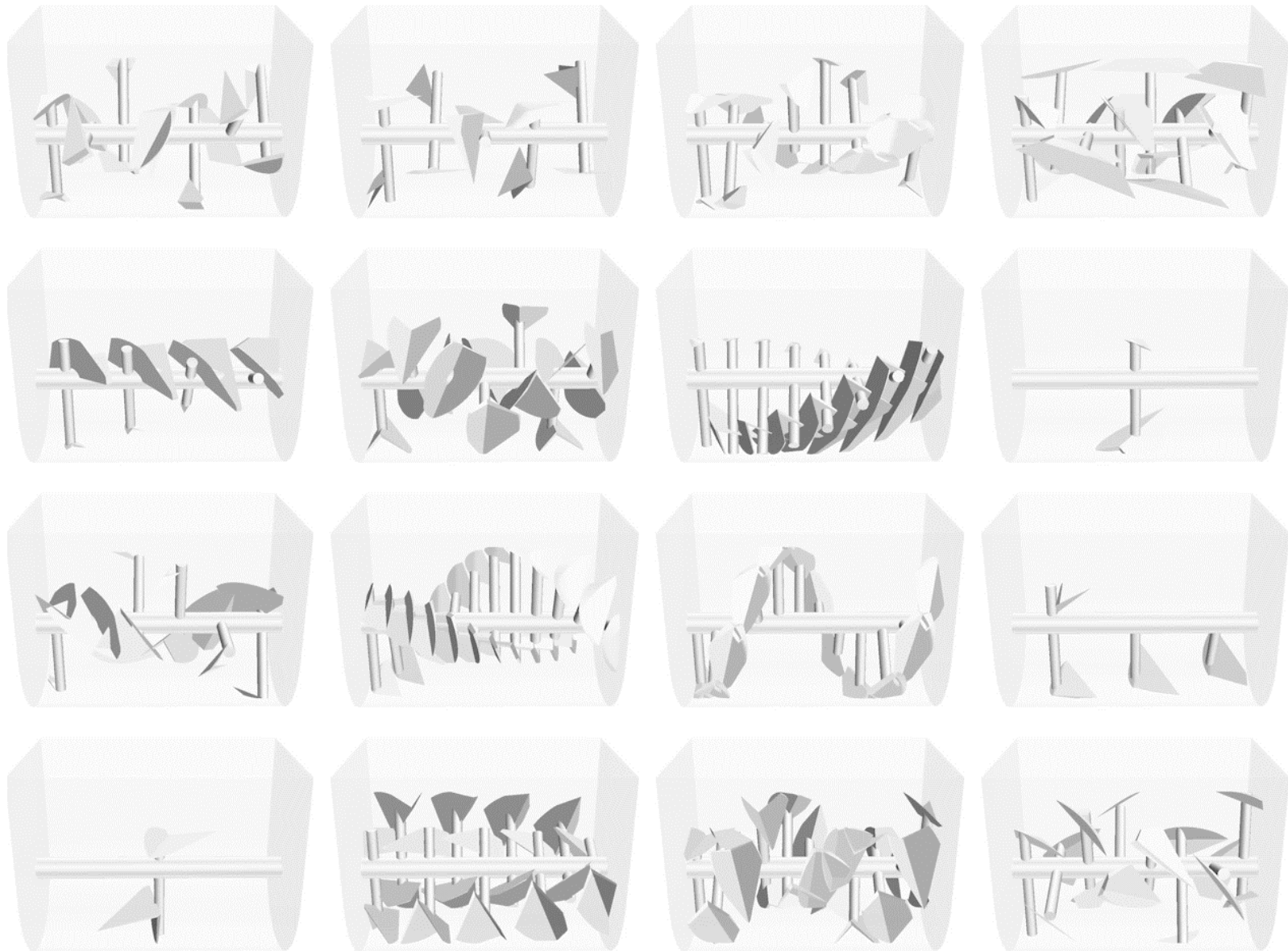


Optimisation

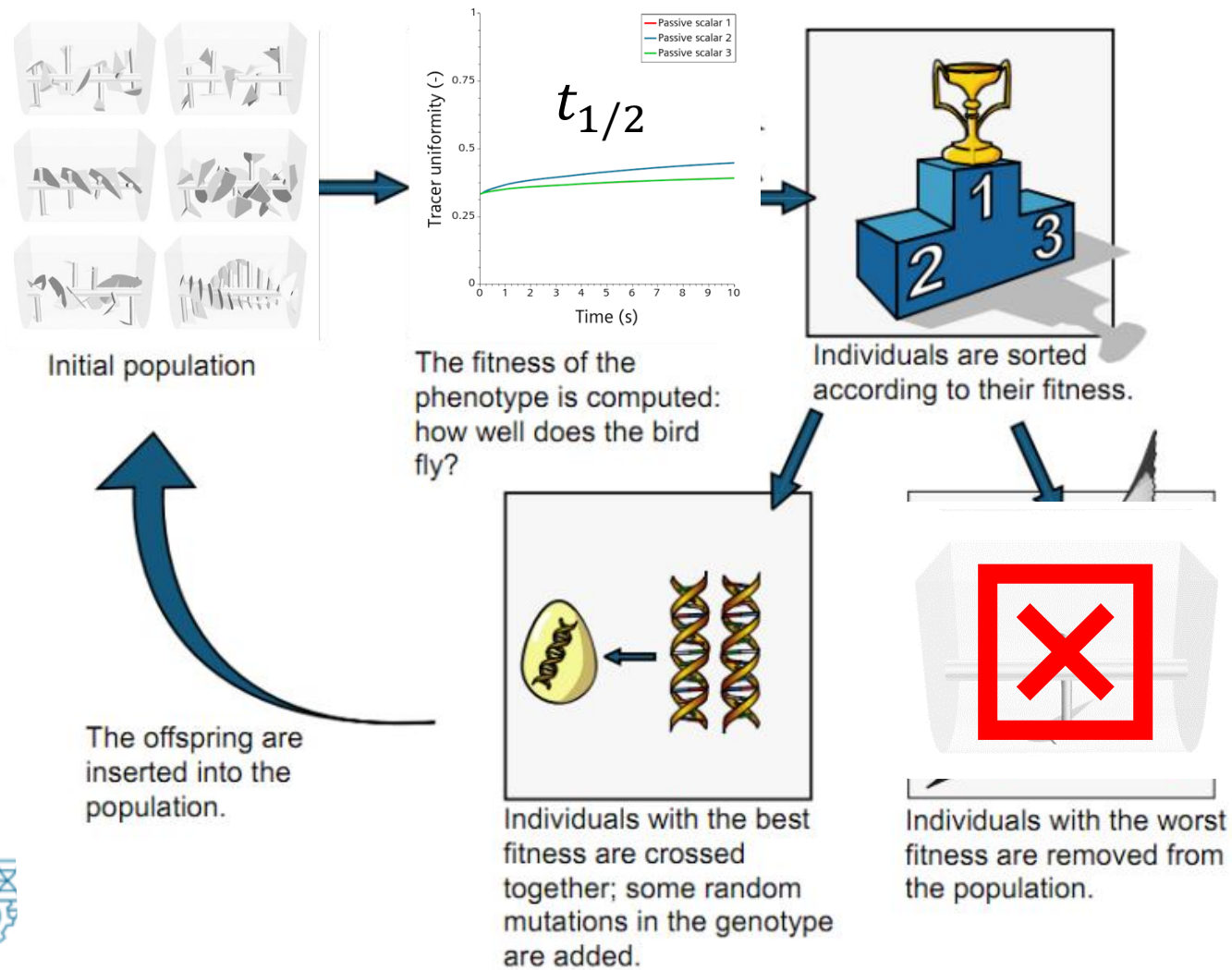
Input parameters



Optimisation

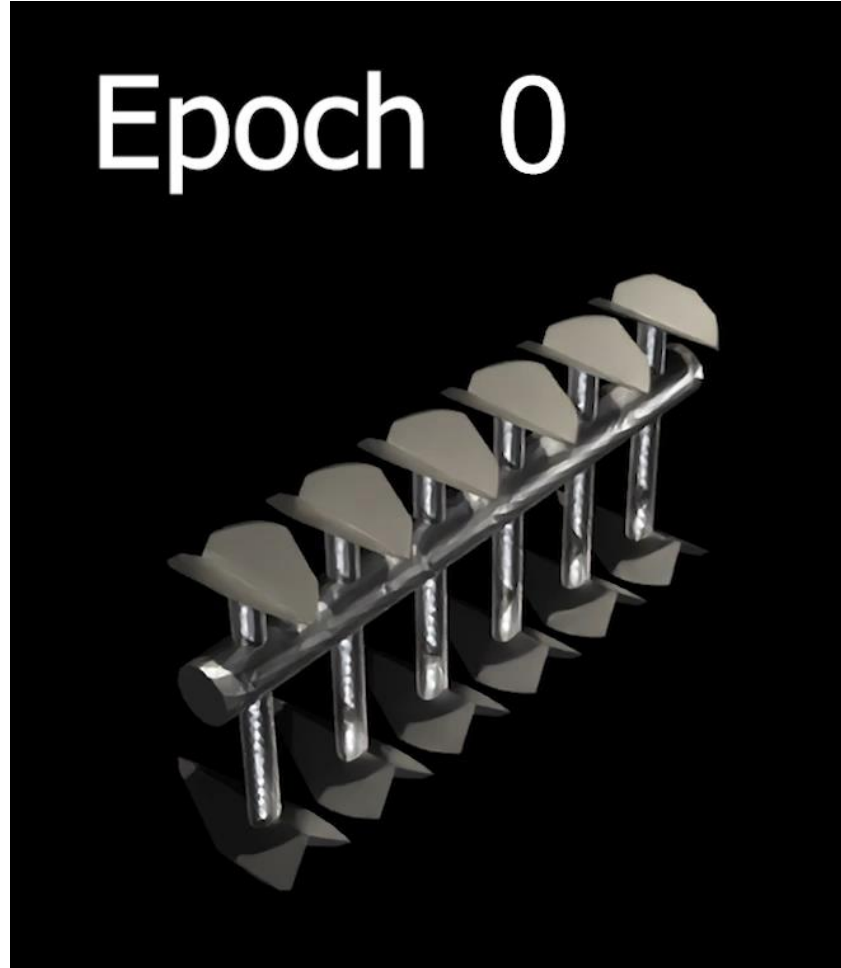


Evolutionary algorithms



Optimisation

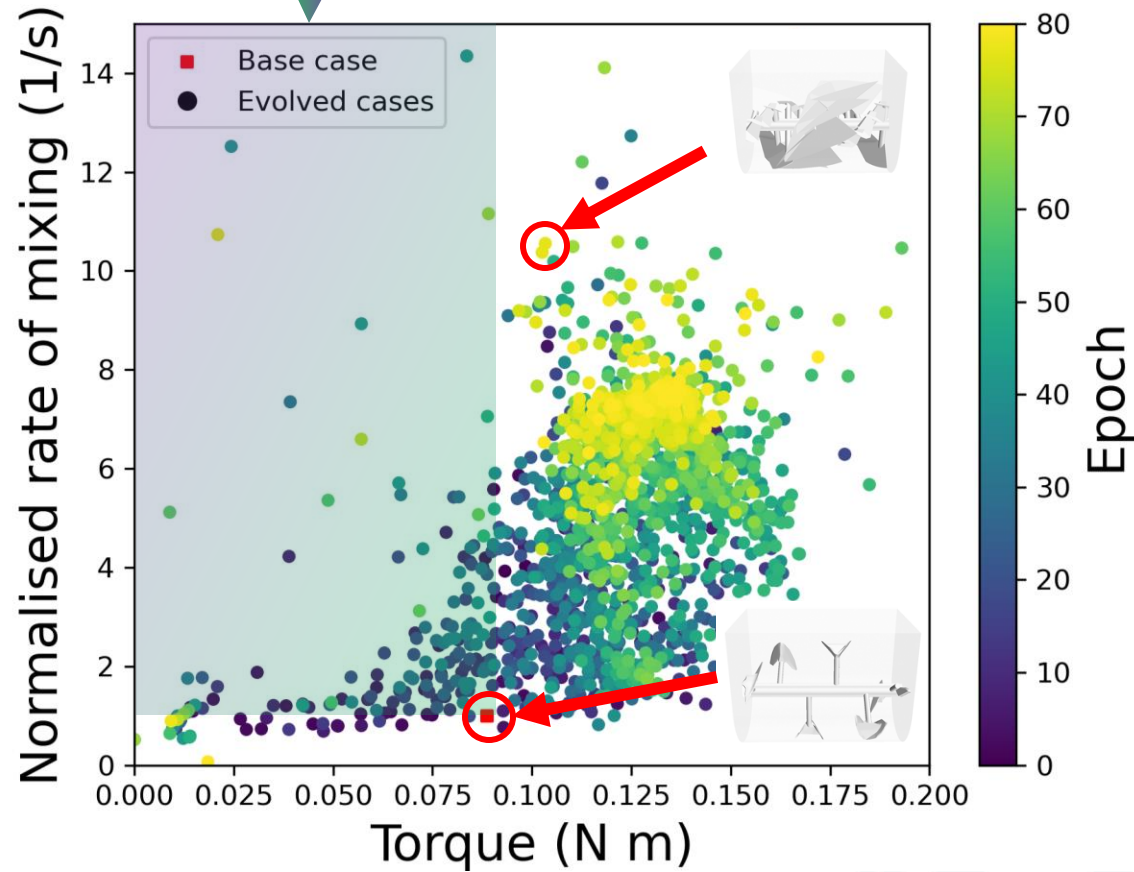
Epoch 0



Optimisation

Increased profit + improved sustainability

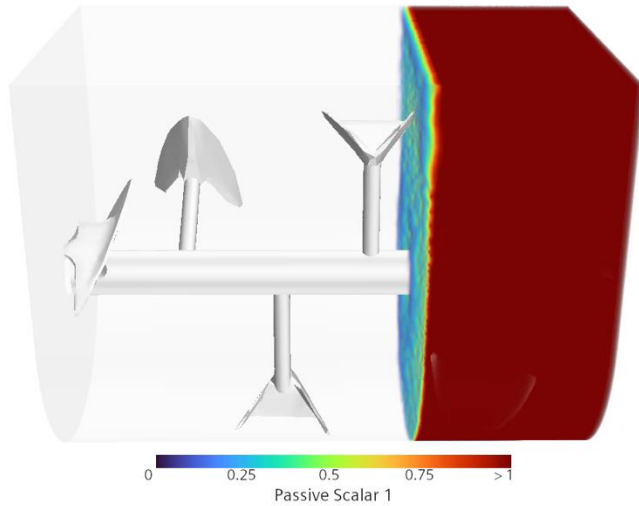
increasing throughput (Profit)



Decreasing energy use (Sustainability)

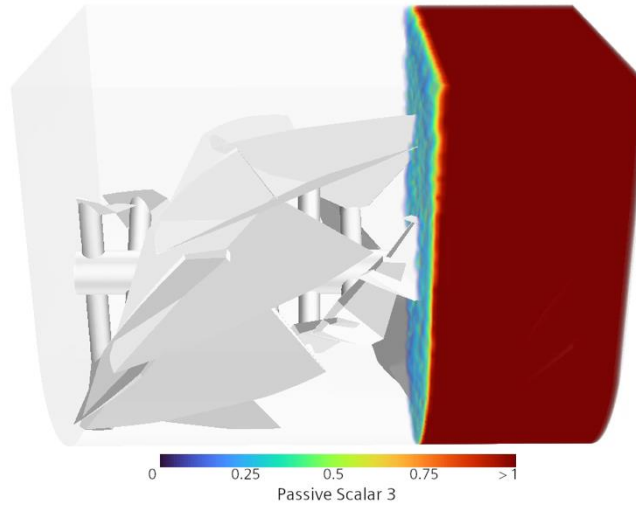
Optimisation

Base case

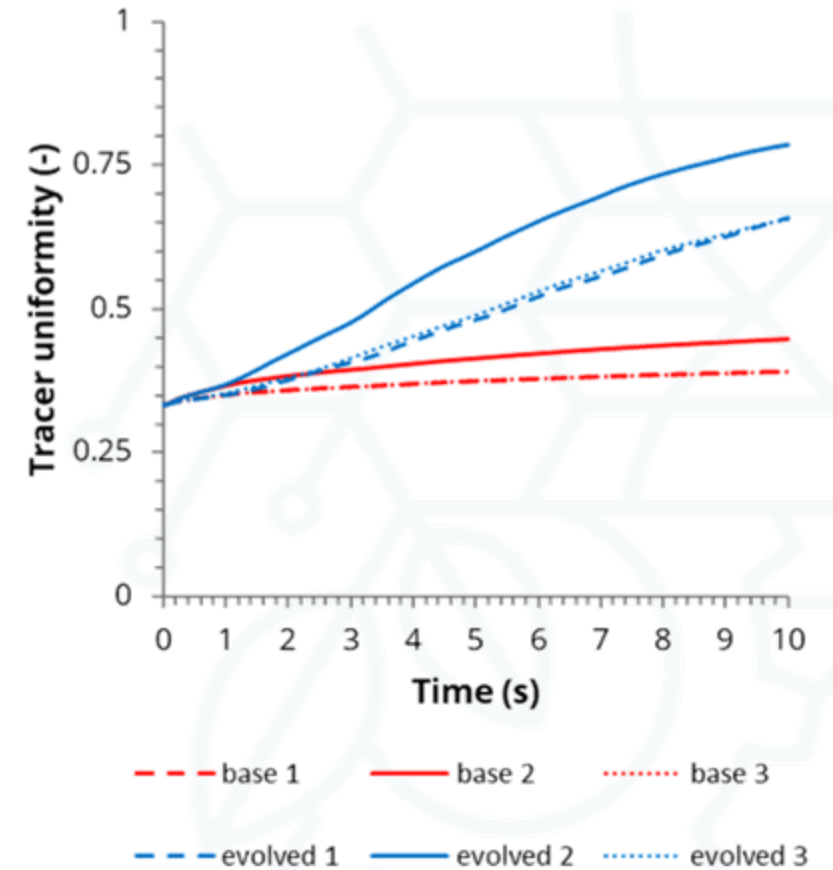


Solution Time 0.04 (s)

Evolved design



Solution Time 0.04 (s)



Impeller comparison



3-D printed design

PEPI experiments

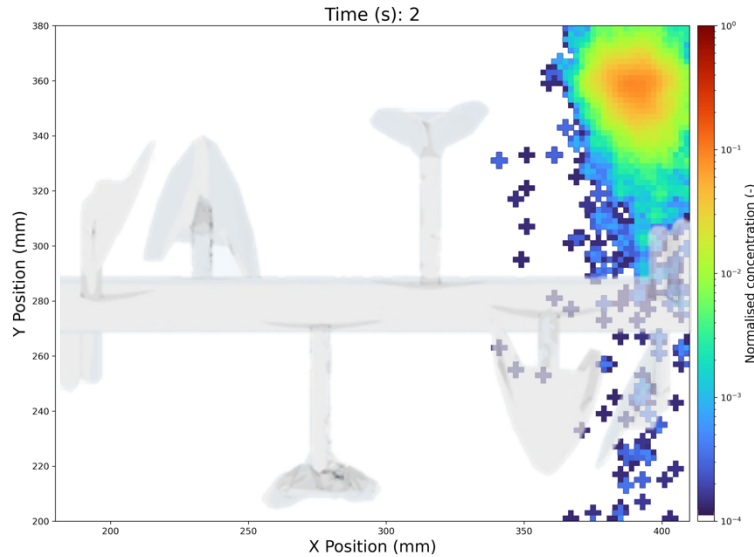
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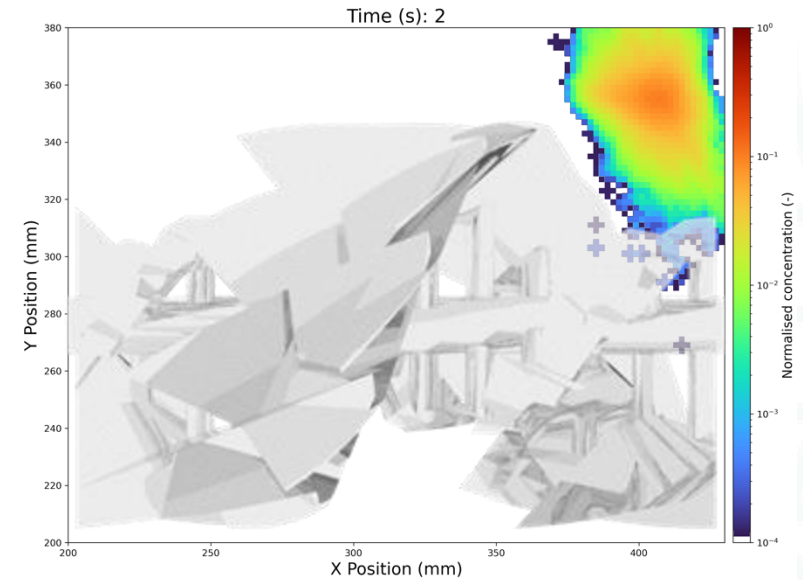
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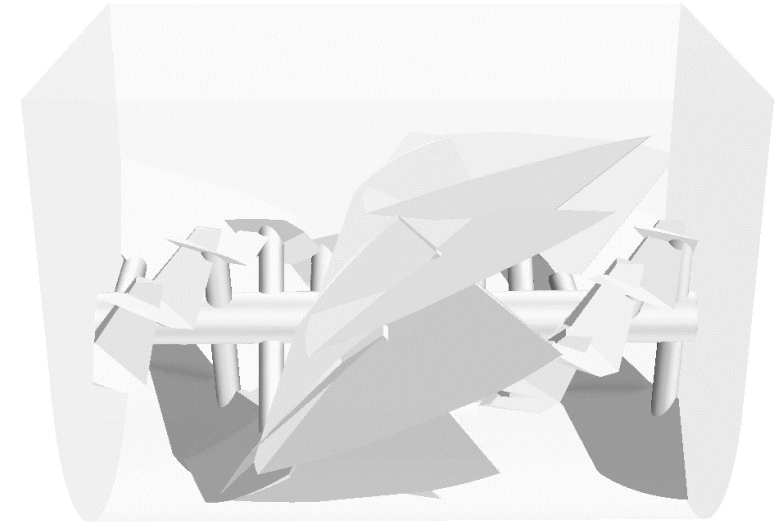
Original design



Evolved design

Conclusions

- PEPI can **validate** model predictions.
- Symbolic regression can discover **predictive models** without prior knowledge
- **General** data-driven approach for autonomous geometry optimisation.
- **Verified >10x** improved rate of axial mixing at similar torque.



Thanks for your time



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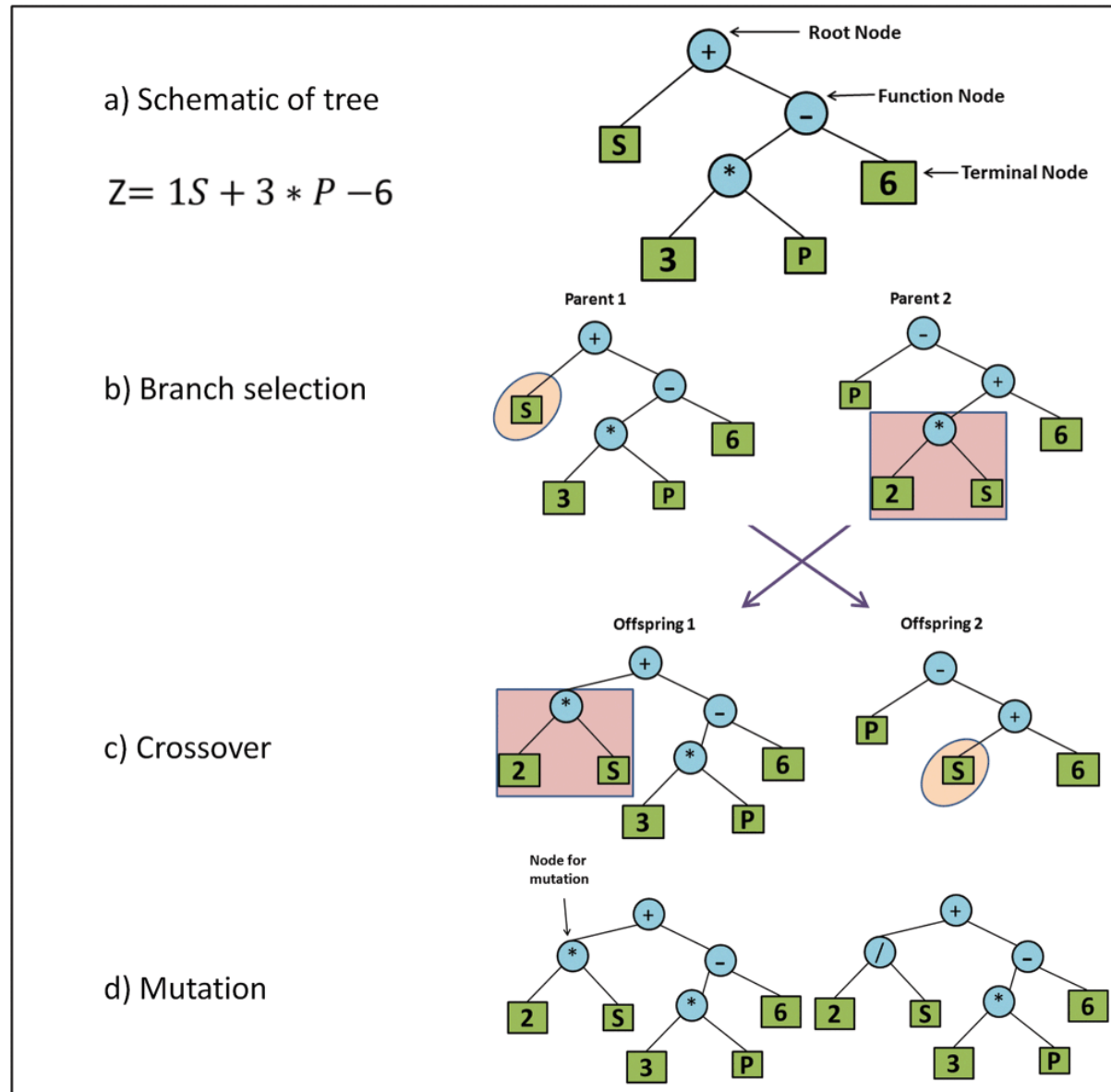
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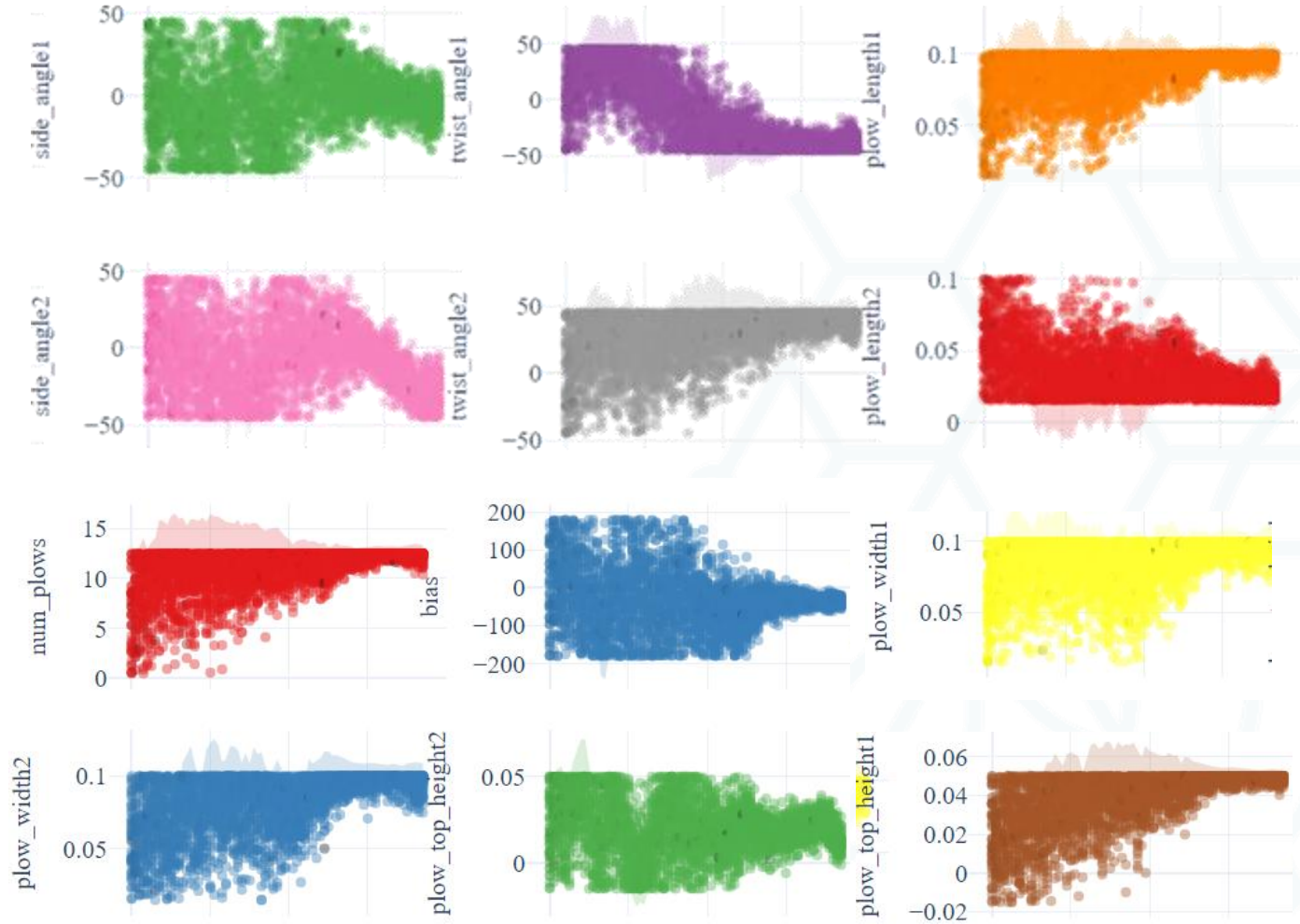
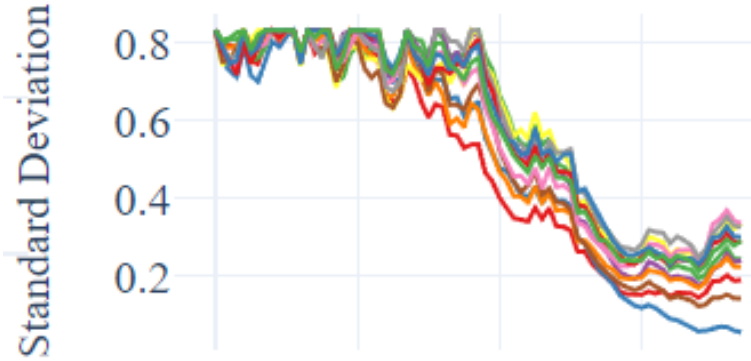
Referenced work

- [1] Jones, J.R., et al 2007. Axial mixing in a ploughshare mixer. *Powder Technology* 178, 73–86.
- [2] Laurent, B.F.C., Cleary, P.W., 2012. Comparative study by PEPT and DEM for flow and mixing in a ploughshare mixer. *Powder Technology* 228, 171-186.
- [3] Forrest, S., et al 2003. Flow patterns in granulating systems. *Powder Technology* 130, 91 -96.
- [4] Hart-Villamil, R., et al 2024. On the autonomous validation and comparison of particle models for a Newtonian laminar flow mixing model using PEPT. *Chemical Engineering Research and Design* 206, 139–150.
- [5] Windows-Yule et al 2022. *PEPT, a Comprehensive Guide*, IoP eBooks, ISBN 9780750330718
- [6] Tatterson, 1991. *Fluid Mixing and Gas Dispersion in Agitated Tanks*, McGraw-Hill, New York.
- [7] Kresta, S. M., et al 2016. *Advances in Industrial Mixing*. John Wiley & Sons.
- [8] Metzner, A. B., Otto, R. E., 1957. Agitation of non-Newtonian fluids. *AIChE J.*, 3: 3-10.
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- [10] Laplante, P. et al 2015. Demulsifier performance in froth treatment. *Fuel Processing Technology*, 138: 361-367.
- [11] Yang, Z., et al 2018. Design and Performance of Helical Ribbon and Screw Impeller Aerobic Compost Bioreactor. *International Journal of Environmental Science and Development* 9.12. 385-389.

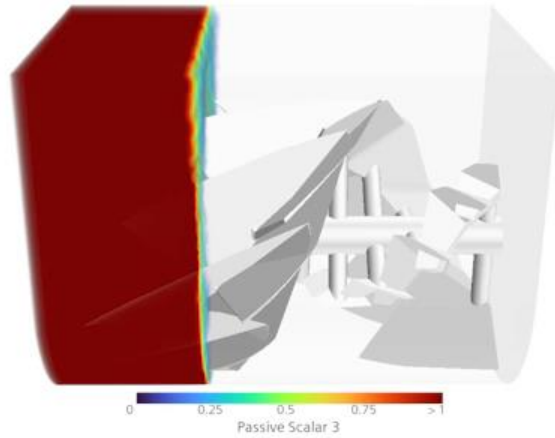
Symbolic regression



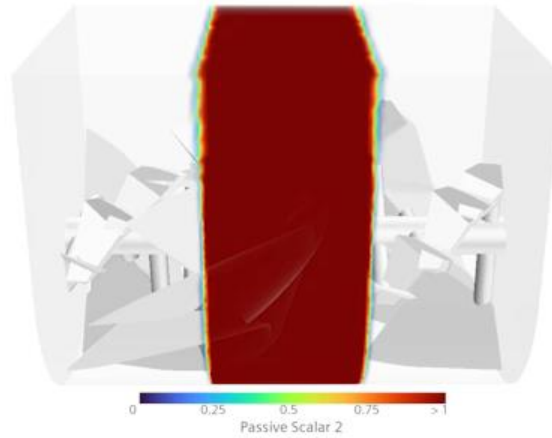
Convergence



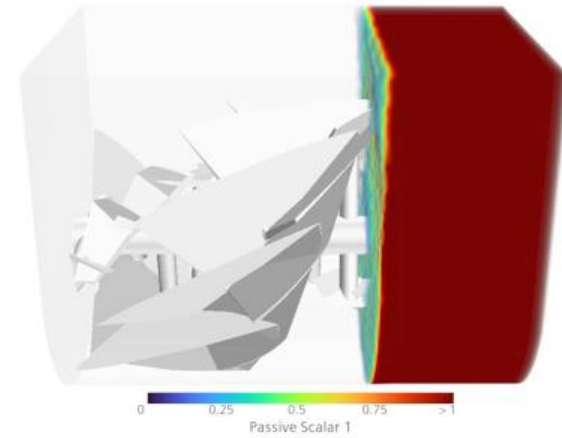
Passive scalar vs Particles



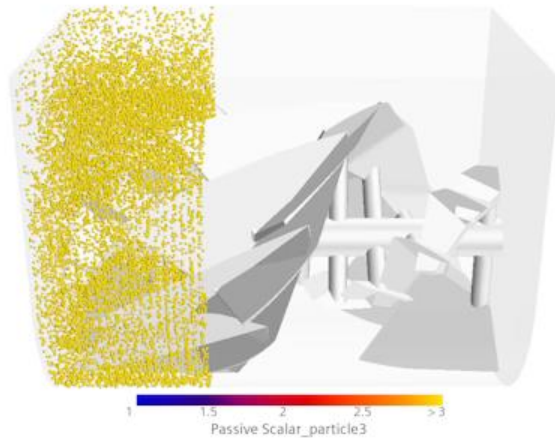
Solution Time 0.04 (s)



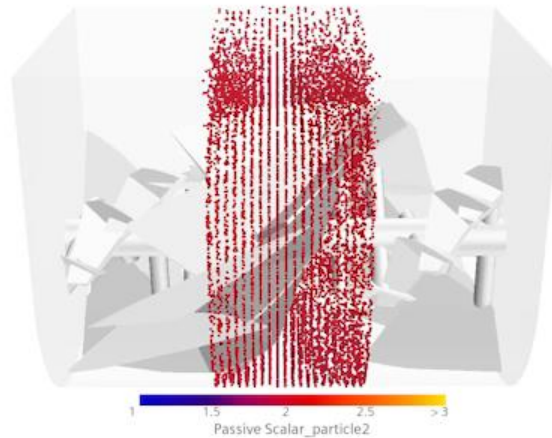
Solution Time 0.04 (s)



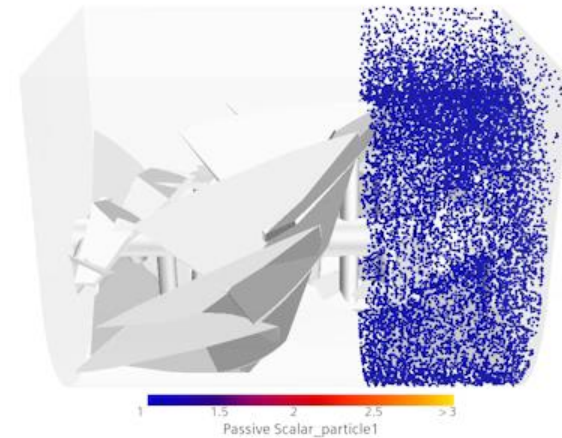
Solution Time 0.04 (s)



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