



- ❖ High viscosity
- ❖ Non-Newtonian rheology (viscoelasticity)

Energy waste

- ❖ Long mixing time
- ❖ Higher minimum mixing speed

Reduced mixing quality

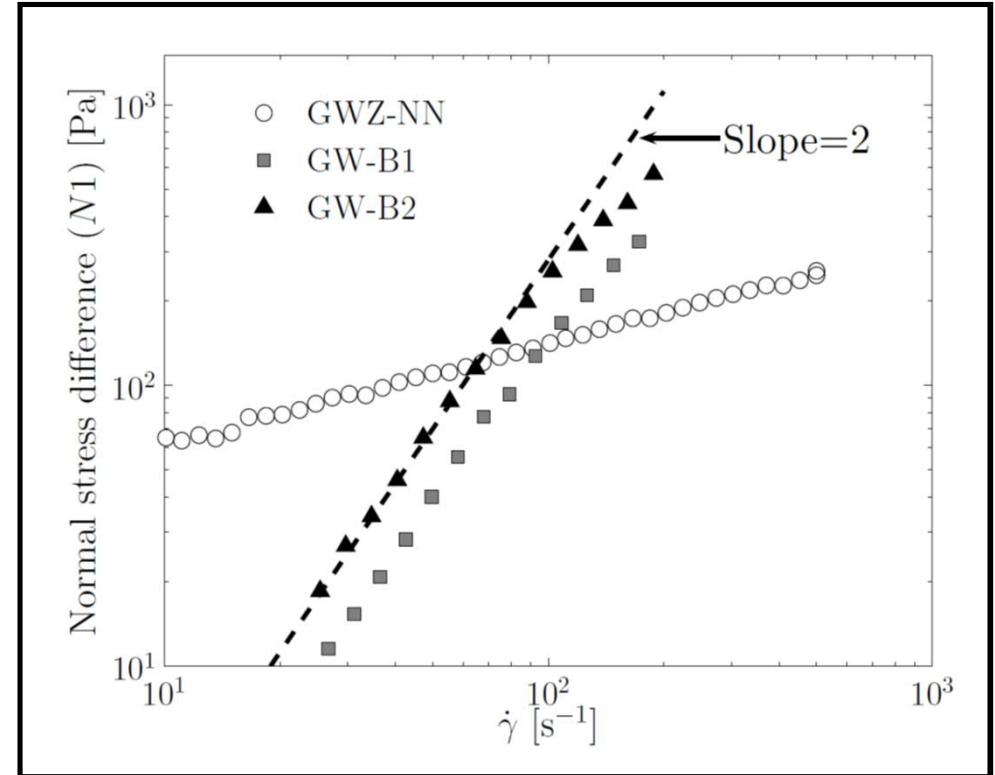
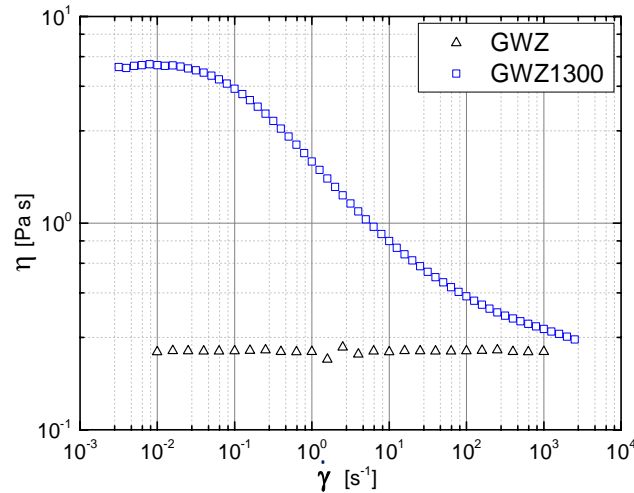
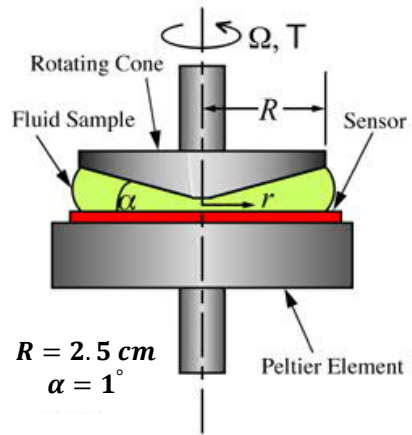
- ❖ Formation of caverns
- ❖ Clustering
- ❖ Dead volumes

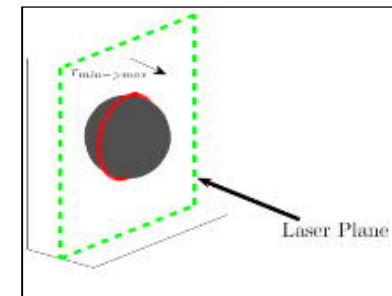
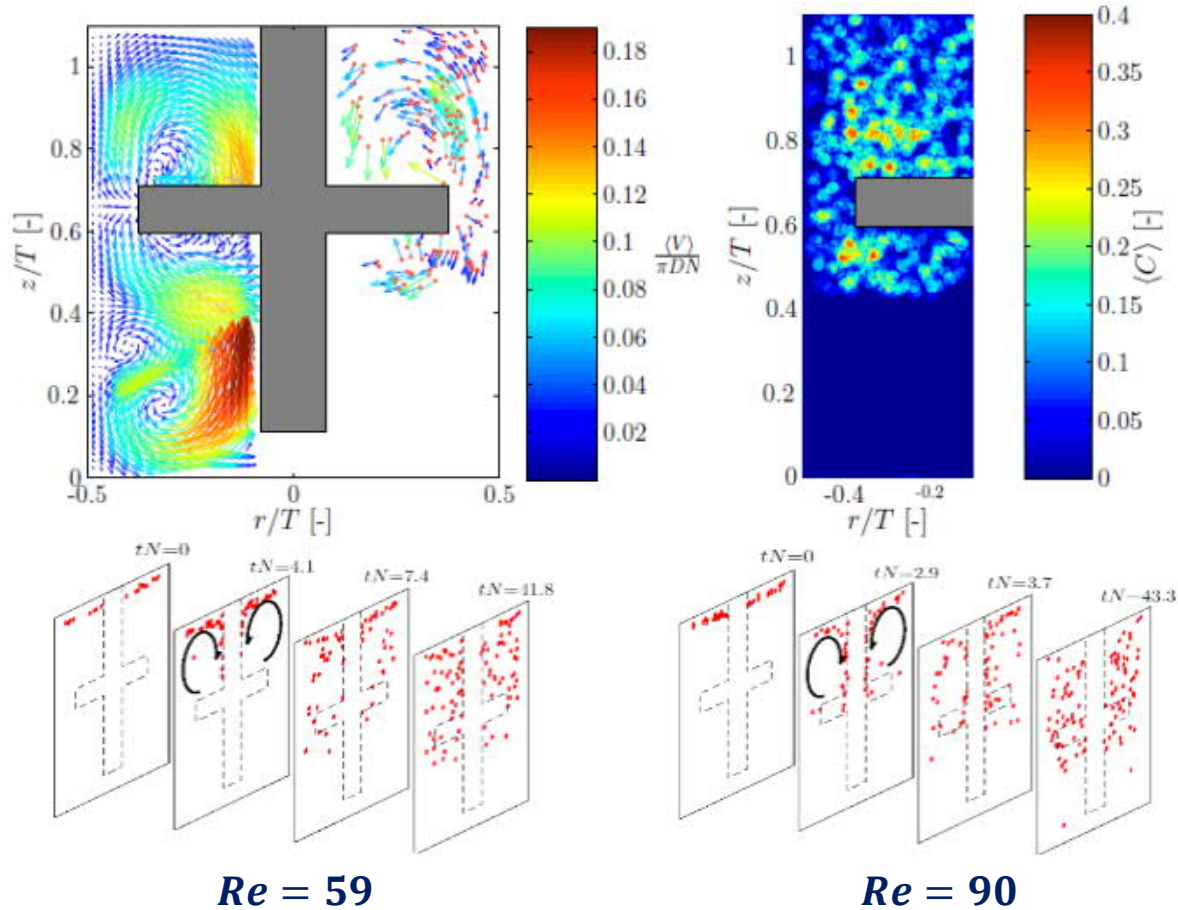
Outline

- Rheological characterization
- Results
 - Newtonian
 - Non-Newtonian
 - Clustering time
- Conclusions and Future work

Rheological characterization

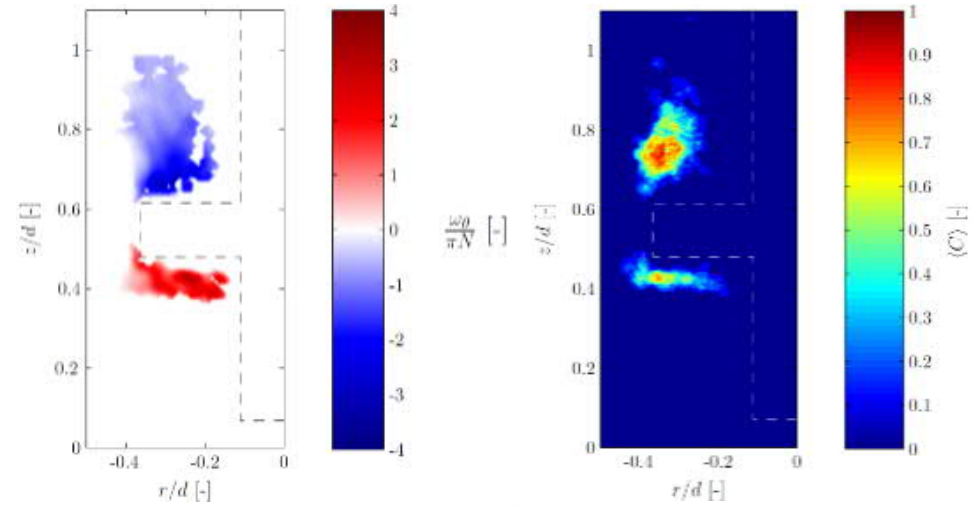
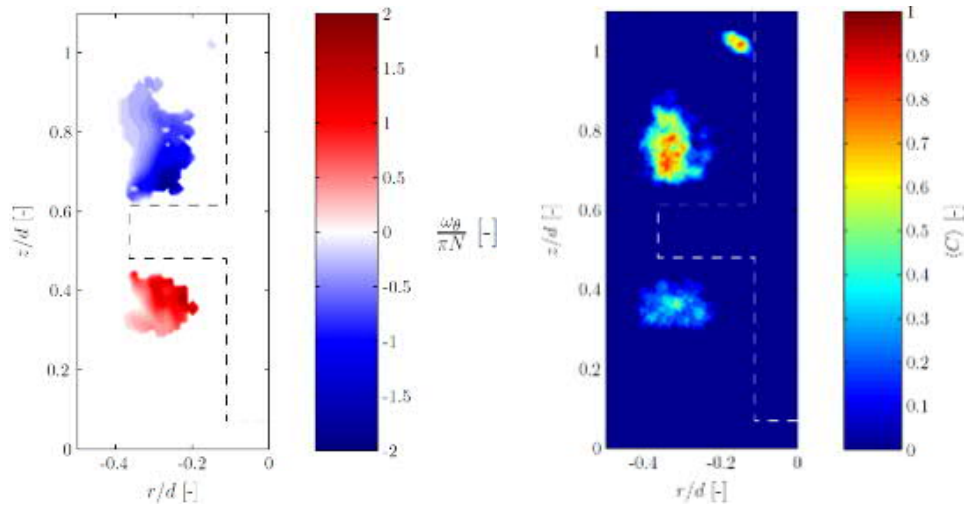
Acronym	Polymer	ρ [Kg/m ³]	μ [Pa s]	r_n
PMMA	-	1180	-	1.489
GWZ-N	-	1630	0.25	1.487
GWZ-NN	0.13% Xanthan gum	1630	ST	1.487
GW	-	1250	0.85	1.475
GW-B1	100 ppm PAA	1250	0.85	1.475
GW-B2	200 ppm PAA	1250	0.85	1.475



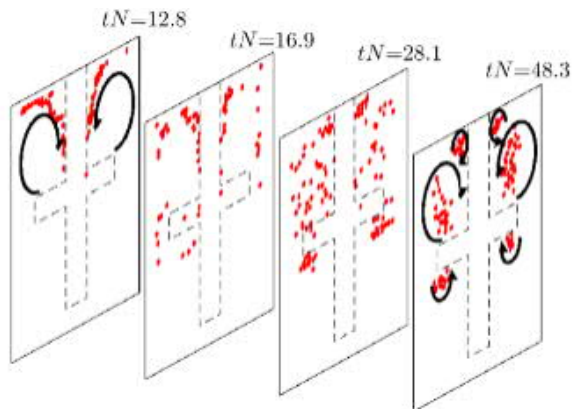


$$\frac{u_{slip}}{u_L} = \left| \frac{u_s - u_L}{u_L} \right| \approx 10^{-2}$$

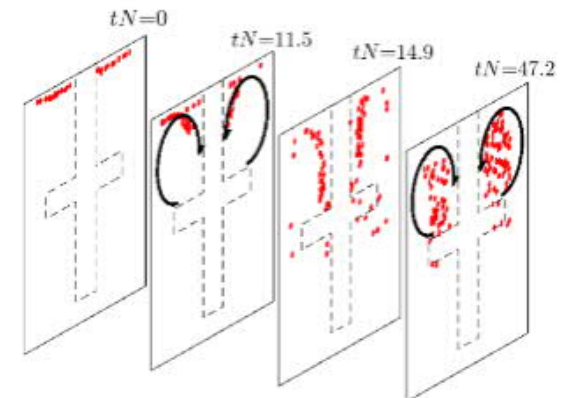
Results – non-Newtonian (GWZ_NN)



Re = 59

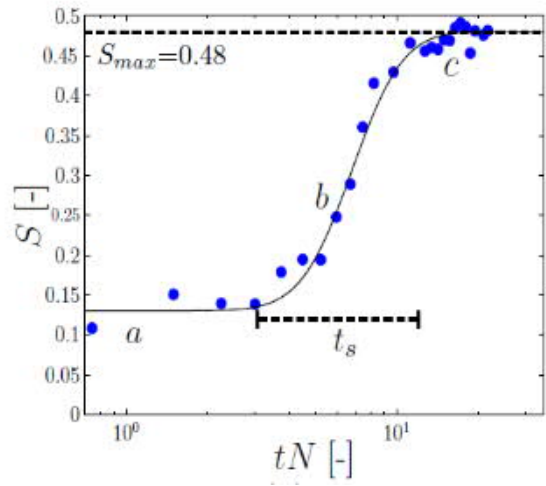
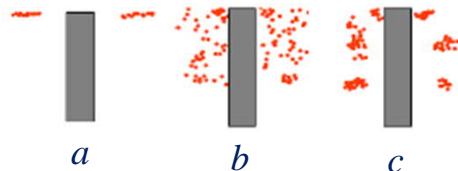
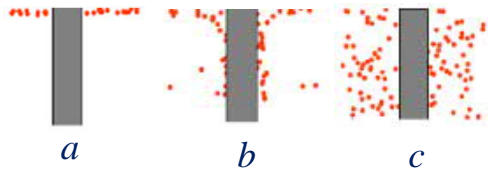


Re = 90

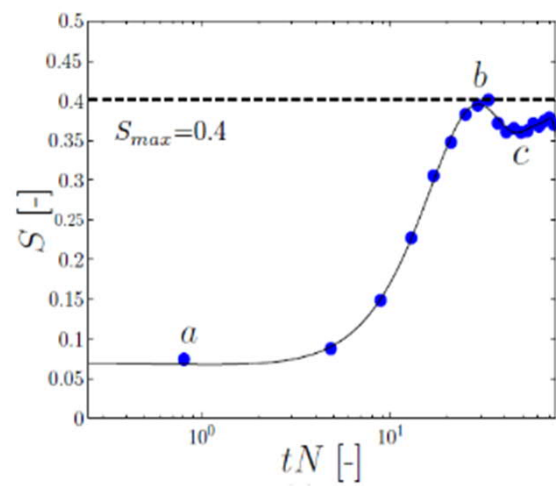


Results – Viscoelasticity driven migration

$$S(t) = p(t)_S \ln(p(t)_S) + p(t)_L \ln(p(t)_L)$$

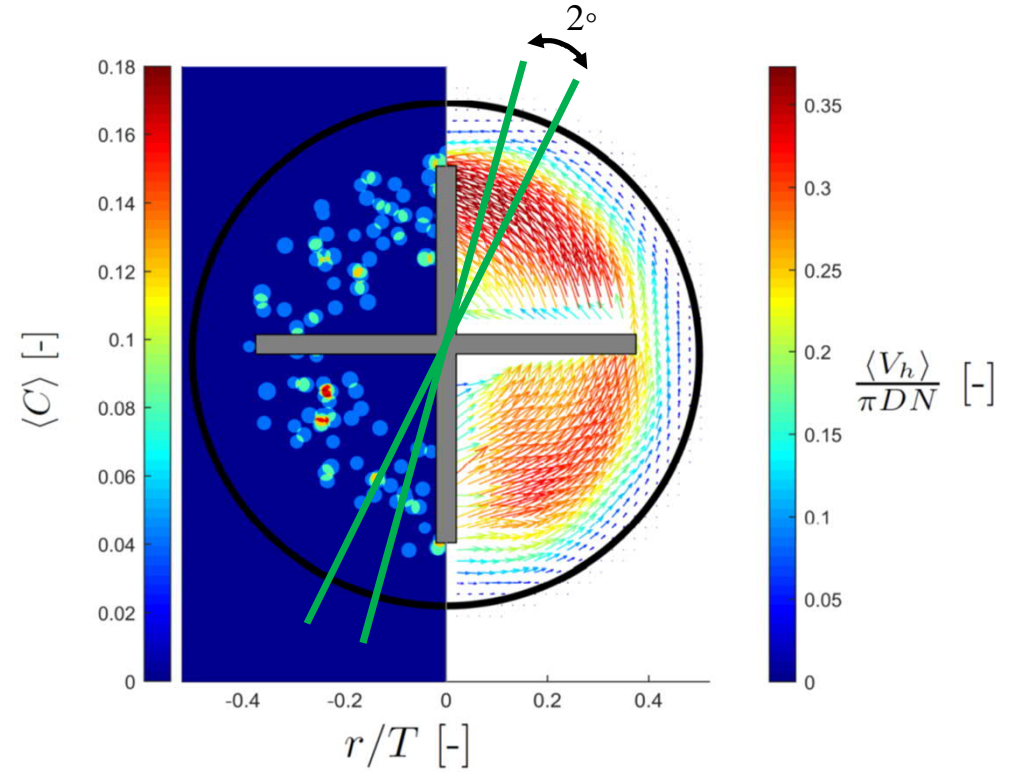
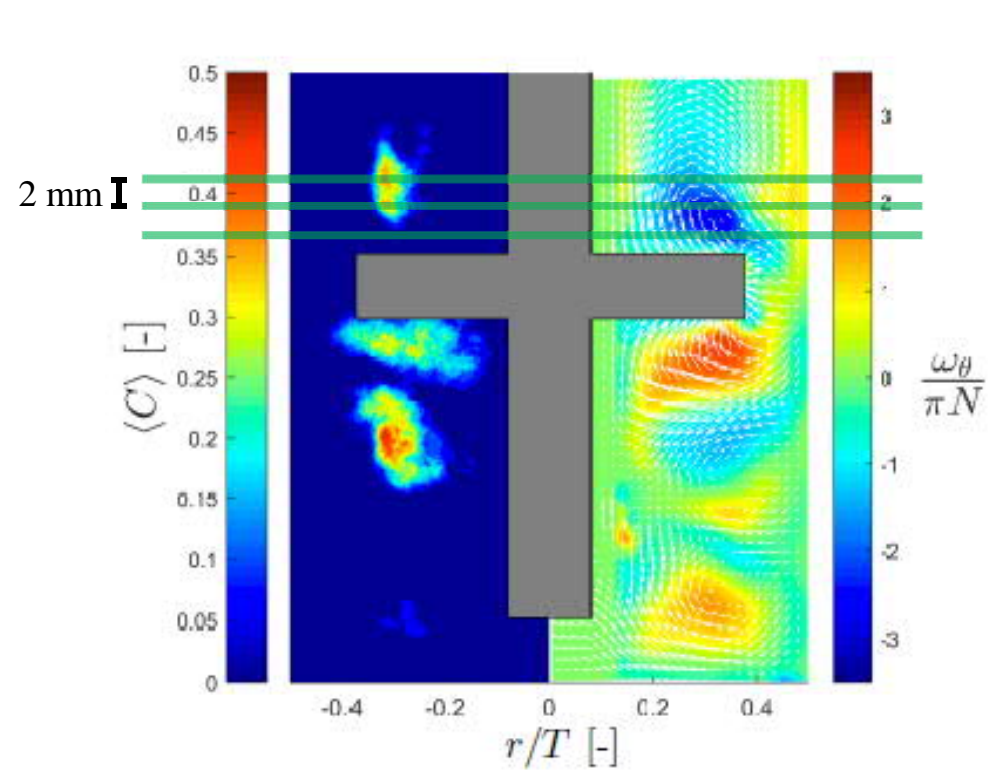


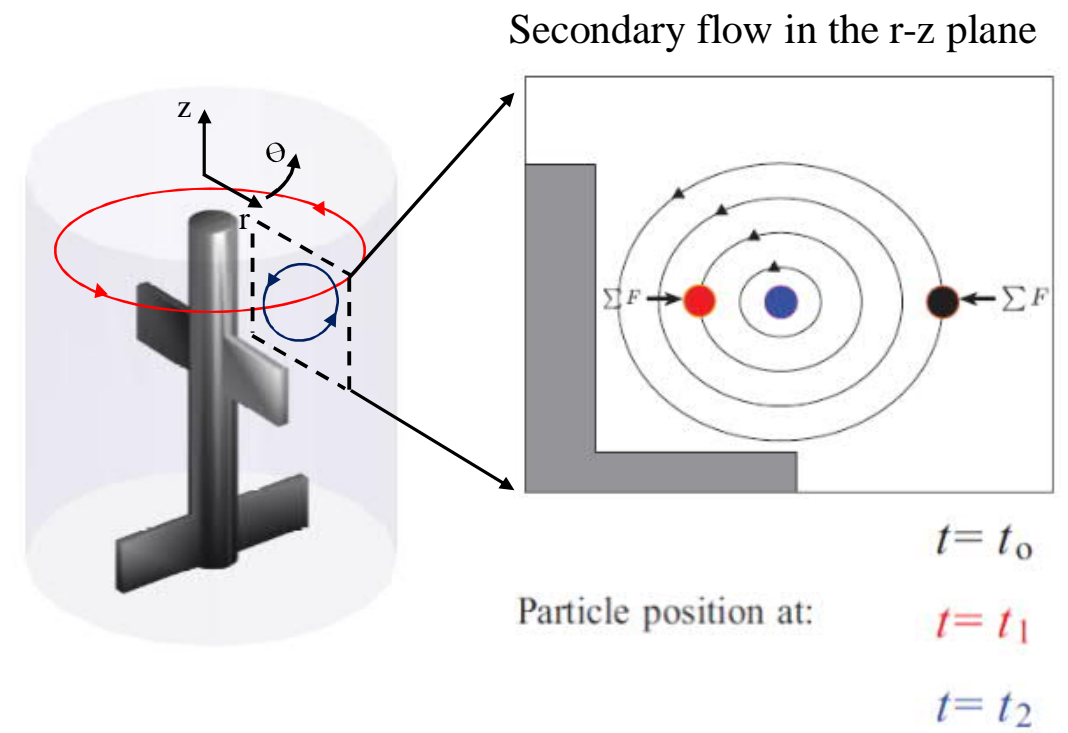
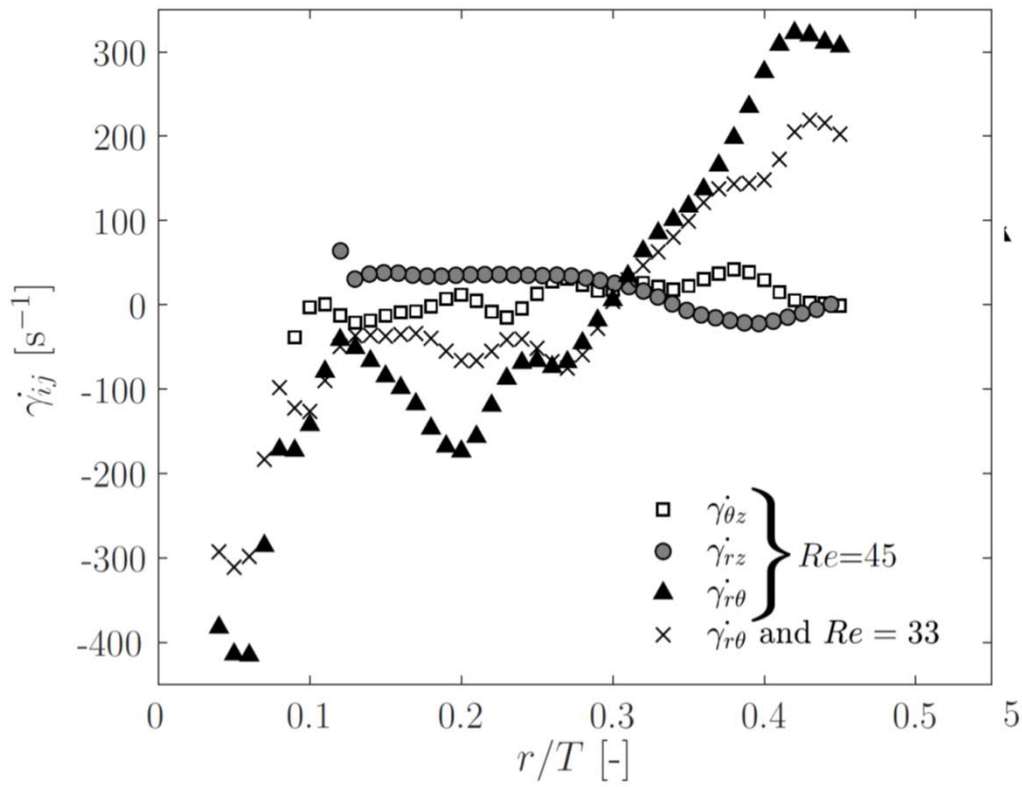
Newtonian Re=58

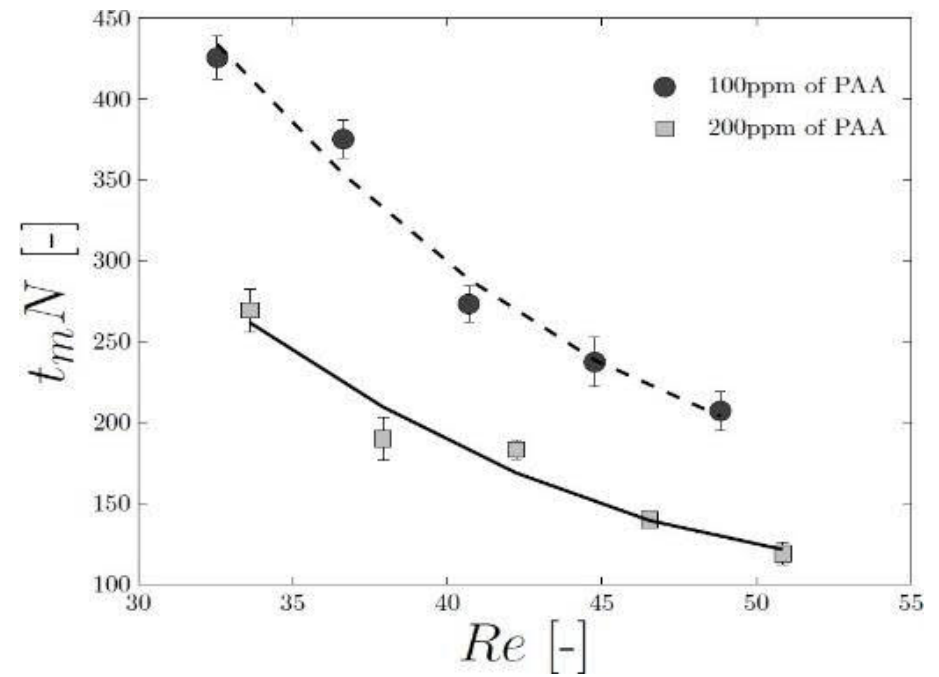
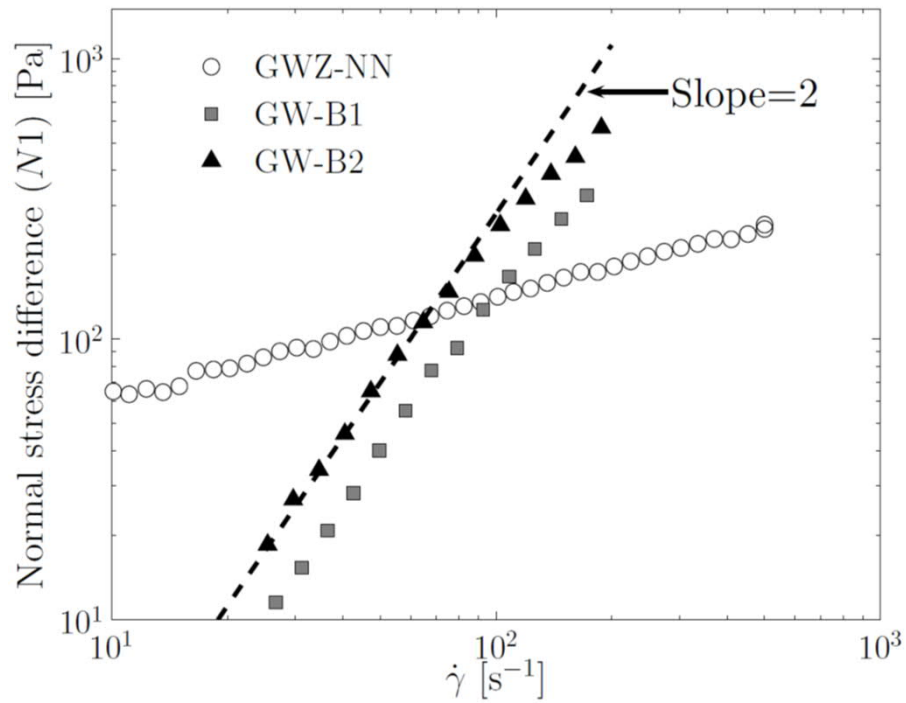


Non-Newtonian Re=58



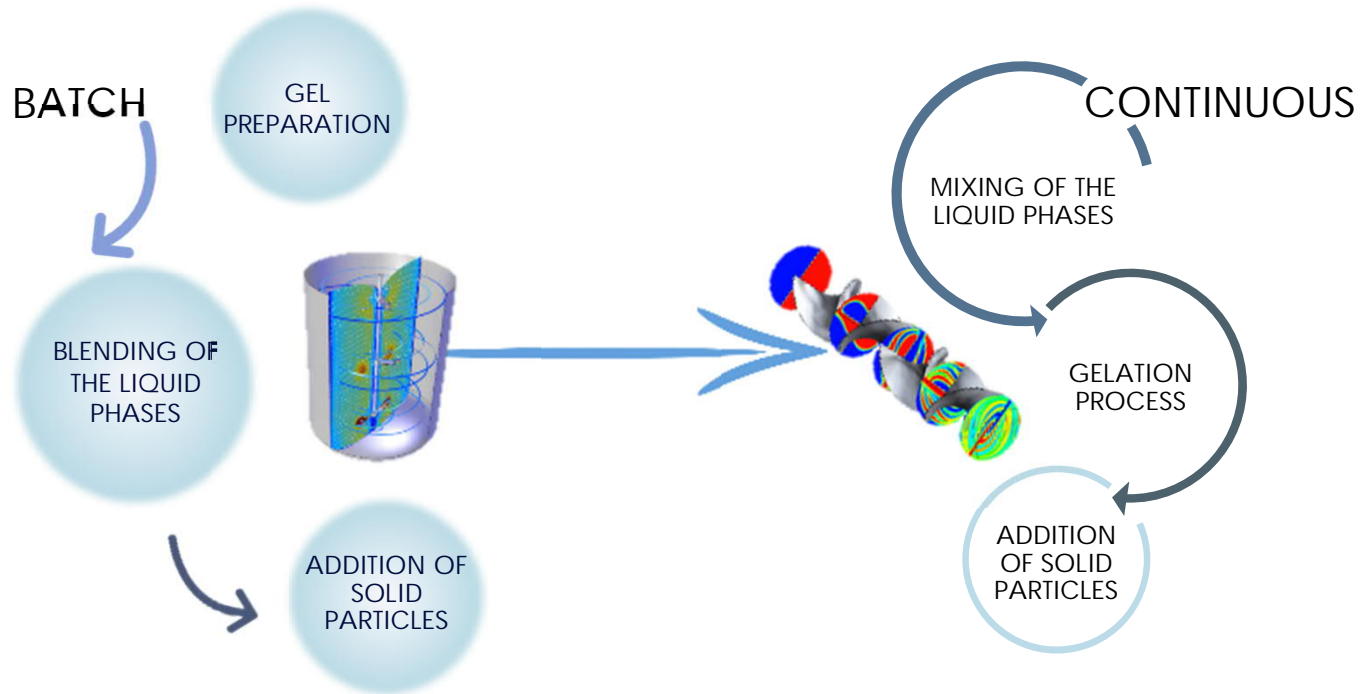






Future work

- Use a multi-phase CFD model to simulate the motion of a solid sphere in a viscoelastic fluid subjected to the 3D flow of a stirred vessel
- Decouple the suspension mechanism from the viscoelastic induced migration in order to estimate a migration velocity (migration time)
- Correlate the migration characteristic time with the rheology of the suspending fluid (scaling law)



- **W. H. Weheliye, G. Meridiano, L. Mazzei, P. Angeli, *Experimental investigation of the solid-liquid separation in a stirred tank owing to viscoelasticity*, Physical Review Fluids (2020)**